Numerical Investigation of Non-linear Radiation Effects in Boundary Layer Oblique Stagnation Point Flow of non-Newtonian Fluids over a Symmetrically Stretching Surface under the Effects of Magnetic Field *Bilal Ahmed^{1,*}*, *M. Noman¹ A. Agsa¹ and S. Kanwal¹*

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Abstract: The numerical solution of the flow of non-Newtonian fluid induced by symmetrically 7 stretching fractal sheet in the region of oblique stagnation point flow under the inducement of ex-8 ternally applied uniform magnetic field orthogonal to the flow is presented. The analysis is made 9 under the assumption of a boundary layer which arrives at the system of partial differential equations 10 which afterward is transformed into ordinary differential equations by using appropriate similarity 11 transformations. The numerical solution of the modeled system of equation is obtained by parallel 12 shooting technique and then presented for different variations of involved parameters. It is noted that 13 enhancement in the magnetic field results in a decrease in horizontal velocity and the boundary layer 14 becomes thinner. The behavior of streamlines shows that the symmetry of the flow is highly de-15 pendent on the obliqueness of the stagnation point flow. It is seen that when the ratio of a/c > 1, the 16 flow has a normal boundary layer structure but when a/c < 1 then the structure shows inverted 17 behavior. It is also seen that there exists no boundary layer when a/c=1. The obtained results are 18 also compared with the available results in the literature and found in excellent agreement in the 19 limiting cases. 20

Keywords: Thermal radiation; uniform magnetic field; boundary layer; Maxwell fluid; oblique 21 stagnation point 22

1. Introduction

When a fluid reaches the stagnation point, its local velocity becomes zero. The surface of the 24 body exists in the flow at fluid stagnation point, and the fluid of the body is at rest. The oblique 25 stagnation point flow discussed and combined at a plane wall are free restriction positions. Stagnation 26 point flow at oblique flow consists of an orthogonal flow to which an infinite velocity is added. When 27 a fluid collides with a surface, its velocity vanishes, or becomes zero, this is referred to as a stagnation 28 point. Recently many researchers have been taking extra interest in stagnation point flows due to 29 numerous applied applications in different industries. Cooling of nuclear reactors is an example of 30 stagnation flow. In stagnation flow, the attention-able thing is that the greatest heat moves, and 31 pressure gradient is found at stagnation stage. Initially Stuart [1] worked on stagnation flow obtained 32 the analytical solutions for the flow. Tamada [2] and Dorrepaal [3] were the first who generalize the 33 flow involving stagnation point and obtained solution for oblique stagnation point. In their study, 34 Tooke and Blyth [4] conducted a concise examination of oblique stagnation point flow. Their find-35

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ings revealed that, in the presence of significant adverse pressure gradients, there exists a region near the wall where the shear component experiences reversed flow. Interestingly, the integration of orthogonal flow with shear flows, each exhibiting varying degrees of reversed flow, consistently results in the same oblique flow pattern. However, the attachment point of stagnation is predictably displaced along the wall. Husain et al. [5] worked on continuous the work viscoelastic fluid model in stagnation point flow.

The non-Newtonian fluid model is more difficult and complex to solve the individual constitu-42 tive equation, but the Newtonian fluid model is easy to solve the constitutive equation. Moreover, the 43 purpose of much research describes their application, Maxwell finds the proposal attention to the 44 simplicity of viscoelastic fluid. Wang and Tan [6] studied the linear stability explanation by the 45 Maxwell fluid model with the thermal diffusion effect. Mukhopadhyay [7] and Nadeem et al. [8] 46 provided more generalized literature. The most important stretching surface used by industrial firms, 47 such as warm progression, metal sheet freezing, crystal fibers, wire drawing, and various other ma-48 terials. The oscillatory convection damaged the system by thermal diffusion and undependability of 49 the rise system due to increase time composure. Bilal et al. [9] the three combined convection radi-50 ative flow of non-Newtonian fluid over an inclined stretching surface in the presence of thermo-51 phoresis and the condition is convective. Javed et al. [10] noticed that Maxwell fluid is the more 52 suggested flow of stagnation point comprehensively. Tariq et al. [11] study the numerical analysis 53 mixed convection boundary layer flow second grand viscoelastic due to cylinder of the elliptic cross 54 section with prescribed surface heat flux. 55

A flow model solves the boundary layer approximation by a non-linear equation like continuous 56 and momentum transformation. Sajid et al. [12] analyzed the heat transfer in the stagnation- point 57 flow of a Jeffrey fluid elapsed lubricant to reduce friction and wear and tear in contact between two 58 surfaces. Khan et al. [13] generalized diffusion effects on Maxwell nanofluid stagnancy point flow 59 over an extended sheet with chemical reaction in slip conditions. Jawad et al. [14] studied the parti-60 tion of Non-linear thermal radiation and the sticky carelessness effect on the time-independent ro-61 tating in the three-dimensional flow of single-wall carbon nanotubes with sedimentary suspensions. 62 Majeed et al. [15] studied the influence of rotating the magnetic field on Maxwell concentrated fer-63 rofluid flow over a heated widening sheet with heat generation. Khalid et al. [16] heat transfer in the 64 flow of Jeffrey fluid past a lubricated surface near a stagnation point flow. Rasool et al. [17] the 65 magnetic field and effects of radiation of stagnation point flow on mixed convection flow of a cyl-66 inder under local thermal non-equilibrium in a porous medium. Reza-E-Rabbi et al. [18] the fluid 67 flow behavior over a stretching sheet computational modeling of multiphase radiative Casson and 68 maxwell fluid the appearance of nano-size particles. 69

Khan et al. [19] the analysis mixed convection flow of Maxwell fluid as the combination of both70coupled free and force convection between two infinite stretching disks with the source of heat. This71paper investigates the problem of oblique hydromagnetic stagnation flow of point an electrically72

Casson fluid over a stretching sheet embedded in a doubly stratified medium in the presence of heat 73 source and thermal radiation with the first chemical reaction. Ibrahim et al. [20] presented study 74 slipped effect on stagnation point flow of upper converted non-Newtonian fluid of nanofluid passing 75 a stretching sheet with chemical reaction. Mekheimer and Ramadan [21] provided the study about the 76 perspectives on gyrotactic microorganisms in the context of bio-thermal convection of Prandtl 77 nanofluid over a permeable sheet subjected to stretching or shrinking and revealed that temperature 78 and density of motile microorganisms are elevated when a shrinking sheet is considered, in contrast 79 to the case of a stretching sheet. 80

Chu et al [22] investigated the heat and mass transfer in hydromagnetic stagnation point flow and 81 provide the dual solution for the Carreau nanomaterial using Runge-Kutta Fehlberg method and 82 concluded that velocity of fluid is raised for both solution by raising the intensity of suction param-83 eter. Khan et al. [23] presented the numerical solution of the stagnation point flow of non-Newtonian 84 fluid Cattaneo-Chirstov heat flux model and deduced that magnitude of drag force or velocity gra-85 dient increases via increase in the strength of applied magnetic field. Mathew et al. [24] considered 86 multi slip and nanoparticle shape to analysis the stagnation point flow of silver blood fluid. Stagna-87 tion point flow and heat transfer analysis over stretching surfaces like plates and cylinders are ad-88 dressed by Turkyilmazoglu [25]. He evaluated the exact solution for the flow modeled equations and 89 deduced from the solution that heat transfer rates from the surfaces in both flow geometries are en-90 hanced by the action of walls, with more cooled surfaces in the presence of wall suction. Zaheer et al. 91 [26] investigated Electroosmotic Forces Driving Boundary Layer Flow of a Non-Newtonian Fluid 92 Containing Planktonic Microorganisms Using the Darcy-Forchheimer Model and concluded that In 93 comparison to a Newtonian fluid, the boundary layer velocity is reduced when dealing with a 94 non-Newtonian fluid. However, the presence of the electro-osmotic parameter causes an increase in 95 boundary layer velocity. 96

Abbasi et al. [27] gave the outcomes about the impacts of nonlinear warm radiation for axisymmetric 97 rotational stagnation point stream with initiation energy and referenced that hub speed increments 98 while auxiliary speed diminishes by expanding the turn boundary. Wahid et al. [28] looked into the 99 MHD stagnation-point flow of nanofluid caused by a shrinking sheet with melting, viscous dissipa-100 tion, and Joule heating effects. They recommended that the concentrate likewise proposes consid-101 ering 2% of alumina volume part rather than 1% so the stream detachment interaction can be post-102 poned, and at the same time support the laminar stream. At a certain level of shrinkage, the increased 103 melting effect reduces skin friction by approximately 5%. Reddy et al. [29] reasoned that an increase 104 in the Prandtl number results in a reduction in the temperature profile when they examined the vehicle 105 properties of the stagnation point stream of hydro-attractive radiative nanofluid on the extending 106 surface. Baig et al. [30] examined the precise solution of stagnation point flow on a nanofluid cyl-107 inder in the presence of ambient heat. Their research revealed that stagnation flow prevails over 108 stretching flow at higher oncoming pressure flow values. Most of the published research on stagna-109 tion point flow uses numerical methods to explain the subject, but the goal of their study is to provide
a precise solution to the issue at hand. Gadelhak et al. [31] provide the Numerical Analysis of Energy
Transport in Williamson Nanofluid Flow over a Curved Stretching Surface Using Finite Difference
Method (FDM) and deduced that the heat flux decreases as the curvature parameter attains higher
values further down. Additionally, both the Sherwood number and Schmidt number increase with
higher values of the curvature parameter.

Many analyses show that the study of two-dimensional boundary layer stagnation point flows is 116 interesting in the analysis of fluid flow and heat transfer over a stretching sheet. The basis for this is 117 that these kinds of research have been used in the manufacturing sector. The creation of glass fiber, 118 hot rolling, continuous casting, extrusion, manufacture of sheets, coating, and production of paper are 119 examples of manufacturing processes. In the present problem, the study of boundary layer oblique 120 stagnation point flow of Maxwell fluid with radiation effects over a linear stretching sheet under the 121 inducement of the magnetic field has been carried out which has not been studied yet. The mathe-122 matical modeling based on Tooke and Blyth [4] and numerical simulation using the parallel shooting 123 technique of governing equations are presented. The effects of different involved parameters on heat 124 and fluid flow are presented through tables and graphs and a detailed discussion is given in the later 125 part of the manuscript. An excellent agreement of results has been found with Pop et al. [32] and 126 Javed and Ghaffari [10]. 127

2. Problem Formulation

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Consider the two-dimensional steady flow of Maxwell fluid over a stretching sheet in the region 129 of non-orthogonal stagnation point under the influence of externally applied uniform magnetic field 130 orthogonal to the flow. The stretching sheet is assumed along the plane y = 0 and the flow moves 131 along the y-axis. The velocity $U_w = cx$ is the stretching velocity of the sheet, with c(>0) being 132 the stretch constant as shown in Figure 1. The governing equations in the presence of body forces that 133 describes the current flow are, 134

$$div\overline{V} = 0,\tag{1}$$

$$\rho \frac{d\overline{V}}{dt} = -\nabla p + div\overline{S} + \rho b, \qquad (2)$$

$$\overline{u}\frac{\partial\overline{T}}{\partial\overline{x}} + \overline{v}\frac{\partial\overline{T}}{\partial\overline{y}} = \frac{k}{\rho c_p}\overline{\nabla}^2\overline{T} - \frac{1}{\rho c_p}\overline{\nabla}.q_r,$$
(3)

The *div* characterizes the divergence operator, $\overline{V} = [\overline{u}, \overline{v}, 0]$ is the vector velocity, \overline{u} and \overline{v} are 135 the velocity movement components in the direction of \overline{x} and \overline{y} axis respectively. The bar shows 136 that these quantities are in dimensionless form that will be converted into dimensional form where ρ 137 is the density, p is the pressure, κ is the thermal conductivity fluid, c_p is the steady pressure of 138 real heat, b is the body force caused by the magnetic field and q_r represents the radiative heat 139 flux and \overline{S} is the extra stress tensor for Maxwell fluid is explain below, 140

$$q_r = -\frac{4\sigma^*}{3(\alpha_r + \sigma_s)} \nabla \overline{T}^4, \tag{4}$$

$$\overline{S} + \lambda_1 \frac{D\overline{S}}{Dt} = \mu \overline{A}_1, \tag{5}$$

where Stefan Boltzmann's-constant is σ^* while α_r, σ_s, μ , and λ_1 the Rosseland definition is the 141 corresponding fluid for dynamic viscosity, scattering coefficient, absorption coefficient, and time 142 relaxation content. \overline{A}_1 is the representation of the first tensor by Rivlin Ericksen, explained by, 143

$$\overline{A}_{1} = \overline{L} + \overline{L}^{T}.$$
(6)

The of velocity gradient and its transpose are represented by \overline{L} and \overline{L}^{T} respectively which are 144 defined as, 145

$$\bar{L} = \begin{pmatrix} \frac{\partial \bar{u}}{\partial \bar{x}} & \frac{\partial \bar{u}}{\partial \bar{y}} & 0\\ \frac{\partial \bar{v}}{\partial \bar{x}} & \frac{\partial \bar{v}}{\partial \bar{y}} & 0\\ 0 & 0 & 0 \end{pmatrix} \text{ and } \bar{L}^{T} = \begin{pmatrix} \frac{\partial \bar{u}}{\partial \bar{x}} & \frac{\partial \bar{v}}{\partial \bar{x}} & 0\\ \frac{\partial \bar{u}}{\partial \bar{y}} & \frac{\partial \bar{v}}{\partial \bar{y}} & 0\\ 0 & 0 & 0 \end{pmatrix}.$$
(7)

The D/Dt is an operator explained correspondingly in the form of a contravariant vector and 146 contravariant tensor of rank 2 in Eq. (8) and (9) respectively. 147

$$\frac{DS}{Dt} = \frac{dS}{dt} - \overline{L}\overline{S},\tag{8}$$

$$\frac{D\overline{S}}{Dt} = \frac{dS}{dt} - \overline{L}\overline{S} - \overline{S}\overline{L}^{T}.$$
(9)

Divergence applied on Eq. (5) yields,

$$\left(1 + \lambda_1 \frac{D}{Dt}\right) \nabla . S = \mu \nabla . \overline{A}_1.$$
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Application of
$$\left(1 + \lambda_1 \frac{D}{Dt}\right)$$
 on both sides of Eq. (2) yields, 149

$$\left(\rho \frac{d\overline{V}}{dt} + \nabla p\right) \left(1 + \lambda_1 \frac{D}{Dt}\right) = \left(1 + \lambda_1 \frac{D}{Dt}\right) div\overline{S} + \left(1 + \lambda_1 \frac{D}{Dt}\right) \rho b, \tag{11}$$

$$\therefore divS = \nabla .S \,. \tag{12}$$

So,

$$\left(\rho \frac{d\overline{V}}{dt} + \nabla p\right) \left(1 + \lambda_1 \frac{D}{Dt}\right) = \left(1 + \lambda_1 \frac{D}{Dt}\right) \nabla S + \left(1 + \lambda_1 \frac{D}{Dt}\right) \rho b,$$
(13)

The body fore defined in the above equation represents the Lorentz force which can be expressed as, 151

$$b^{i} = \sigma \left[\overline{V} \times \overline{B} \right] \times \overline{B} . \tag{14}$$

As flow is the x – direction and B_0 is the strength of uniform constant magnetic field that applied in 152 y – direction, therefore we have, 153

$$\overline{B} = (0, B_0, 0). \tag{15}$$

Thus

$$\overline{V} \times \overline{B} = (0, 0, uB_0)$$

and

$$\left(\overline{V} \times \overline{B}\right) \times \overline{B} = \left(-uB_0^2, 0, 0\right). \tag{16}$$

Using Eq. (16) in Eq. (14) yields,

$$div\overline{V} = 0, b^i = (-\sigma u B_0^2, 0, 0).$$
 (17)

Using Eq. (17) in Eq. (13) and then expressed in component form,

x – component,

$$\left(\overline{u}\frac{\partial\overline{u}}{\partial\overline{x}}+\overline{v}\frac{\partial\overline{u}}{\partial\overline{y}}\right) = -\frac{1}{\rho}\frac{\partial p}{\partial\overline{x}} - \frac{\lambda_{1}}{\rho}\left(\overline{u}\frac{\partial^{2}p}{\partial\overline{x}^{2}}+\overline{v}\frac{\partial^{2}p}{\partial\overline{x}\partial\overline{y}} - \frac{\partial\overline{u}}{\partial\overline{x}}\frac{\partial p}{\partial\overline{x}} - \frac{\partial\overline{u}}{\partial\overline{y}}\frac{\partial p}{\partial\overline{y}}\right) + v\left(\frac{\partial^{2}\overline{u}}{\partial\overline{x}^{2}}+\frac{\partial^{2}\overline{u}}{\partial\overline{y}^{2}}\right) - \lambda_{1}\left(\overline{u}^{2}\frac{\partial^{2}\overline{u}}{\partial\overline{x}^{2}}+2\overline{u}\overline{v}\frac{\partial^{2}\overline{u}}{\partial\overline{x}\partial\overline{y}}+\overline{v}^{2}\frac{\partial^{2}\overline{u}}{\partial\overline{y}^{2}}\right) - \sigma uB_{0}^{2} + \lambda_{1}\left(-\sigma B_{0}^{2}v\frac{\partial u}{\partial\overline{y}}\right), \tag{18}$$

y – component,

$$\left(\overline{u}\frac{\partial\overline{v}}{\partial\overline{x}}+\overline{v}\frac{\partial\overline{v}}{\partial\overline{y}}\right) = -\frac{1}{\rho}\frac{\partial p}{\partial\overline{y}} - \frac{\lambda_{1}}{\rho}\left(\overline{v}\frac{\partial^{2}p}{\partial\overline{y}^{2}}+\overline{u}\frac{\partial^{2}p}{\partial\overline{x}\partial\overline{y}} - \frac{\partial\overline{v}}{\partial\overline{x}}\frac{\partial p}{\partial\overline{x}} - \frac{\partial\overline{v}}{\partial\overline{y}}\frac{\partial p}{\partial\overline{y}}\right) + v\left(\frac{\partial^{2}\overline{v}}{\partial\overline{x}^{2}} + \frac{\partial^{2}\overline{v}}{\partial\overline{y}^{2}}\right) - \lambda_{1}\left(\overline{u}^{2}\frac{\partial^{2}\overline{v}}{\partial\overline{x}^{2}} + \overline{2u}\overline{v}\frac{\partial^{2}\overline{v}}{\partial\overline{x}\partial\overline{y}} + \overline{v}^{2}\frac{\partial^{2}\overline{v}}{\partial\overline{y}^{2}}\right) + \lambda_{1}\left(\sigma B^{2}{}_{0}u\frac{\partial v}{\partial\overline{x}}\right). \tag{19}$$

The boundary conditions discussed by Javed and Ghaffari [10] are given below in the present flow 160 problem are, 161

$$\overline{u} = \overline{cx}, \ \overline{v} = 0, \quad \text{at} \quad \overline{y} = 0 \\ \overline{u} = a\overline{x} + b\overline{y}, \quad \text{as} \quad \overline{y} \to \infty,$$
 (20)

Eqs. (19) and (20) reduced by using boundary layer approximation as follows,

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$$\left(\overline{u} \frac{\partial \overline{u}}{\partial \overline{x}} + \overline{v} \frac{\partial \overline{u}}{\partial \overline{y}} \right) = -\frac{1}{\rho} \frac{\partial p}{\partial \overline{x}} - \frac{\lambda_1}{\rho} \left(\overline{u} \frac{\partial^2 p}{\partial \overline{x}^2} + \overline{v} \frac{\partial^2 p}{\partial \overline{x} \partial \overline{y}} - \frac{\partial \overline{u}}{\partial \overline{x}} \frac{\partial p}{\partial \overline{x}} - \frac{\partial \overline{u}}{\partial \overline{y}} \frac{\partial p}{\partial \overline{y}} \right) + v \left(\frac{\partial^2 \overline{u}}{\partial \overline{x}^2} + \frac{\partial^2 \overline{u}}{\partial \overline{y}^2} \right) - \lambda_1 \left(\overline{u}^2 \frac{\partial^2 \overline{u}}{\partial \overline{x}^2} + 2\overline{u}\overline{v} \frac{\partial^2 \overline{u}}{\partial \overline{x} \partial \overline{y}} + \overline{v}^2 \frac{\partial^2 \overline{u}}{\partial \overline{y}^2} \right) + \frac{\sigma B_0^2}{\rho} \left(-u - \lambda_1 v \frac{\partial u}{\partial \overline{y}} \right).$$
(21)

To get the simulation of the modeled governing equations one need to transform the governing 163 equations by using appropriate similarity transformation given as, 164

$$\overline{x} = x \sqrt{\frac{v}{c}}, \quad \overline{y} = y \sqrt{\frac{v}{c}}, \quad \overline{u} = u \sqrt{cv}, \quad \overline{v} = v \sqrt{cv}, \\ \overline{T} = T, \quad T_w = \Delta T + T_{\infty}, \quad p = \rho c v P \end{cases}$$
(22)

Eq. (21) in dimensionless from takes the form given as,

$$\left(u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y}\right) = -\frac{\partial P}{\partial x} + \beta \left(\frac{\partial u}{\partial y}\frac{\partial P}{\partial y}\right) + \left(\frac{\partial^2 u}{\partial y^2}\right) - \beta \left(u^2\frac{\partial^2 u}{\partial x^2} + 2uv\frac{\partial^2 u}{\partial x\partial y} + v^2\frac{\partial^2 u}{\partial y^2}\right) + M^2 \left(-u - \lambda_1 cv\frac{\partial u}{\partial y}\right).$$

$$(23)$$

Boundary conditions take the form given as,

u = x, v = 0 at y = 0, (24)

$$u = \frac{a}{c}x + \frac{b}{c}y, \quad \text{as} \quad y \to \infty.$$
 (25)

Now, for heat transfer analysis, assume that T_{∞} is the temperature of the fluid while the temperature 167 of the stretching surface is represented by T_{w} . By using the transformation given in Eq. (22) and Eq. 168 (4), Eq. (3) becomes, 169

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \frac{1}{Pr}\frac{\partial}{\partial y}\left(\left(1 + \frac{4}{3}Rd\left(\left(\theta_{w} - 1\right)T + 1\right)^{3}\right)\frac{\partial T}{\partial y}\right).$$
(26)

The boundary conditions become,

$$T = 1 \quad \text{at} \quad y = 0, \\ T = 0 \quad \text{as} \quad y \to \infty$$

$$(27)$$

where $\beta = \lambda_1 c$ is Deborah number which represents the fluidity of the material, $Pr = \mu c_p / k$ is 171 the Prandtl number, $M^2 = \sigma B_0^2 / \rho$ is the Hartmann number, $Rd = 4\sigma^* T_\infty^3 / k(\alpha_r + \sigma_s)$ and 172 $\theta_w = T_w / T_\infty$ represents the temperature of the surface same used by Ghaffari et al. (2016). The 173 stream function ψ that will be used in the governing equations, as shown below, 174

$$u = \frac{\partial \psi}{\partial y}$$
, $v = -\frac{\partial \psi}{\partial x}$. (28)

Using Eq. (28) in (23) to (27), one can have,

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$$\frac{\partial\psi}{\partial y}\frac{\partial^{2}\psi}{\partial x\partial y} - \frac{\partial\psi}{\partial x}\frac{\partial^{2}\psi}{\partial y^{2}} + \beta \left(\left(\frac{\partial\psi}{\partial y} \right)^{2} \frac{\partial^{3}\psi}{\partial y^{3}} - 2 \frac{\partial\psi}{\partial y}\frac{\partial\psi}{\partial x}\frac{\partial^{3}\psi}{\partial x\partial y^{2}} + \left(\frac{\partial\psi}{\partial x} \right)^{2} \frac{\partial^{3}\psi}{\partial x^{2}\partial y} \right) = -\frac{\partial P}{\partial x} + \beta \left(\frac{\partial^{2}\psi}{\partial y^{2}}\frac{\partial P}{\partial y} \right) + \left(\frac{\partial^{3}\psi}{\partial y^{3}} \right) + M^{2} \left(-\frac{\partial\psi}{\partial y} + \beta \frac{\partial\psi}{\partial x}\frac{\partial^{2}\psi}{\partial y^{2}} \right),$$
(29)

$$\left(\frac{\partial\psi}{\partial y}\frac{\partial T}{\partial x}-\frac{\partial\psi}{\partial x}\frac{\partial T}{\partial y}\right)=\frac{1}{Pr}\frac{\partial}{\partial y}\left(\left(1+\frac{4}{3}Rd\left(\left(\theta_{w}-1\right)T+1\right)^{3}\right)\frac{\partial T}{\partial y}\right),$$
(30)

$$\psi = 0, \quad \frac{\partial \psi}{\partial y} = x, \quad T = 1 \quad \text{at} \quad y = 0,$$

 $\psi = 0, \quad \frac{\partial \psi}{\partial y} = x, \quad T = 1 \quad \text{at} \quad y = 0 \quad ,$
(31)

$$\psi = \frac{a}{c}xy + \frac{1}{2}\gamma y, \quad T = 0 \quad \text{as} \quad y \to \infty.$$
 (32)

where $\gamma = b/c$ denotes shear in the free stream of the flow. Suppose the solution of Eqs. (29) and 176 (30) subject to boundary conditions Eq. (31) and (32) is of the form, 177

$$\psi = x\tilde{f}(y) + \tilde{g}(y), \quad T = \tilde{\theta}(y).$$
 (33)

The functions $\tilde{f}(y)$ and $\tilde{g}(y)$ are the oblique and normal elements of the streams. Using Eq. (33) 178 in Eqs. (29) to (32) we have, 179

$$\left(x\tilde{f}'(y) + \tilde{g}'(y) \right) \tilde{f}'(y) - \tilde{f}(y) \left(x\tilde{f}''(y) + \tilde{g}''(y) \right) + \beta \left(\left(\tilde{f}(y) \right)^2 \left(x\tilde{f}'''(y) + \tilde{g}''(y) \right) \right)$$

-2 $\tilde{f}(y) \left(x\tilde{f}'(y) + \tilde{g}'(y) \tilde{f}''(y) \right) = -\frac{\partial P}{\partial x} + \beta \left(x\tilde{f}''(y) + \tilde{g}''(y) \right) \frac{\partial P}{\partial y} + x\tilde{f}'''(y) + \tilde{g}'''(y)$
+ $M^2 \left(- \left(x\tilde{f}'(y) + \tilde{g}'(y) \right) + \beta \tilde{f}(y) \left(x\tilde{f}''(y) + \tilde{g}''(y) \right) \right),$ (34)

$$\frac{\partial}{\partial y} \left(\left(1 + \frac{4}{3} Rd \left(\left(\theta_{w} - 1 \right) \tilde{\theta} + 1 \right)^{3} \right) \tilde{\theta}^{'} \right) + Pr\tilde{f} \left(y \right) \tilde{\theta}^{'} = 0,$$
(35)

$$\tilde{f}(y) = 0, \quad \tilde{f}'(y) = 1, \quad \tilde{g}(y) = 0, \quad \tilde{g}'(y) = 0, \quad \tilde{\theta}(y) = 1 \quad \text{at} \quad y = 0,$$
 (36)

$$\tilde{f}'(y) = \frac{a}{c}, \quad \tilde{g}'(y) = \gamma y, \quad \tilde{\theta}(y) = 0, \quad \text{as} \quad y \to \infty.$$
 (37)
the pressure from Eq. (34), it takes the form as follows, 180

After eliminating the pressure from Eq. (34), it takes the form as follows,

$$\left(x\tilde{f}'(y) + \tilde{g}'(y)\right)\tilde{f}'(y) - \tilde{f}(y)\left(x\tilde{f}''(y) + \tilde{g}''(y)\right) + \beta\left(\left(\tilde{f}(y)\right)^{2}\left(x\tilde{f}''(y) + \tilde{g}''(y)\right) - 2\tilde{f}(y)\left(x\tilde{f}'(y) + \tilde{g}'(y)\tilde{f}''(y)\right)\right) = -A\gamma + x\left(\frac{a}{c}\right)^{2} + x\tilde{f}'''(y) + \tilde{g}'''(y) + M^{2}\left(\frac{a}{c}\right)x + M^{2}\left(-\left(x\tilde{f}'(y) + \tilde{g}'(y)\right) + \beta\tilde{f}(y)\left(x\tilde{f}''(y) + \tilde{g}''(y)\right)\right).$$
(38)

Now by comparing the coefficient as x^1 and x^0 in Eq. (38), one can have,

$$\tilde{f}^{"} + \left(\frac{a}{c}\right)^2 - \tilde{f}^{'2} + \tilde{f}\tilde{f}^{"} - \beta\left(\tilde{f}^2\tilde{f}^{"} - 2\tilde{f}\tilde{f}^{'}\tilde{f}^{"} - M^2\tilde{f}\tilde{f}^{"}\right) + \left(\frac{a}{c}\right)M^2 - M^2\tilde{f}^{'} = 0, \qquad (39)$$

$$\tilde{g}^{"} + \tilde{g}^{"}\tilde{f} - \tilde{g}^{'}\tilde{f}^{'} - \beta \Big(\tilde{f}^{2}\tilde{g}^{"} - 2\tilde{f}\tilde{g}^{'}\tilde{f}^{"} - M^{2}\tilde{g}^{"}\tilde{f}\Big) - M^{2}\tilde{g}^{'} = A\gamma,$$

$$\tag{40}$$

where boundary layer displacement is represented by A. Now for more simplification using a new variable is introduced which is defined as, 183

$$\tilde{g}'(y) = \gamma \tilde{h}(y). \tag{41}$$

Eq. (38) and the associated boundary condition are reduced to,

$$\tilde{h}^{"} + \tilde{h}^{'}\tilde{f} - \tilde{h}\tilde{f}^{'} - \beta \left(\tilde{f}^{2}\tilde{h}^{"} - 2\tilde{f}\tilde{h}\tilde{f}^{"} - M^{2}\tilde{h}^{'}\tilde{f}\right) - M^{2}\tilde{h} = A,$$

$$(42)$$

$$h(y) = 0$$
 at $y = 0$, (43)

$$\tilde{h}'(y) = 1 \quad \text{as} \quad y \to \infty.$$
 (44)

The local Nusselt number of physical quantities is defined below as,

$$Nu_{x} = \frac{\overline{x} \ q_{w}}{k \left(T_{w} - T_{\infty}\right)},\tag{45}$$

where,

$$q_{w} = -\left[\left(\frac{4}{3}\frac{4\sigma^{*}\overline{T}^{3}}{\left(\alpha_{r}+\sigma_{s}\right)}+k\right)\frac{\partial\overline{T}}{\partial\overline{y}}\right].$$
(46)

Using dimensionless variables and transformation given in Eq. (22) the above equation reduces to, 187

$$Nu_{x}\left(Re_{x}\right)^{\frac{-1}{2}} = -\left[\left(\frac{4}{3}Rd\left(\theta_{w}\right)^{3}+1\right)\tilde{\theta}^{'}\right].$$
(47)

It is worth mention here that limiting case for Newtonian case can be obtained by placing $\beta = 0$ and 188 case orthogonal stagnation point flow can also be obtained by placing $\gamma = 0$. 189

3. Numerical Solution

Using the boundary condition (36), (37), (43), and (44) in the non-linear equation of (35), (39), and 191 (42). They solve these equations in numerical with the parallel shooting method. The simple shooting 192 method is very easy in the compare of parallel shooting method, but the simple shooting method is 193 very difficult to solve higher non-linear problems. That way we used parallel shooting as presented 194 by Shi et al. (2021). The parallel method of shooting is well-organized. The technique is described 195 below: 196

Equations (35), (39) and (42) are reduced to the first order of differential equations by letting $\tilde{f} = f_1$ 197

$$h = f_4, \quad \tilde{h} = f_5, \quad \text{and} \quad \tilde{\theta} = f_6.$$
 198

$$f_{1}^{'} = f_{2}, f_{2}^{'} = f_{3},$$

$$f_{3}^{'} = \frac{1}{1 - \beta f_{1}^{2}} \left(f_{2}^{2} - \left(\frac{a}{c}\right)^{2} - f_{1} f_{3} - \beta \left(2\beta f_{1} f_{2} f_{3} + M^{2} f_{1} f_{3}\right) - \left(\frac{a}{c}\right) M^{2} + M^{2} f_{2} \right),$$
(47)

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$$f_{4}' = f_{5},$$

$$f_{5}' = \frac{1}{1 - \beta f_{1}^{2}} \Big(-f_{1} f_{5} - \beta \Big(2f_{1} f_{3} f_{4} + \sigma B_{0}^{2} f_{1} f_{5} \Big) + \sigma B_{0}^{2} f_{4} + A \Big),$$

$$f_{6}' = f_{7},$$
(48)

$$f_{7}' = \frac{1}{1 + \frac{4}{3}Rd\left(1 + \left(\theta_{w} - 1\right)f_{6}\right)^{3}} \left(\left(-4Rd\left(\theta_{w} - 1\right)\left(1 + \left(\theta_{w} - 1\right)f_{6}\right)^{2}\right)\left(f_{7}\right)^{2} - Prf_{1}f_{7}\right).$$
(49)

The boundary conditions are given below,

$$f_1(0) = 0, f_2(0) = 1, f_2(y_{\infty}) = \frac{a}{c},$$
(50)

$$f_4(0) = 0, f_5(y_{\infty}) = 1.$$
 (51)

The considered domain from 0 to y_{∞} is divided into the 'n' number of intervals where 'n' 200 depends strictly on the required convergence of the solution. The problem is solved for the first in-201 terval by setting suitable initial guess and the obtained solution is considered as an initial guess for 202 next interval and this process is carried out until the solution for the last interval is obtained. The 203 solution for each interval is obtained such that it satisfies the boundary condition at y_{∞} . The algo-204 rithm is self-developed in MATLAB R2015a. 205

4. Validation

To present the accuracy of our present computed results the comparison of f'(0) and h(0) has 207 been made with Pop [32] and Javed and Ghaffari [10] which includes the results for Newtonian and 208 non-Newtonian Maxwell fluid given in Table (1). It is found that our present computed results are 209 highly convergent with Pop [32] and Javed and Ghaffari [10] It is clear from the table that the value of 210 f''(0) is increases as we enhance the value of a/c but h'(0) increases at a certain value and then 211 decreased. 212

5. Results and Discussion

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Eqs. (35), (39) and (42) with appropriate conditions given in Eqs. (36), (37), (43) and (44) have been 214 solved by implementing above mentioned scheme for various values of involved parameters 215 β , a/c, γ and M. Figures (2a) to (2d) are plotted to present the variation of horizontal velocity u216 for various values of velocities ratio a/c with fixed values of x, β , M, $\gamma = 0.0, 0.5, 1.0$ and 5.0 217 It is seen that the velocity u increase with enhancement of γ . The Figure (2a) represents the or-218 thogonal flow i.e., $\gamma = 1.0$, whereas Figure (2b) to (2d) shows the non-orthogonal stagnation point 219 flow ($\gamma \neq 0$). It is observed from the figures that there exist two boundary layer structures which 220 depend upon the ratio of straining and stretching velocities. It is seen that when a/c > 1 the flow has 221 normal boundary layer structure but when a/c < 1 then the structure shows inverted behavior which 222

206

is same as reported by Javed and Ghaffari [10]. It is also noted that the thickness of boundary layer 223 decreases as we increase the value of a/c. It is also seen that there exists no boundary layer when 224 a/c = 1 its means that viscous effects near the boundary vanishes when both shearing and straining 225 velocities are equal. This behavior is same for both orthogonal and non-orthogonal stagnation point 226 flows. The Figures (2a) to (2d) show that velocity increases as there is an increase in value of γ . 227 Figure (3a) and (3b) is plotted to examine the variational effects of Deborah number β for or-228 thogonal flow ($\gamma = 0$) and non-orthogonal flow ($\gamma = 1.0$) with a fixed value of M on horizontal 229 velocity u. It is seen that by increasing the value of β figures show that for the inverted boundary 230 layer, the horizontal velocity decreases and thickness of boundary layer decrease but for normal 231 boundary layer the velocity increases and thickness increases for both $\gamma = 0$ and $\gamma = 1$. Figures (4a) 232 and (4b) shows the variational effects of magnetic field on the orthogonal stagnation point flow and 233 non-orthogonal point flow respectively for fixed values of β . It is clear from the figures that by 234 enhancing the magnetic field the horizontal velocity decreases, but the boundary layer becomes 235 thinner for an inverted boundary and for the normal boundary layer, the horizontal velocity u in-236 creases and the boundary layer thickness decreases. The Deborah number (De) is a dimensionless 237 number, often used in rheology to characterize the fluidity of materials under specific flow condi-238 tions. It quantifies the observation that given enough time even a solid-like material might flow, or a 239 fluid-like material can act solid when it is deformed rapidly enough. 240

Figure (5) shows that the horizontal velocity decreased when the value of β is enhanced by keeping 241 the other parameters fixed. The enhancement in the strength of the applied magnetic field dominates 242 the electromagnetic forces in comparison to the viscous forces which retards the motion of the flow. 243 Therefore, successive decrement in the magnitude of axial velocity in the center of the channel is 244 addressed by incrementing the value of magnetic parameter M, whereas one can see the counter 245 behavior of the fluid's velocity near the boundary. Figure (6) is designed to examine the effects of 246 varying M on horizontal velocity for fixed values of $\gamma, a/c$ and β . Same behavior is observed 247 as that was in the case of effects of β but a minor decrease is observed for M = 1 and 2. Figures 248 (7a) and (7b) shows the streamlines for oblique flow for a/c = 0.5 (dashed lines) and 5.0 (solid 249 lines) with fixed $\beta = 4, M = 2.0$ and $\gamma = 0.2$ and 2.0, It is seen that by increasing stretching 250 velocity the streamlines symmetry of the flow disturbs and lines get more tilted towards left due to 251 increase in straining velocity for $\gamma = 2.0$ but there is no tilted behavior is seen for $\gamma = 0.2$ and flow 252 becomes symmetric. 253

Figure (8a) and (8b) shows streamlines for oblique flow, for $\gamma = -10$ and -30 (dashed lines) and 10 254 and 30 (solid lines) with fixed $\beta = 4$, M = 2.0 nd a/c = 0.5. It is seen that by increasing the value 255 of $|\gamma|$ results in more obliqueness consequently causes the disturbance in the symmetry of the flow. 256

Figure (9) is plotted to represent the effects of θ_w for various values of θ_w with fixed values of 257 β , M, γ , a/c, Pr and Rd. It is seen that the temperature of fluid increases rapidly by increasing 258 the value of surface temperature. A concave curve is seen at $\theta_w = 2.0$. Figure (10) is designed to 259 elaborate the effects of Prandal number with fixed values of $\beta = 0.2, M = 1.0, \gamma = 5.0, a/c = 0.2,$ 260 Rd = 2.0 and $\theta_w = 2.0$. It is observed from the figure that the enhancement in the Prandtl number 261 results in a decrease in the value of temperature of flow. This figure demonstrates that the increase of 262 Prandtl number which consequently decreases of thermal conductivity that results in decrease of 263 temperature distribution which tend to zero as the space variable η increase from the wall and hence 264 thermal boundary layer thickness decreases as Prandtl number Pr increases. Near the boundary the 265 thermal boundary layer thickness is higher. Figure (11) shows the effects of radiation parameter Rd, 266 with fixed values of $\beta = 0.2, M = 1.0, \gamma = 5.0, a/c = 2.0, Pr = 0.05$ and $\theta_w = 2.0$ It is observed 267 the by increasing the values of Rd the temperature of flow increases; also, concave curves are ob-268 served for Rd = 5 and 10. 269

6. Closing Remarks

The stretching surface is surrounded by a small band of static fluid layer known as the boundary 271 layer. How quickly fluids and energy are transferred from the surface to the surrounding fluid de-272 pends on the thickness of the boundary layer. The amount of heat, energy, and fluid that a layer re-273 leases into the system can be decreased by a thick boundary layer. The influence of Hartmann number 274 and radiation parameter on the boundary layer flow of Maxwell fluid in the region of oblique stag-275 nation point over linear symmetrically stretching sheet is investigated. The participation of the in-276 volved parameters is studied by plotting their different variation through graphs and tables. This 277 study concludes increase in the parameter a/c decreases the boundary layer thick of oblique 278 stagnation point flow of non-Newtonian fluid while radiation parameter and surface heating param-279 eter increase the thermal boundary layer thickness. By increasing the value of Deborah number for 280 inverted boundary layer, the horizontal velocity decreases, and thickness of boundary layer de-281 creases. It is also noted that enhancing the strength of magnetic field, the horizontal velocity de-282 creases but boundary layer becomes thinner. Streamlines shows that increasing the value of $|\gamma|$ 283 results in more obliqueness. Temperature of fluid increases rapidly by increasing the value of surface 284 temperature and radiation parameter but decreases by increasing the Prandtl number. The boundary 285 layer flow of oblique stagnation point flow disturbs the symmetry of the flow. 286

Nomenclature:

- μ Absorption coefficient
- *E* Activation energy

 T_{∞} Ambient temperature

A Boundary layer displacement

b	Body forces	k	Boltzmann constant
<i>x</i> , <i>y</i>	Cartesian coordinates	σ	Chemical rate constant
β	Deborah number	μ	Dynamic viscosity
ρ	Density of fluid	θ	Dimensionless temperature
С	Dimensional constant	T_{∞}	Fluid temperature
\overline{A}_1	First tensor by Rivlin Ericksen	а	Fluid velocity
М	Hartmann number	V	Kinematic viscosity
∇^2	Laplacian operator	В	Magnetic field vector
$\tilde{g}(y)$	Normal element of the streams	Nu_x	Nusselt number
$\tilde{f}(y)$	Oblique element of the streams	Pr	Prandtl number
Р	Pressure of fluid	Rd	Radiation parameter
α_r	Roseland definition	q_r	Radiative heat flux
$\sigma_{_s}$	Scattering coefficient	Ψ	Stream function
S_{c}	Schmidt number	$oldsymbol{eta}_0$	Strength of magnetic field
γ	Shear in the free stream of the flow	\overline{S}	Stress tensor
η	Similarity variable	С	Stretching constant
C_p	Steady pressure of real heat	T_w	Stretching surface temperature
σ^*	Stefan Boltzmann's-constant	$U_{_{W}}$	Stretching velocity of sheet
δ	Temperature relative parameter	φ	Thermal stratification parameter
к	Thermal conductivity	$\overline{\lambda_1}$,	Time relaxation content
α	Thermal diffusivity	$\overline{L}^{{ \scriptscriptstyle T}}$	Transpose of velocity gradient
\overline{L}	Velocity gradient	u,v	Velocity components
\overline{V}	Velocity vector	T_w	Wall temperature
$ heta_{_w}$	Wall temperature	λ	Weissenberg number

	Newtonian Fluid ($\beta = 0.0$)				Non-Newtonian Fluid ($\beta = 0.2$)			
		Javed			Javed		Javed	
	Pop	and	Present	Pop	and	Present	and	Present
	[32]	Ghaffari	Results	(2004)	Ghaffari	Results	Ghaffari	Results
		[10]			[10]		[10]	
a/c	<i>f</i> "(0)	<i>f</i> "(0)	<i>f</i> "(0)	<i>f</i> "(0)	<i>f</i> "(0)	<i>f</i> "(0)	h'(0)	h'(0)
0.01	-0.9981	-0.99802	-0.9980	-1.0499	-1.05009	-1.0500	-0.51368	-0.5137
0.02	-0.9958	-0.99579	-0.9957	-10476	-1.04778	-1.0477	-0.24667	-0.2467
0.05	-0.9876	-0.98758	-0.9875	-1.0393	-1.03939	-1.0394	0.07239	0.0724
0.10	-0.9694	-0.96939	-0.9693	-1.0207	-1.02082	-1.0208	0.28154	0.2815
0.20	-0.9181	-0.91811	-0.9181	-0.96823	-0.96823	-0.9683	0.49218	0.4922
0.50	-0.6673	-0.66726	-0.6672	-0.70779	-0.70779	-0.7077	0.79610	0.7961
1.00	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	1.0000	1.0000
2.00	2.0175	2.01749	2.0175	2.2225	2.22314	2.2231	1.09213	1.0921
3.00	4.7294	4.72824	4.7294	5.3544	5.35217	5.3522	0.78434	0.7843
5.00	11.7537	11.75190	11.7534	14.0144	17.00169	17.0017	-2.04649	-2.0465
10.0	36.2689	36.25704	36.2699	48.3354	48.33540	48.3354	-2.34185	-2.3419

Table 1: Numerical values of f''(0) and h'(0) for the different values of β and a/c



Figure 1: Geometry of the considered physical plane

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Figure 2. Graph of variation of horizontal velocity u along y-axis at x = 1 for various values of a/c and $\beta = 0.4$ and M = 2.0 with (a) $\gamma = 0.0$ (b) $\gamma = 0.5$ (c) $\gamma = 1.0$ (d) $\gamma = 5.0$



Figure 3. Graph of variation of horizontal velocity u along y-axis at x = 1 for various values of β and a/c = 0.1, 0.5, 1.0 and 1.5 and M = 2.0 with (a) $\gamma = 0.0$ (orthogonal flow) (b)



 $\gamma = 1.0$ (non-orthogonal flow)

Figure 4. Graph of variation of horizontal velocity u along y-axis at x=1 for various values of

M when a/c = 0.1, 0.5, 1.0 and 1.5 and $\beta = 0.5$ with (a) $\gamma = 0.0$ (orthogonal flow) (b)

 $\gamma = 1.0$ (non-orthogonal flow)







Figure 6. Graph of variation of horizontal velocity *u* along *y*-axis at x=1 for various values of *M* with fixed a/c=0.2 and $\beta=0.5$ for $\lambda=1.0$ (non-orthogonal flow)



Figure 7. Graph of streamlines for oblique flow, for a/c = 0.5 (dashed lines) and 5.0 (solid lines) with fixed $\beta = 4, M = 2.0$ with (a) $\gamma = 0.2$ and (b) $\gamma = 2.0$



Figure 8. Graph of streamlines for oblique flow, for fixed $\beta = 4, M = 2.0$ and a/c = 0.5 with (a) $\gamma = -10$ (dashed lines) and 10 (solid lines) and (b) $\gamma = -30$ (dashed lines) and 30 (solid lines)



Figure 9. Graph of variation of θ for various values of θ_w with fixed $\beta = 0.2, M = 1.0$,

$$\gamma = 5.0, a/c = 2.0, Rd = 2.0, Pr = 0.05$$
 and $Rd = 2.0$



Figure 10. Graph of variation of θ for various values of Pr with fixed $\beta = 0.2, M = 1.0$, $\gamma = 5.0, a/c = 2.0, Rd = 2.0, Rd = 2.0$ and $\theta_w = 2.0$



Figure 11. Graph of variation of θ for various values of Rd with fixed $\beta = 0.2, M = 1.0, \gamma = 5.0, a/c = 2.0, Pr = 0.05$ and $\theta_w = 2.0$

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Biography

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During the period 2014-2018, Dr. Bilal joined the International Islamic University Islamabad (PAK) to teach405courses related to mathematics and Allama Iqbal Open University, Islamabad (AIOU, PAK) to teach courses406related to Physics, where he worked as a visiting faculty member. In 2017, Dr. Bilal was selected as a Senior407Research Assistant in the National Research Program for the University (NRPU) by Higher Education of Paki-408stan (HEC, PAK) for the project entitled "Study of Mixed Convection Flows Inside a Lid Driven Cavity Using409Finite Element Method "and producing some the outstanding research articles.410

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"Sadia Kanwal has established a robust academic foundation, having successfully 434 attained both her Bachelor of Science (BS) and Master of Philosophy (M.Phil) 435 degrees in Mathematics from the University of Lahore, situated in Sargodha, 436 Pakistan. Her academic journey has been marked by a dedicated focus on the 437 intricate domain of Fluid Mechanics, delving into its complexities and nuances. 438 Furthermore, her scholarly pursuits have extended into exploring alternative 439 theories on peristalsis—an area of significant interest within the realm of biological 440 fluid dynamics. Kanwal's profound curiosity and commitment to these subjects 441 signify a passion for uncovering new perspectives and advancing understanding 442 within these specialized fields of study. Her academic trajectory showcases a 443 commitment to academic excellence and a genuine enthusiasm for probing the 444 boundaries of mathematical theory within the realm of fluid dynamics and 445 biological processes." 446