

1 **An effective dispersive liquid-liquid microextraction method**
2 **for pharmaceutical extraction: Optimization via central**
3 **composite design**

4
5 Zahra Nadi, Ahmad Rahbar-Kelishami^{*}, Hadi Shayesteh

6
7
8
9 *Corresponding author

10 ahmadrahbar@iust.ac.ir

11 Research Lab for Advanced Separation Processes, Faculty of Chemical, Petroleum and Gas
12 Engineering, Iran University of Science and Technology (IUST), Narmak, Tehran, Iran

13 Tel/Fax: +98 21 77451505; Mobile number: +989126405942

14

15 **Zahra Nadi**

16 Email: z.nadi.iust95@gmail.com

17

18 **Hadi Shayesteh**

19 Email: hadi_shayesteh@chemeng.iust.ac.ir

20

21

22

23 **Abstract**

24 In this study, a simple and efficient dispersive liquid-liquid microextraction procedure (DLLME)
25 was developed to remove diclofenac sodium (DF) from water samples. Various parameters such
26 as diclofenac concentration in aqueous phase (10-50 mg/L), process time (2-10 min), extraction
27 solvent concentration (0.005-0.025 M), and centrifuge speed (1000-5000 rpm) were investigated.
28 The experimental design was performed by the Response Surface Methodology (RSM)
29 according to the central composite design to reduce the number of experiments and determine the
30 optimal extraction conditions. The effect of the single and simultaneous operational parameters
31 was evaluated. In this regard, the extraction concentration of 0.01 M, the initial diclofenac
32 concentration in aqueous phase 20 mg/L, the rotation speed of the centrifuge 4000 rpm, and the
33 residence time of 8 min were obtained as the optimum operating conditions. According to the
34 other studies and available findings, the ratio of two-phase organic and aqueous discharges
35 (Q_{org}/Q_{aq}) was set to 1:9. The diclofenac extraction from the aqueous phase was 77.91% in
36 optimum operating conditions.

37

38 **Keywords:** Dispersive Liquid-liquid microextraction; Solvent extraction; Diclofenac; Response
39 Surface Methodology.

40

41

42

43

44 **1. Introduction**

45 Diclofenac sodium is a non-steroidal anti-inflammatory medicine that has been used in humans
46 since the 1970s. By blocking the effect of the enzyme cyclooxygenase, this drug reduces the
47 production of a prostaglandin chemical in the body, responsible for causing pain and
48 inflammation in the affected area [1–5]. In present days, one of the most crucial environmental
49 problems is the emerging contaminant from the pharmaceutical industry, hospitals, and home
50 drains in aquatic environments because of their persistence and potentially harmful effects on
51 any form of aquatic life. Diclofenac accumulates in edible fruits and vegetables, having a direct
52 effect on human health. Additionally, several research on the toxicity of diclofenac on birds,
53 mammals, aquatic species, and plants have been published [6–10].

54 The sample preparation phase is an extremely important part of the analysis process. In this step,
55 a desired component will be extracted from purified and concentrated. There are a variety of
56 preparation methods available, each with its own advantages in terms of speed and ease [11].
57 The selection of each technique is dependent on the analyte conditions, both physical and
58 chemical [12–17]. Liquid-Liquid extraction has long been one of the most common methods of
59 separating contaminants. The long process time, high solvent and extraction solvent
60 consumption, the possibility of emulsion formation, and the need for intense mixing have made
61 the use of this method difficult. To address the limitations of liquid-liquid extraction, liquid-
62 phase microextraction methods (LPME) have been developed.

63 LPMEs may be classified into four broad categories: (a) single drop microextraction (SDME);
64 (b) continuous flow microextraction (CFME); (c) hollow fiber liquid-phase microextraction (HF-
65 LPME); and (d) dispersive liquid-liquid microextraction (DLLME). These are different in how
66 the solvent contacts the aqueous phase [18–27].

67 In this research, a dispersive liquid-liquid microextraction method has been applied to separate
68 the diclofenac from an aqueous solution. DLLME system consists of three components: water is
69 a common part (aqueous sample), and about the other two components, one of them is insoluble
70 in water (extraction solvent), and the other one is soluble in the other two components
71 (dispersive solvent).

72 DLLME protocols are typically composed of the following steps: an extraction solvent is
73 combined with a dispersive solvent, and the solvent mixture is then quickly injected into an
74 aqueous sample. An aqueous sample is rapidly injected with an extraction-dispersive solvent
75 mixture, resulting in the formation of a cloudy solution composed of microdroplets of extraction
76 solvent scattered throughout the sample. Cloudy solution production allows for the immediate
77 partitioning of analytes from the aqueous sample into the extraction phase, which is
78 advantageous in some cases (a major advantage of this technique). Using centrifugation, the hazy
79 solution is separated into two phases, allowing for the simple recovery of the extraction solvent
80 for subsequent examination of the results [28]. This method, for its very simple texture, is well
81 compatible with most instrumental methods. For example, in gas chromatography, liquid
82 chromatography, Ultraviolet-visible spectrometry, and flame atomic absorption spectrometry,
83 the organic solvent can be inducted directly into the analysis instrument [29,30].

84

85 **2. Materials and methods**

86 **2.1. Material**

87 Diclofenac sodium (Sodium 2-[2-[(2,6dichlorophenyl)amino]acetate, $C_{14}H_{10}Cl_2NNaO_2$), a white
88 powder with more than 98% purity, was supplied by Sigma-Aldrich (Steinheim, Germany)

89 (Table 1). n-Butanol as an organic solvent and Tetra-n-butylammonium bromide (TBAB) was
90 provided by Merck Co.(Germany). TBAB is added to the solvent phase, and its cationic form is
91 complexed with the anionic form of the diclofenac. In the dispersive liquid-liquid
92 microextraction, the extraction solvent was selected from solvents that, in addition to being
93 insoluble in water and having a higher density than water, could extract the desired compound
94 [30,31]. Also, the base of the dispersive solvent is its solubility in both the aqueous phase of the
95 sample and the organic phase of the extractor. Due to the physical and chemical properties,
96 TBAB was selected as the dispersive solvent with the highest recycling rate.

97

98 **2.2. Instrumental**

99 The ultraviolet-visible (UV-vis spectrophotometry (Shimadzu UV-1800, Japan)) method was
100 applied to measure and determine the concentration of diclofenac in the aqueous sample.
101 Centrifuged (EBA 20-Hettich, Germany) was used to centrifuge the sample. In order to measure
102 and control the pH during the experiments related to this research, a pH meter (PL-700PV
103 model, Taiwan) was used.

104

105 **2.3. Procedure**

106 n-Butanol as an extraction solvent and TBAB as a dispersive solvent were considered. We
107 experimented with the preconcentration of diclofenac according to the dispersive liquid-liquid
108 microextraction method. The influential factors such as diclofenac concentration in aqueous
109 phase (10-50 mg/L), process time (2-10 min), extraction solvent concentration (0.005-0.025 M),
110 and centrifuge speed (1000-5000 rpm) were also considered for the focus of determining optimal
111 values. During the process, diclofenac concentrations in the aqueous phase ranged from 10 to 50

112 mg/L with a constant 1:9 ratio of organic to aqueous phases including butanol and at 1000 to
113 5000 rpm were evaluated at various times. The calibration curve of diclofenac was prepared
114 based on 1, 5, 10, 15, 20, 30, and 40 mg/L concentrations. 5 mL of each sample was taken and
115 analyzed by spectrometry (Fig. 1(a)). In general, the maximum absorption of diclofenac occurs at
116 275 nm wavelength. By linear fitting of the points obtained from the visible-ultraviolet
117 spectrometry analysis, the calibration curve with the coefficient of determination close to 1 ($R^2=$
118 0.998) was obtained (Fig. 1(b)). Using this line equation, the concentration of diclofenac in
119 unknown samples can be calculated.

120

121 The extraction efficiency (EE (%)) was used for determining the mass transfer performance, and
122 the Eq. (1) can be used for the calculation of EE%.

$$EE(\%) = \frac{C_{aq,in} - C_{aq,out}}{C_{aq,in}} \times 100 \quad (1)$$

123 $C_{aq,in}$ $C_{aq,out}$ (mg/L) are input concentration and output concentration, respectively.

124 Response surface approach based on the central composite design was used to optimize the
125 independent factors that influenced the process efficiency in the evaluation of extraction
126 efficiency in the dispersive liquid-liquid microextraction method. Independent variables, namely
127 diclofenac concentration in aqueous phase (A), process time (B), extraction solvent
128 concentration (C), and centrifuge speed (D), were selected in five levels with three replicable
129 center points. The selected ranges and levels of each factor are shown in Table 2. Also, 27 tests
130 as per the central composite design (CCD) to evaluate the effect of variables and optimize them
131 for diclofenac extraction were performed, as shown in Table 3 [32,33].

132

133

134

135 **3. Results and discussion**

136 **3.1. The pH effect**

137 The effect of solution pH on the rate of diclofenac extraction from the aqueous phase by
138 extractor with a concentration of 0.01 M, diclofenac concentration in 20 mg/L, the rotation speed
139 of the centrifuge 3000 rpm, and the residence time of 6 min have been investigated as a single
140 factor, which is shown in Fig. 2. As can be observed in Fig. 2, the pH of the diclofenac samples
141 was adjusted by using NaOH or HNO₃ solutions. The extraction efficiency is reduced by
142 decreasing the pH to less than 4. Given that the ionization constant of diclofenac is 4.16,
143 diclofenac is protonated at a pH less than 4.16, resulting in an acidic form, which is reduced to
144 form complexes with TBAB. As pH increased, the ionized form of diclofenac increased, which
145 resulted in an increase in complex formation, so extraction efficiency increased. The decreases in
146 extraction efficiency at alkaline pH can be attributable to OH and diclofenac ions competing with
147 one another for bonds with extractant molecules [34]. In all experiments performed, the aqueous
148 phase pH was set to 5 because the maximum extraction rate was obtained at pH 5.

149

150 **3.2. Statistical design**

151 After performing experiments with the surface response method, the concentration of the
152 aqueous phase after each experiment was analyzed to calculate the extraction efficiency of
153 diclofenac. As a function of factors independent of the process used for diclofenac extraction by
154 liquid-liquid microextraction method, a quadratic polynomial model is derived as Eq. (2):

$$EE(\%) = +36.38 -11.94A +2.79B +2.10C +4.50D -7.53AC -10.65AD +2.18BD -11.31CD +1.96A^2 +0.0828B^2 +3.10C^2 \quad (2)$$

155 According to Eq. (2), E indicates the percentage of diclofenac extracted; A, B, C, and D also
156 represent the diclofenac concentration in aqueous phase, process time, extraction solvent
157 concentration, and centrifuge speed the extraction, respectively. Also, the laboratory values for
158 diclofenac extraction efficiency obtained by Eq. (1) and predicted by Eq. (2) were summarized in
159 Table 4. A maximum laboratory value (80.88) and predicted value (78.81) for diclofenac
160 extraction efficiency can be found in run7, which includes diclofenac concentration in aqueous
161 phase 20 mg/L, process time 8 minutes, extraction solvent concentration 0.02 M, centrifuge
162 speed 4000 rpm.

163 An analysis of variance (ANOVA) was carried out to determine the impact of process variables
164 on diclofenac extraction efficiency, and the results are listed in Table 5. The values of F and p for
165 each factor are expressed. The analysis considers the 95% confidence interval, so each factor's p-
166 value indicates the significance or insignificance of that factor in the model [35]. In accordance
167 with the analysis of variance, the p-value for the selected model for diclofenac extraction is less
168 than 0.05; it indicates that the chosen model is statistically significant. In contrast, the value of
169 the model coefficient for the fitted model was 0.9751. The values of the adjusted coefficient of
170 determination and the predicted coefficient of determination were 0.9461 and 0.8590,
171 respectively, which shows that the selected model is able to cover laboratory data relatively well
172 [36]. Also, based on Fig.3, there is a good correlation between the predicted and laboratory
173 values of extraction efficiency, respectively.

174

175

176 **3.3. Interaction of operational parameters on diclofenac extraction**

177 In order to investigate the interaction of variables, contour plots and three-dimensional diagrams
178 of the effect of parameters on the efficiency of diclofenac extraction by DLLME were drawn by
179 changing the values of two parameters and maintaining the other parameter constant. As shown
180 in Fig. 4(a), the extraction efficiency has increased with increasing time and decreasing the feed
181 phase's initial concentration. In fact, initial increase in extraction time promotes the solute
182 transfer, thereby increasing the extraction performance. Experiments by many previous
183 researchers indicated that the emulsion breakage increases with increase in extraction time due to
184 gradual increase of swelling [37–39]. In Fig. 4(b), as the concentration of the extraction solvent
185 increases, the extraction efficiency of diclofenac increases more than the concentration of the
186 aqueous phase. Also, the extraction efficiency has increased by increasing the extraction
187 concentration and decreasing the feed phase's initial concentration. This can be due to the
188 organic phase being saturated with a diclofenac complex. Initially, at low concentrations of the
189 feed phase, the transfer of diclofenac depends on the activity of the extraction, but at high
190 concentrations, the activity coefficient is due to the colombian interaction between anion and
191 cation. Due to the increase in ionic strength, it leads to low salt activity and thus reduces
192 extraction [40]. Fig. 4(c) shows that the effect of centrifuge rotation speed on diclofenac
193 extraction efficiency is greater than the initial diclofenac concentration in aqueous phase. Also,
194 the extraction efficiency has increased by increasing the centrifuge's rotation speed and
195 decreasing the initial concentration of the feed phase. In fact, an increase in mixing speed would
196 increase interfacial area and the mass transfer coefficient, thereby increasing overall enrichment
197 and extraction [41]. Fig. 5(a) shows that the effects of both factors on diclofenac extraction
198 efficiency are very close to each other. Also, with increase the extraction concentration and

199 increasing the extraction time, the extraction efficiency has increased. According to Fig. 5(b),
200 the effect of both factors on diclofenac extraction efficiency is relatively similar. Also, the
201 extraction efficiency has increased with increasing the centrifuge's rotation speed and increasing
202 the extraction time. Finally, in Fig. 5(c), it is apparent that the extraction efficiency increases
203 with increasing the extractor concentration and centrifuge rotation speed.

204

205 **3.3. Determination of the values of the parameters in the optimum state**

206 After investigating the effect of process variables on diclofenac extraction in the organic solvent,
207 these variables' values can be obtained in the optimal state to achieve maximum efficiency. For
208 this purpose, the optimization part of Design-Expert software was used. The diclofenac
209 extraction process's optimal conditions were included 20 mg/L initial concentration of the
210 aqueous phase, 0.01 M extraction concentration, the centrifuge rotation speed of 4000 rpm, and
211 residence time of 8 min (Table 6). The extraction percentage of diclofenac is predicted to be
212 78.78% based on these values. Under optimal conditions, the extraction percentage was 77.91%,
213 which indicates that the fitted model is accurate.

214

215

216 **4. Conclusion**

217 In this study, the DLLME method was successfully applied to the extraction of diclofenac from
218 aqueous samples. The effect of parameters such as initial aqueous phase concentration, extractor
219 concentration, centrifuge rotation speed, and residence time under test design and pH at the
220 optimum point as a single factor was investigated. An analysis of variance was performed to
221 determine whether operational parameters affected the rate of diclofenac extraction. A quadratic

222 mathematical model with a reliability coefficient of 0.975 was developed to predict the amount
223 of diclofenac extraction from the aqueous phase by dispersive-liquid-liquid microextraction.
224 Based on the results, 0.01 M extraction concentration, 20 mg/L initial aqueous phase
225 concentration, 4000 rpm centrifugation speed, 8-minute residence time, and pH 5 were
226 determined to be the optimal conditions for the extraction. Under these conditions, the extraction
227 efficiency was 77.91%. Since diclofenac effluents create environmental issues, the micro-
228 aqueous organic system may be a viable solution due to the smaller organic phase than aqueous
229 extraction, as well as the quick extraction time.

230

231 **References**

- 232 1. Ansarimehr, M., Rahbar kelishami, A., and Shayesteh, H., “Evaluation of flow patterns
233 maps of diclofenac sodium solvent extraction in microfluidic systems based on
234 dimensionless numbers”, *J. Appl. Res. chemistry* (2022).
- 235 2. Xie, J., Liu, M., He, M., Liu, Y., Li, J., Yu, F., Lv, Y., Lin, C., and Ye, X., “Ultra-efficient
236 adsorption of diclofenac sodium on fish-scale biochar functionalized with H₃PO₄ via
237 synergistic mechanisms”, *Environ. Pollut.*, p. 121226 (2023).
- 238 3. Shayesteh, H., Nodehi, R., and Rahbar-Kelishami, A., “Trimethylamine functionalized
239 clay for highly efficient removal of diclofenac from contaminated water: Experiments and
240 theoretical calculations”, *Surfaces and Interfaces*, **20**, p. 100615 (2020).
- 241 4. de Azevedo, C. F., Machado, F. M., de Souza, N. F., Silveira, L. L., Lima, E. C.,
242 Andrezza, R., and Bergamnn, C. P., “Comprehensive adsorption and spectroscopic
243 studies on the interaction of carbon nanotubes with diclofenac anti-inflammatory”, *Chem.*
244 *Eng. J.*, **454**, p. 140102 (2023).
- 245 5. Zhang, M., Wang, W., Zhang, Q., and Deng, S., “Pore surface engineering of covalent
246 organic frameworks by simultaneously appending amine group and tailoring pore size for
247 efficient adsorption of diclofenac sodium”, *Chem. Eng. J.*, **459**, p. 141561 (2023).
- 248 6. Sathishkumar, P., Meena, R. A. A., Palanisami, T., Ashokkumar, V., Palvannan, T., and
249 Gu, F. L., “Occurrence, interactive effects and ecological risk of diclofenac in
250 environmental compartments and biota - a review”, *Sci. Total Environ.*, **698**, p. 134057
251 (2020).
- 252 7. Vieno, N. and Sillanpää, M., “Fate of diclofenac in municipal wastewater treatment plant -
253 A review”, *Environ. Int.*, **69**, pp. 28–39 (2014).
- 254 8. Zhao, Y., Liu, F., and Qin, X., “Adsorption of diclofenac onto goethite: Adsorption
255 kinetics and effects of pH”, *Chemosphere*, **180**, pp. 373–378 (2017).
- 256 9. Zhou, L., Dai, S., Xu, S., She, Y., Li, Y., Leveneur, S., and Qin, Y., “Piezoelectric effect
257 synergistically enhances the performance of Ti₃₂-oxo-cluster/BaTiO₃/CuS p-n

- heterojunction photocatalytic degradation of pollutants”, *Appl. Catal. B Environ.*, **291**(February), p. 120019 (2021).
10. Areeb, A., Yousaf, T., Murtaza, M., Zahra, M., Zafar, M. I., and Waseem, A., “Green photocatalyst Cu/NiO doped zirconia for the removal of environmental pollutants”, *Mater. Today Commun.*, **28**, p. 102678 (2021).
11. Alcantara, G. K. S., Calixto, L. A., Rocha, B. A., Júnior, F. B., de Oliveira, A. R. M., and de Gaitani, C. M., “A fast DLLME-LC-MS/MS method for risperidone and its metabolite 9-hydroxyrisperidone determination in plasma samples for therapeutic drug monitoring of patients”, *Microchem. J.*, **156**, p. 104894 (2020).
12. Mohammadi, M., Khosravi, S., Nili-Ahmadabadi, A., Kamalabadi, M., Ghasemzadeh-Mohammadi, V., and Afkhami, A., “Rapid determination of ampyra in urine samples using dispersive liquid-liquid microextraction coupled with ion mobility spectrometry”, *J. Pharm. Biomed. Anal.*, **224**, p. 115185 (2023).
13. Perisic, D. J., Gilja, V., Stankov, M. N., Katancic, Z., Kusic, H., Stangar, U. L., Dionysiou, D. D., and Bozic, A. L., “Removal of diclofenac from water by zeolite-assisted advanced oxidation processes”, *J. Photochem. Photobiol. A Chem.*, **321**, pp. 238–247 (2016).
14. Davarnejad, R. and Sabzehei, M., “Sodium diclofenac removal from a pharmaceutical wastewater by electro-Fenton process”, *Sep. Sci. Technol.*, **54**(14), pp. 2294–2303 (2019).
15. Oral, O. and Kantar, C., “Diclofenac removal by pyrite-Fenton process: Performance in batch and fixed-bed continuous flow systems”, *Sci. Total Environ.*, **664**, pp. 817–823 (2019).
16. Cantarella, M., Carroccio, S. C., Dattilo, S., Avolio, R., Castaldo, R., Puglisi, C., and Privitera, V., “Molecularly imprinted polymer for selective adsorption of diclofenac from contaminated water”, *Chem. Eng. J.*, **367**, pp. 180–188 (2019).
17. Ali, I., Alharbi, O. M. L., AlOthman, Z. A., Alwarthan, A., and Al-Mohaimed, A. M., “Preparation of a carboxymethylcellulose-iron composite for uptake of atorvastatin in water”, *Int. J. Biol. Macromol.*, **132**, pp. 244–253 (2019).
18. Xu, S., Zhu, Q., Xu, S., Yuan, M., Lin, X., Lin, W., Qin, Y., and Li, Y., “The phase behavior of n-ethylpyridinium tetrafluoroborate and sodium-based salts ATPS and its application in 2-chlorophenol extraction”, *Chinese J. Chem. Eng.*, **33**, pp. 76–82 (2021).
19. Yamini, Y., Rezazadeh, M., and Seidi, S., “Liquid-phase microextraction – The different principles and configurations”, *TrAC - Trends Anal. Chem.*, **112**, pp. 264–272 (2019).
20. Reinsdorf, M. and Triplett, J. E., “A Review of Reviews”, *Price Index Concepts Meas.*, **149**, pp. 17–84 (2013).
21. Sarafraz-Yazdi, A. and Amiri, A., “Liquid-phase microextraction”, *TrAC Trends Anal. Chem.*, **29**(1), pp. 1–14 (2010).
22. Liu, H. and Dasgupta, P. K., “Analytical chemistry in a drop”, *TrAC - Trends Anal. Chem.*, **15**(9), pp. 468–475 (1996).
23. Arthur, C. L. and Pawliszyn, J., “Solid Phase Microextraction with Thermal Desorption Using Fused Silica Optical Fibers”, *Anal. Chem.*, **62**(19), pp. 2145–2148 (1990).
24. Dadfarnia, S. and Haji Shabani, A. M., “Recent development in liquid phase microextraction for determination of trace level concentration of metals-A review”, *Anal. Chim. Acta*, **658**(2), pp. 107–119 (2010).
25. Lee, J., Lee, H. K., Rasmussen, K. E., and Pedersen-Bjergaard, S., “Environmental and bioanalytical applications of hollow fiber membrane liquid-phase microextraction: A

- review”, *Anal. Chim. Acta*, **624**(2), pp. 253–268 (2008).
- 305 26. Pinto, M. I., Sontag, G., Bernardino, R. J., and Noronha, J. P., “Pesticides in water and the
306 performance of the liquid-phase microextraction based techniques. A review”,
307 *Microchem. J.*, **96**(2), pp. 225–237 (2010).
- 308 27. Guo, J., Xu, S., Qin, Y., Li, Y., Lin, X., He, C., and Dai, S., “The temperature influence
309 on the phase behavior of ionic liquid based aqueous two-phase systems and its extraction
310 efficiency of 2-chlorophenol”, *Fluid Phase Equilib.*, **506**, p. 112394 (2020).
- 311 28. Quigley, A., Cummins, W., and Connolly, D., “Dispersive liquid-liquid microextraction in
312 the analysis of milk and dairy products: A review”, *J. Chem.*, **2016** (2016).
- 313 29. Albert-García, J. R., Icardo, M. C., and Calatayud, J. M., “Analytical strategy
314 photodegradation/chemiluminescence/continuous-flow multicommutation methodology
315 for the determination of the herbicide Propanil”, *Talanta*, **69**(3), pp. 608–614 (2006).
- 316 30. Farahani, H., Norouzi, P., Dinarvand, R., and Ganjali, M. R., “Development of dispersive
317 liquid-liquid microextraction combined with gas chromatography-mass spectrometry as a
318 simple, rapid and highly sensitive method for the determination of phthalate esters in
319 water samples”, *J. Chromatogr. A*, **1172**(2), pp. 105–112 (2007).
- 320 31. Maia, G. S., de Andrade, J. R., da Silva, M. G. C., and Vieira, M. G. A., “Adsorption of
321 diclofenac sodium onto commercial organoclay: Kinetic, equilibrium and thermodynamic
322 study”, *Powder Technol.*, **345**, pp. 140–150 (2019).
- 323 32. Jalilvand, P., Rahbar-Kelishami, A., Mohammadi, T., and Shayesteh, H., “Optimizing of
324 malachite green extraction from aqueous solutions using hydrophilic and hydrophobic
325 nanoparticles”, *J. Mol. Liq.*, **308**, p. 113014 (2020).
- 326 33. Heidari, B. S., Oliaei, E., Shayesteh, H., Davachi, S. M., Hejazi, I., Seyfi, J., Bahrami, M.,
327 and Rashedi, H., “Simulation of mechanical behavior and optimization of simulated
328 injection molding process for PLA based antibacterial composite and nanocomposite bone
329 screws using central composite design”, *J. Mech. Behav. Biomed. Mater.*, **65**, pp. 160–176
330 (2017).
- 331 34. Sampath U. Gunathilake, T. M., Ching, Y. C., Chuah, C. H., Rahman, N. A., and Nai-
332 Shang, L., “pH-responsive poly(lactic acid)/sodium carboxymethyl cellulose film for
333 enhanced delivery of curcumin in vitro”, *J. Drug Deliv. Sci. Technol.*, **58**, p. 101787
334 (2020).
- 335 35. Shayesteh, H., Norouzbeigi, R., and Rahbar-Kelishami, A., “Hydrothermal facile
336 fabrication of superhydrophobic magnetic nanopiky nickel wires: Optimization via
337 statistical design”, *Surfaces and Interfaces*, **26**, p. 101315 (2021).
- 338 36. Farahani, A., Rahbar-Kelishami, A., and Shayesteh, H., “Microfluidic solvent extraction
339 of Cd(II) in parallel flow pattern: Optimization, ion exchange, and mass transfer study”,
340 *Sep. Purif. Technol.*, **258**(Ii), p. 118031 (2021).
- 341 37. Raji, M., Abolghasemi, H., Safdari, J., and Kargari, A., “Nanofluid-based emulsion liquid
342 membrane for selective extraction and separation of dysprosium”, *Int. J. Chem. Mol. Eng.*,
343 **11**(12), pp. 787–792 (2017).
- 344 38. Ahmad, A. L., Kusumastuti, A., Derek, C. J. C., and Ooi, B. S., “Emulsion liquid
345 membrane for heavy metal removal: An overview on emulsion stabilization and
346 destabilization”, *Chem. Eng. J.*, **171**(3), pp. 870–882 (2011).
- 347 39. Lende, A. B. and Kulkarni, P. S., “Selective recovery of tungsten from printed circuit
348 board recycling unit wastewater by using emulsion liquid membrane process”, *J. water
349 Process Eng.*, **8**, pp. 75–81 (2015).

- 350 40. Ghanbarian, B., Hunt, A. G., Ewing, R. P., and Sahimi, M., "Tortuosity in porous media: a
351 critical review", *Soil Sci. Soc. Am. J.*, **77**(5), pp. 1461–1477 (2013).
352 41. Kulkarni, P. S., Tiwari, K. K., and Mahajani, V. V., "Membrane stability and enrichment
353 of nickel in the liquid emulsion membrane process", *J. Chem. Technol. Biotechnol. Int.*
354 *Res. Process. Environ. Clean Technol.*, **75**(7), pp. 553–560 (2000).

355
356 **Zahra Nadi** was born in 1995, Tehran, Iran and spent primary, high school and higher
357 education in this city. She received her M.Sc. degree in Chemical Engineering from Iran
358 University of Science and Technology (IUST) in November 2020. Generally, her research
359 experiences include wastewater treatment and separation processes. she has been awarded
360 distinguished M.Sc. Excellent Student. Currently, she is working in a similar area focusing on
361 the evaluation of critical micelle concentration point behavior on the adsorptive removal of
362 pharmaceutical pollutant.

363
364 **Hadi Shayesteh** was born in 1991, Tehran, Iran and spent primary, high school and higher
365 education in this city. He received his Ph.D. degree in Chemical Engineering from Iran
366 University of Science and Technology (IUST) on September 2022. Generally, his research
367 experiences include synthesis of various nanoparticles with different process, wastewater
368 treatment, and surface wettability phenomena. During his Master's and Ph.D. degrees, he have
369 worked on several industrial and practical projects (wide range of preparation methods,
370 characterization techniques, and optimization), including superhydrophobic/superoleophilic
371 nanostructures, adsorption process, microfluidic systems, soil bioremediation, and liquid
372 membranes. He has been awarded distinguished M.Sc. Excellent Student and two times as
373 distinguished Ph.D. Researcher from IUST. He has published more than 35 ISI papers and 3 ISC
374 paper. Currently, he is working in a similar area focusing on synthesizing metal-organic
375 framework materials and their derived porous carbon nanocomposite.

376
377 **Ahmad Rahbar-Kelishami** was born in 1980, Tehran, Iran and spent primary, high school and
378 higher education in this city. He achieved his PhD at the University of Tehran and finished his
379 thesis in 2010. He has been an active faculty member at Iran's University of Science and
380 Technology (IUST), School of Chemical, Petroleum and Gas Engineering since 2019. His
381 specialty branches are liquid phase separation, and water/waste water treatment with a 25 H-
382 index according to Google scholar. He has published more than 70 ISI papers, 10 ISC papers,
383 and wrote and published one professional book in the field of chemical engineering. He has
384 engineering experience in oil, gas and energy plant design. At the moment, he directs and
385 supervises dissertation of 4 PhD and 10 M.A. students. He is an Associate Professor at the
386 School of Chemical Petroleum and Gas Engineering, Iran University of Science and Technology
387 (IUST), P.O. Box 16765-163 Tehran Iran.

388
389 **Figure captions**

390 Fig. 1. (a) Visible spectrum – ultraviolet of diclofenac sodium at the various concentration (1-50
391 mg/L) and (b) diclofenac sodium calibration curve.

392 Fig. 2. The effect of feed phase pH on extraction efficiency.

393 Fig. 3. Correlation between predicted and laboratory values of extraction efficiency.

394 Fig. 4. The response levels simultaneously interaction between initial diclofenac concentration in
395 aqueous phase (a) process time, (b) solvent concentration, and (c) centrifuge speed on the DF
396 extraction.

397 Fig. 5. The response levels simultaneously interaction between (a) process time and solvent
398 concentration, (b) process time and centrifuge speed, and (c) solvent concentration and
399 centrifuge speed on the DF extraction.

400

401

402

403 **Table captions**

404 Table 1. Physical and chemical properties of diclofenac sodium.

405 Table 2. The selected ranges and levels in diclofenac extraction efficiency.

406 Table 3. Central composite design.

407 Table 4. Calculated and predicted results of diclofenac extraction efficiency.

408 Table 5. analysis of variance for diclofenac liquid-liquid microextraction.

409 Table 6. Optimal values of parameters and percentage of predicted and experimental extraction.

410

411

412

413

414

415

416

417

418

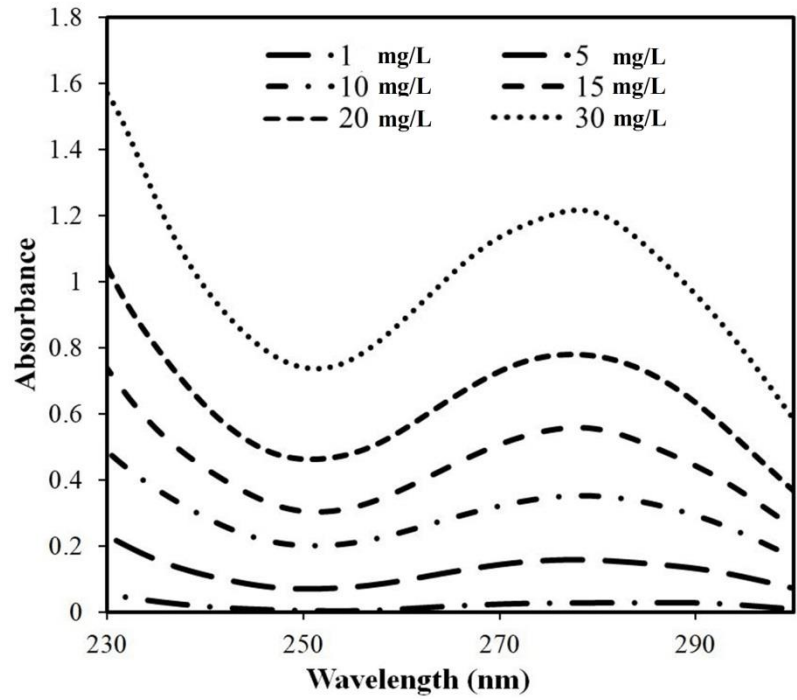
419

420 Fig. 1. (a) Visible spectrum – ultraviolet of diclofenac sodium at the various concentration (1-50

421 mg/L) and (b) diclofenac sodium calibration curve.

422

(a)



(b)

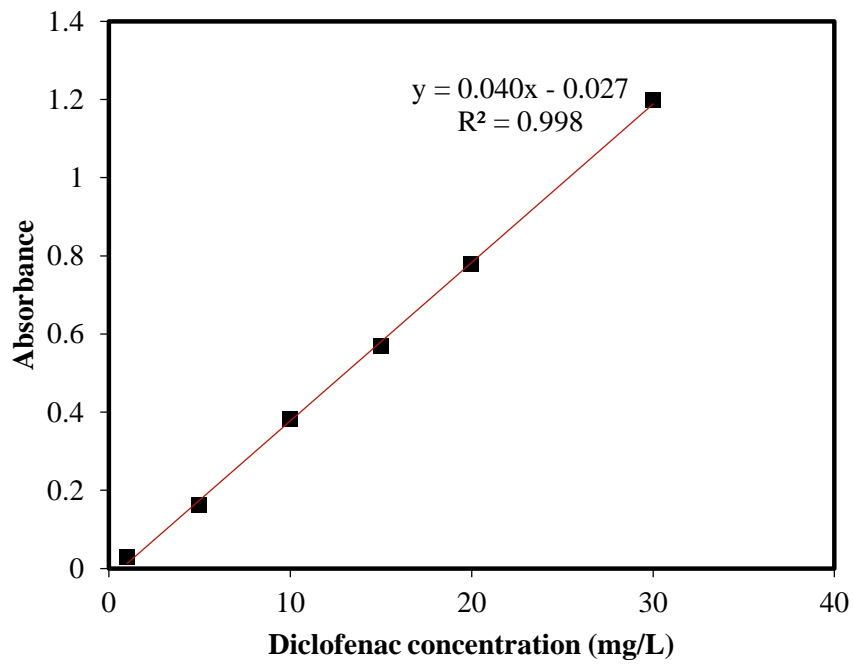
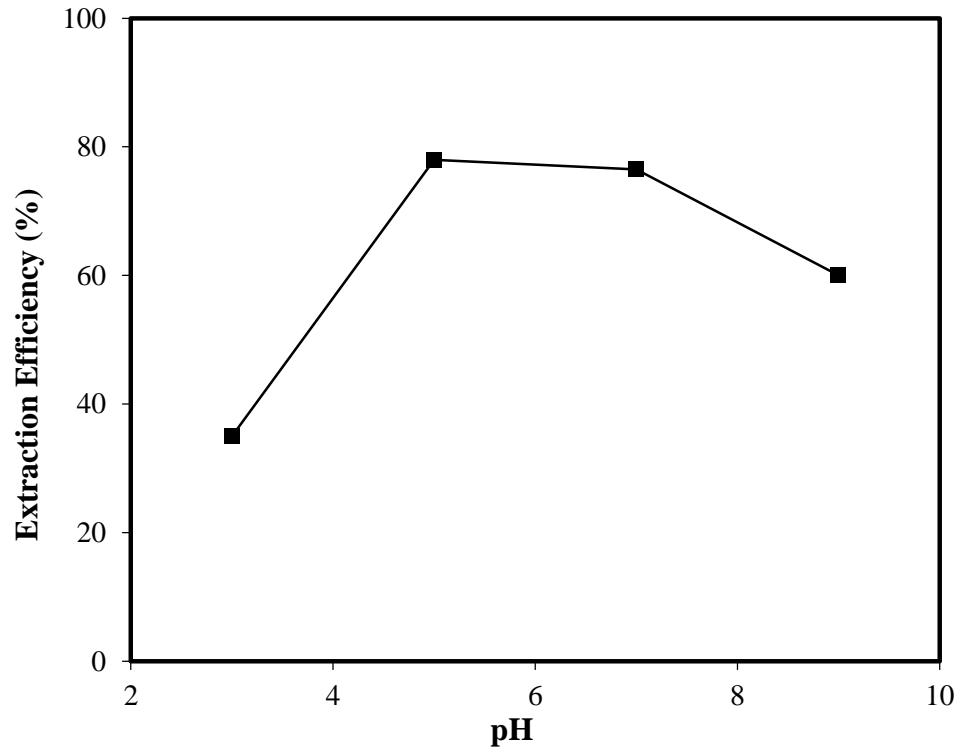


Fig. 2. The effect of feed phase pH on extraction efficiency.



424

425

426

427

428

429

430

431

432

433

434

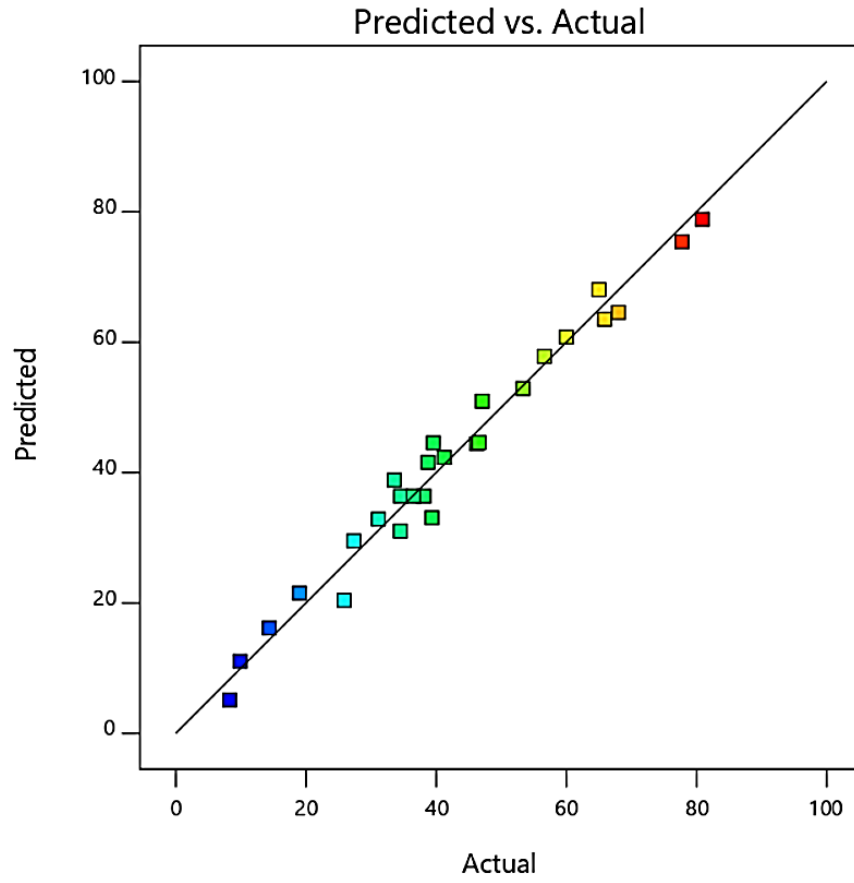
435

436

437

438

Fig. 3. Correlation between predicted and laboratory values of extraction efficiency.



439

440

441

442

443

444

445

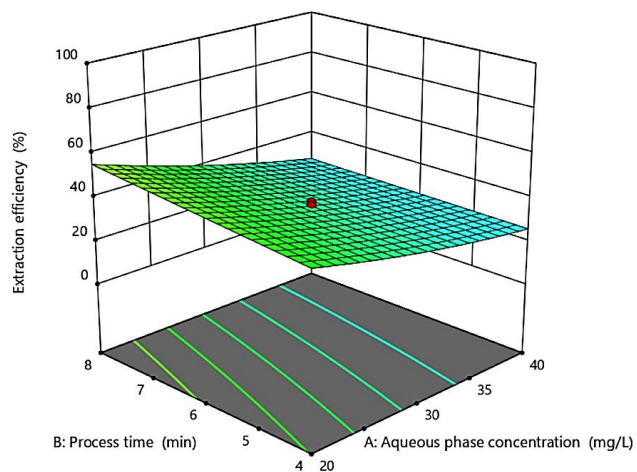
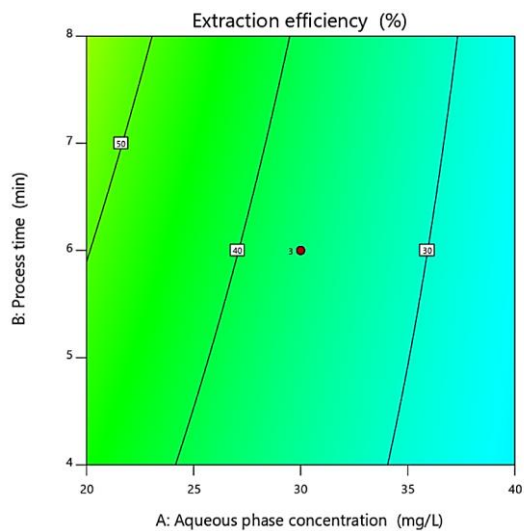
446

447

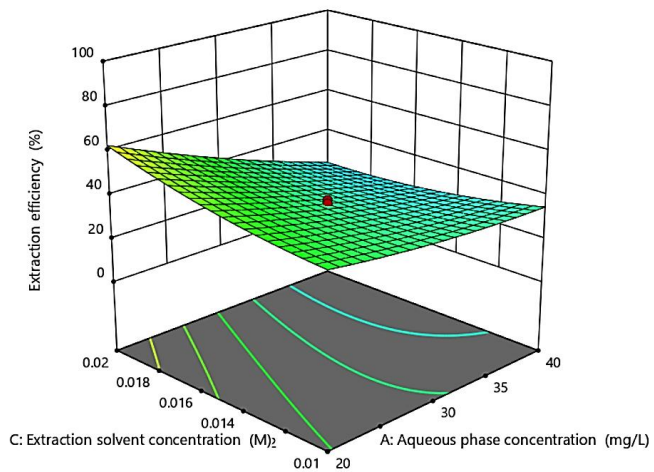
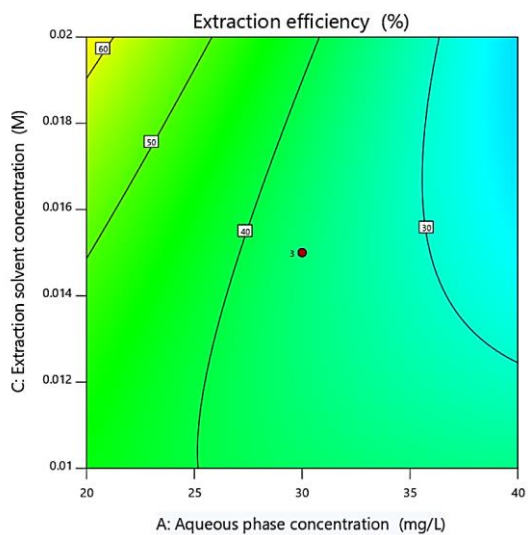
448

449 Fig. 4. The response levels simultaneously interaction between initial diclofenac concentration in
 450 aqueous phase (a) process time, (b) solvent concentration, and (c) centrifuge speed on the DF
 451 extraction.

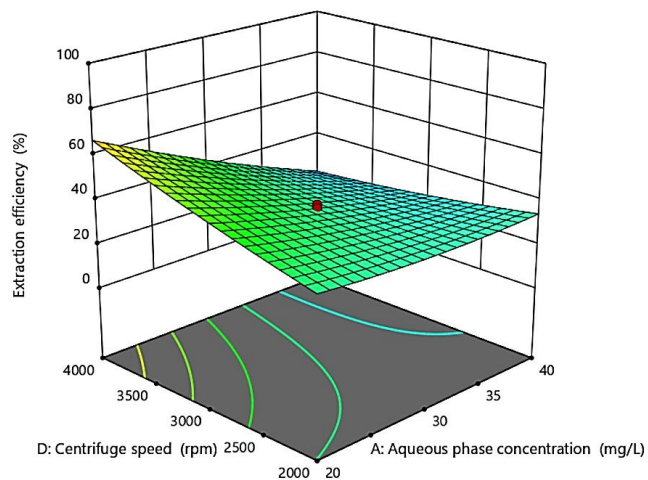
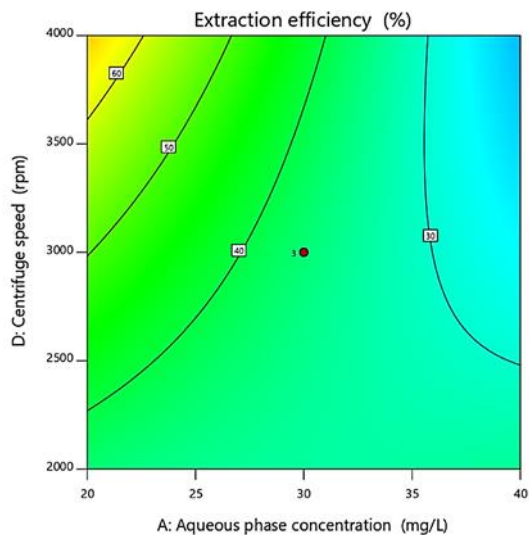
(a)



(b)



(c)



452

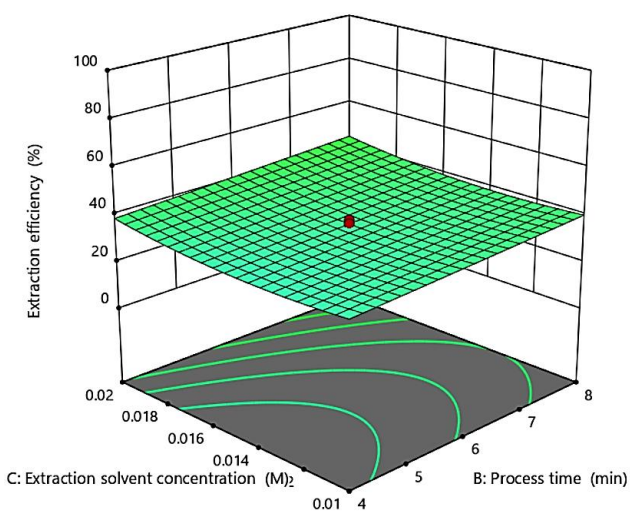
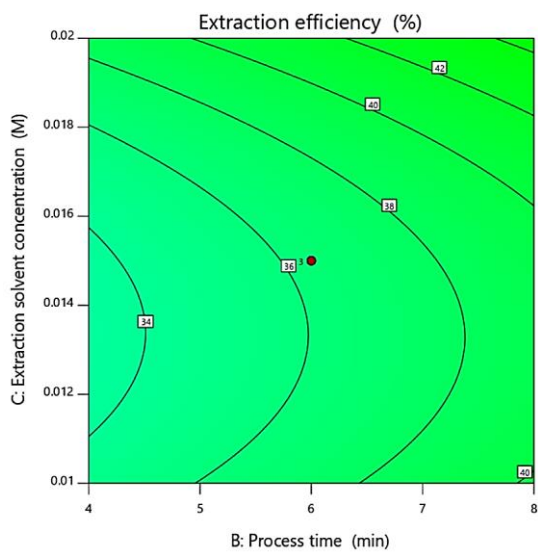
453

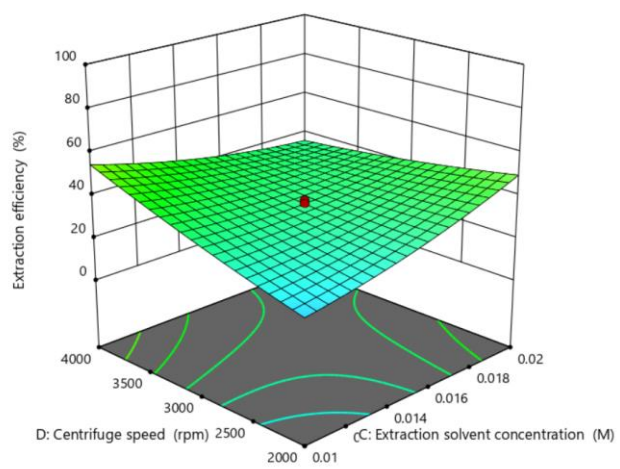
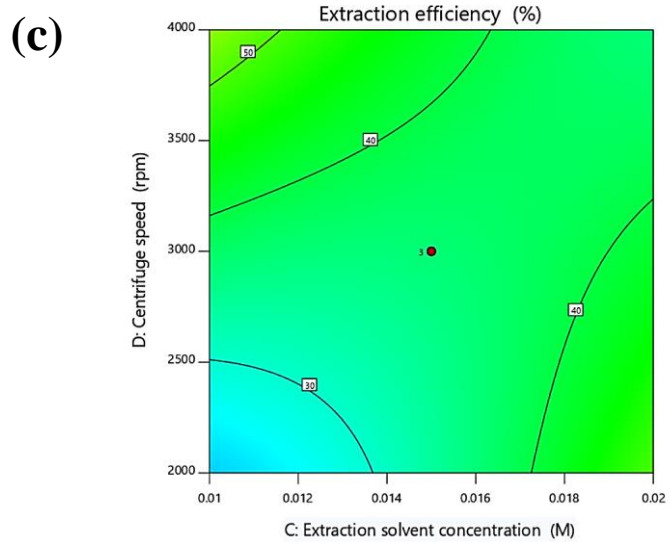
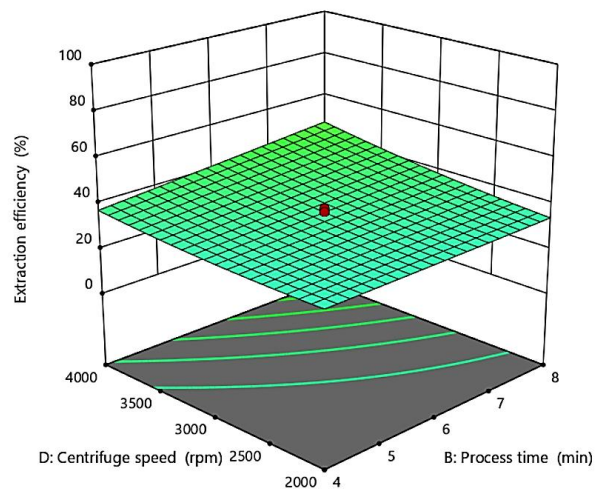
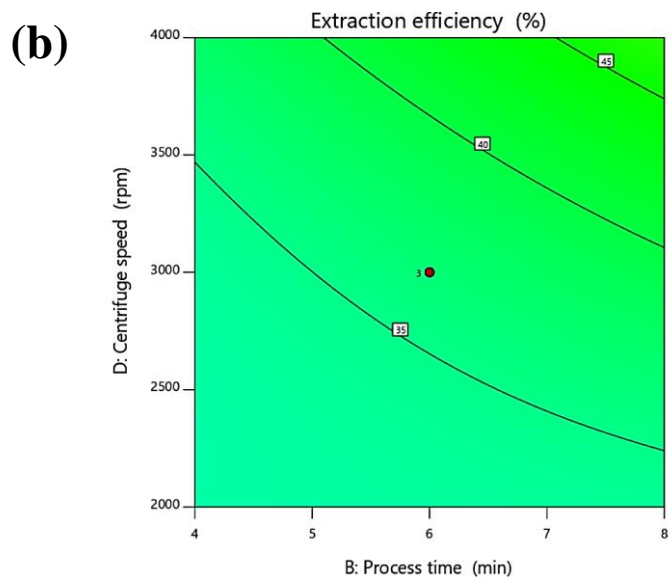
454 Fig. 5. The response levels simultaneously interaction between (a) process time and solvent

455 concentration, (b) process time and centrifuge speed, and (c) solvent concentration and centrifuge

456 speed on the DF extraction.

(a)





457

458

459

460

461

462

463

464

Table 3. Central composite design.

Run	Diclofenac concentration in aqueous phase (mg/L)	Process time (min)	Extraction solvent concentration (mg/L)	Centrifuge speed (rpm)
1	10	6	0.015	3000
2	40	4	0.01	2000
3	30	2	0.015	3000
4	20	8	0.02	4000
5	30	6	0.025	3000
6	40	8	0.02	2000
7	40	4	0.02	2000
8	40	4	0.02	4000
9	40	8	0.01	4000
10	20	8	0.02	2000
11	50	6	0.015	3000
12	20	8	0.01	2000
13	40	8	0.01	2000
14	20	4	0.01	2000
15	20	4	0.02	2000
16	20	4	0.01	4000
17	30	6	0.005	3000
18	30	6	0.015	3000
19	40	4	0.01	4000
20	20	4	0.02	4000
21	30	10	0.015	3000
22	30	6	0.015	3000
23	40	8	0.02	4000
24	30	6	0.015	5000
25	20	8	0.01	4000
26	30	6	0.015	3000
27	30	6	0.015	1000

473

474

475

476

477

478

479

Table 4. Calculated and predicted results of diclofenac extraction efficiency.

Run	Variables				Extraction efficiency (%)	
	A	B	C	D	Experimental	Predict
1	10	6	0.015	3000	68.096	64.86
2	40	4	0.01	2000	31.13	32.87
3	30	2	0.015	3000	34.50	31.16
4	20	8	0.02	4000	77.75	75.52
5	30	6	0.025	3000	53.33	53.03
6	40	8	0.02	2000	38.76	41.61
7	40	4	0.02	2000	39.75	44.55
8	40	4	0.02	4000	8.26	5.29
9	40	8	0.01	4000	46.24	44.47
10	20	8	0.02	2000	65.88	63.46
11	50	6	0.015	3000	25.87	20.39
12	20	8	0.01	2000	19.00	21.50
13	40	8	0.01	2000	27.39	29.77
14	20	4	0.01	2000	14.38	16.11
15	20	4	0.02	2000	56.63	57.92
16	20	4	0.01	4000	68.02	64.68
17	30	6	0.005	3000	46.58	44.63
18	30	6	0.015	3000	34.53	36.42
19	40	4	0.01	4000	33.49	38.84
20	20	4	0.02	4000	60.72	61.25
21	30	10	0.015	3000	41.24	42.33
22	30	6	0.015	3000	36.50	36.42
23	40	8	0.02	4000	9.87	11.07
24	30	6	0.015	5000	47.08	51.13
25	20	8	0.01	4000	80.88	78.81
26	30	6	0.015	3000	38.12	36.42
27	30	6	0.015	1000	39.38	33.09

481

482

483

484

485

486

487

488

489

Table 5. Analysis of variance for diclofenac liquid-liquid microextraction.

Source	Sum of Squares	df	Mean Square	F-value	p-value	
Model	14	9364.54	668.9	33.58	< 0.0001	significant
A-Feed	1	3409.36	3409.36	171.15	< 0.0001	
B-Time	1	191.08	191.08	9.59	0.0092	
C-TBAB	1	102.87	102.87	5.16	0.0423	
D-Speed	1	480.23	480.23	24.11	0.0004	
AB	1	75.6	75.6	3.8	0.0752	
AC	1	897.3	897.3	45.05	< 0.0001	
AD	1	1798.4	1798.4	90.28	< 0.0001	
BC	1	0.1208	0.1208	0.0061	0.9392	
BD	1	79.48	79.48	3.99	0.069	
CD	1	2064.79	2064.79	103.66	< 0.0001	
A ²	1	82.28	82.28	4.13	0.0649	
B ²	1	0.1166	0.1166	0.0059	0.9403	
C ²	1	204.27	204.27	10.25	0.0076	
D ²	1	42.3	42.3	2.12	0.1707	
Residual	12	239.04	19.92			
Lack of Fit	10	232.57	23.26	7.2	0.1281	not significant
Pure Error	2	6.46	3.23			
Cor Total	26	9603.57				

490 *df: Degree of freedom

491

492 Table 6. Optimal values of parameters and percentage of predicted and experimental extraction.

Operational parameters	The optimal amount	Units	
Extractor concentration	0.01	M	
The initial concentration of the aqueous phase	20	mg/L	
Centrifuge rotation speed	4000	rpm	
stay time	8	min	
	Predicted (%)	Experimental (%)	Error (%)
Extraction efficiency	78.78	77.91	1.12

493

494

495