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# Effect of HCl on the structure and catalytic activity of $Pt/Al_2O_3$ nanocatalyst prepared in microemulsion system

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#### **KEYWORDS**

Nanocatalyst; Pt nanoparticles; Microemulsion; Shape-controlled catalyst; Catalyst activity. Abstract. Nowadays, preparation of special and effective nanocatalysts is a hot research topic. Obviously, the size and structure of the active site of a catalyst plays a key role in catalytic activity. In this novel research, the Pt nanocatalyst supported on  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> was prepared in two different microemulsion systems to clarify the effect of microemulsion essence on catalyst character and activity. Two types of microemulsion systems were constructed from Triton X-100/2-butanol as surfactant and co-surfactant, i.e., *n*-heptane as organic phase and H<sub>2</sub>O + H<sub>2</sub>PtCl<sub>6</sub> (or HCl(aq) + H<sub>2</sub>PtCl<sub>6</sub>) as aqueous phase, to investigate the effect of HCl on the shape and structure of the prepared nanocatalysts. Shape, size, and size distribution of the Pt nanoparticles on the alumina were monitored by cyclic voltammetry and SEM analysis. Activity of the nanocatalysts was determined by reduction of *p*-nitrophenol as a reaction model.

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#### 1. Introduction

In recent years, the number of research studies in the field of catalysis has grown remarkably because of environmental and industrial needs, such as the need to remove air pollutants or the proposition of alternative energy sources. These studies aimed to investigate the influence of shape, size, size distribution, and composition of surface sites of the catalysts on their activity [1-3]. With the advent of nanotechnology and its application in catalytic reaction, the major step has been taken to design novel nanocatalysts [4-6]. The fabrication of metal nanoparticles with shape control and sizes

\*. Corresponding author. Tel.: +98 86 32627530; Fax: +98 86 34173406 E-mail addresses: a-salabat@araku.ac.ir (A. Salabat); a-keshavarz@phd.araku.ac.ir (A. Keshavarz). is critical for catalytic applications. This subject has been confirmed by investigating platinum nanoparticle morphology, prepared in the presence of different capping polymers on their catalytic properties [7].

Long et al. prepared polyhedral and nonpolyhedral Pt nanoparticles by a modified polyol method using  $AgNO_3$  as a structure-modifying agent [8]. In addition, they reported on a polyol method used for fabricating stabilized Pt nanoparticles (Pt NPs) as cubic and octahedral shapes [9]. In another research work, published recently by Arán-Ais et al. [10], preferentially oriented (100) Pt NPs were synthesized by different methodologies and studied electrochemically.

Cuenya et al. published a review on the role of nanoparticle size and shape in chemisorption and catalytic performance [11]. They discussed the effect of the nanoparticles' shape and atomic structures on catalytic performance. Martinez-Rodriguez et al. synthesized Pt NPs by microemulsion method at different HCl or  $H_2SO_4$  concentrations [12,13]. They confirmed that cubic Pt nanoparticles could be obtained in the presence of HCl or  $H_2SO_4$ . In addition, they reported that the optimal HCl percentage in the water phase should be about 25% to obtain the highest amount of cubic nanostructures [14].

Further to our research works [15-17] and other literature results, we are encouraged to fabricate, for the first time,  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalyst with controlling shape of Pt NPs dispersed on alumina using microemulsion systems. For this purpose, two different w/o microemulsion systems containing  $(H_2O + H_2PtCl_6)/n$ -heptane/Triton X-100/2butanol and  $(HCl(aq) + H_2PtCl_6)/n$ -heptane/Triton X-100/2-butanol were used to prepare  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts. The shape of the prepared Pt NPs in these two types of microemulsion systems was monitored electrochemically. Characterization of the synthesized nanocatalysts was also performed by XRD and SEM analysis. To determine catalytic activity of the nanocatalysts with different structures, reduction of p-NP over the prepared nanocatalysts was investigated.

### 2. Experimental procedures

#### 2.1. Materials

Hexachloroplatinic acid (H<sub>2</sub>PtCl<sub>6</sub>) (99%), *n*-heptane, 2-butanol, and *p*-nitrophenol (*p*-NP) were obtained from Merck Company and used as received. The nonionic surfactant poly(ethylene glycol) *p*-(1,1,3,3tetramethylbutyl)-phenyl ether (TX-100) with purity of 98% was purchased from Acros Company and used without further purification. Alumina ( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>) was obtained from Japan Aerosil with the surface area of 110 m<sup>2</sup>/g. All of the solutions were prepared by deionized water.

#### 2.2. Preparation of Pt colloidal system

A colloidal system of platinum nanoparticles was prepared using a w/o microemulsion composed of nheptane as oil phase, nonionic surfactant of TX-100, and co-surfactant of 2-butanol. Then, a suitable amount of 0.1 M aqueous solutions of  $H_2PtCl_6$ , prepared in pure water or aqueous 25% HCl, was added to a solution of *n*-heptane, TX-100, and 2-butanol to obtain microemulsion systems. Typical volume percentage of the microemulsion system includes 3%  $H_2$ PtCl<sub>6</sub> solution, 40.5% *n*-heptane, 16.5% TX-100, and 40% 2-butanol. The prepared microemulsion systems were stirred and settled down for 3 hours to equilibrate. Afterwards, the platinum precursor was reduced to the metallic Pt nanoparticles with the addition of NaBH4 to the microemulsion systems. In all experiments, the reducing agent  $(NaBH_4)$  to Pt molar ratio was kept at 10. The two different types of Pt colloidal systems (synthesized without and with HCl)

are now ready for characterization or precipitation on the support and for producing nanocatalyst samples.

#### 2.3. Fabrication of $Pt/\gamma$ - $Al_2O_3$ nanocatalysts

In order to prepare the nanocatalysts' samples, the support of catalyst  $(\gamma$ -Al<sub>2</sub>O<sub>3</sub>) was added to the platinum colloidal systems. Then, Pt nanoparticles were harvested from colloidal suspensions with the drop-wise addition of THF to precipitate platinum particles on the alumina support. Subsequently, the produced nanocatalysts of Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> were dried at room temperature for two days and, then, calcined at 600°C for 2 hours.

#### 2.4. Characterization of nanocatalysts

A Philips diffractometer with Cu K $\alpha$  radiation (Cu K $\alpha_1$ : 1.54056 Å, Cu K $\alpha_2$ : 1.54439 Å) was used to carry out X-ray diffraction (XRD) experiment on the produced nanocatalysts at room temperature. The  $2\theta$  angular region, with the step time of 0.02 s, between 20° and 80°, was considered.

To determine the size and size distribution of Pt NPs precipitated on alumina, the Scanning Electron Microscope (SEM) was applied using a MIRA3 TES-CAN instrument.

The electrochemical characterization, as Cyclic Voltammetry (CV), of the platinum nanoparticles was carried out in an electrochemical cell with three electrodes. An AUTOLAB system of 101 (Eco Chemie By, the Netherlands) was used to control the electrode potential. A platinum wire was used as a counter To run the electrochemical experiments, electrode. the potentials were measured against a Reversible Hydrogen Electrode (RHE). A gold collector electrode was used to deposit the platinum nanoparticles over it and, finally, polished with alumina powder before each experiment. The electrolyte used for electrochemical characterization of the prepared electrode was 0.5 M of  $H_2SO_4$  solution. The method for cleaning the Pt nanoparticles and CV condition was adjusted, as can be found in [13].

#### 2.5. Catalytic activity test

In order to determine catalytic activity of the synthesized nanocatalysts with different structures, reduction of p-NP over the prepared nanocatalysts was investigated as a reaction model. The catalytic reduction of p-NP was performed in a stainless steel autoclave. The amount of 0.1 g catalyst and 10 ml aqueous solution of p-NP (with the initial concentration of 20 ppm) were added to the autoclave and sealed. In order to remove air, the autoclave was purged with hydrogen gas. Then, hydrogen gas was introduced into the reactor to a desired pressure. Finally, the hydrogenation reaction was performed at 303 K and 1 atm. The hydrogenation reaction progress was monitored by the intensity of the characteristic peak of

p-NP at 400 nm using the UV-vis spectrophotometer [18]. Catalytic conversion of p-NP reduction was calculated through the following equation:

$$Conversion\% = \frac{C_0 - C_t}{C_0} \times 100, \tag{1}$$

where  $C_0$  is the initial concentration of *p*-NP, and  $C_t$  is the concentration at various times of *t*.

#### 3. Results and discussion

# 3.1. SEM analysis of the prepared nanocatalysts

The obtained SEM images of pristine  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> and Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts, prepared in H<sub>2</sub>Omicroemulsion and HCl(aq)-microemulsion, are shown in Figure 1. It was found that the catalyst kept the layer structure of the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> support and Pt nanoparticles well dispersed on the support. As can be seen from the size distribution histogram of Figure 1, the size of Pt nanoparticles is populated in the range of 2-10 nm for H<sub>2</sub>O-microemulsion and 10-20 nm for HCl(aq)-microemulsion. Martínez-Rodríguez et al. observed the growth of the Pt particle size by increasing HCl concentration [13]. These results confirm that the growth step of the nanoparticles' synthesis in microemulsion systems depends considerably on the environmental conditions of the reaction.

# 3.2. X-ray diffraction spectroscopy of the prepared nanocatalyst

XRD patterns of the  $Pt/\gamma$ - $Al_2O_3$  nanocatalyst samples, prepared in  $H_2O$ -microemulsion and HCl(aq)-microemulsion, are shown in Figure 2. The main reflection angles shown in Figure 2, related to  $\gamma$ - $Al_2O_3$  or Pt,

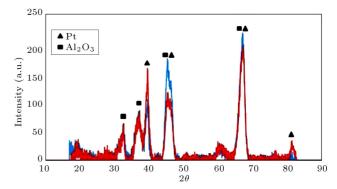
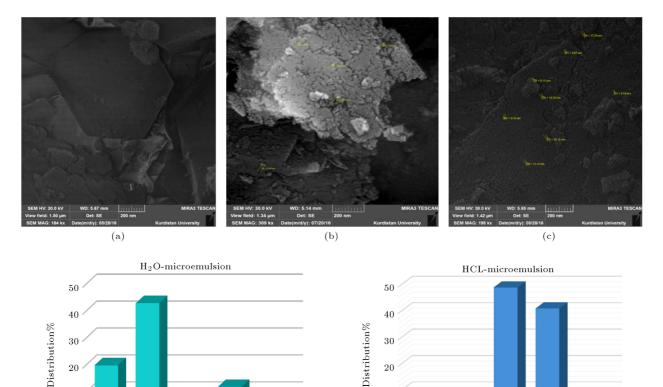


Figure 2. XRD patterns for  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts (blue line) prepared in HCl-microemulsion and (red line) in H<sub>2</sub>O-microemulsion systems.



10 10 0 0 5 - 1010 - 1515 - 2020 - 250-55 - 1010 - 1515 - 2020 - 250-5Size of Pt nanoparticles (nm) Size of Pt nanoparticles (nm)

Figure 1. SEM images of (a)  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, (b) Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> prepared in H<sub>2</sub>O-microemulsion, and (c) Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> prepared in HCl-microemulsion and particle size distribution histogram of fabricated nanocatalysts.

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have been approved by literature data. The reflection angles of  $2\theta = 39.8^{\circ}$ ,  $46.4^{\circ}$ , and  $66.8^{\circ}$  correspond to Pt(111), Pt(200), and Pt(220), respectively. As can be seen from XRD patterns, the two last peaks are overlapped at the same angles with alumina reflection data. As an interesting result, the intensity of surface (111) has been reduced and surface (200) increased for Pt nanoparticles synthesized in HCl(aq)-microemulsion system.

#### 3.3. Electrochemical results

Cyclic voltammetry experiment on platinum nanoparticles, prepared in  $H_2O$ -microemulsion and HCl(aq)microemulsion systems, was used to distinguish the effect of HCl on the shape of Pt particles. As reported by several investigations of CV for Pt NPs [13,14,19], four characteristic peaks of 0.12, 0.27, 0.37, and 0.53 V versus RHE should be observed. These peaks correspond to (110) sites, (100) steps and terrace borders, (100) terraces or wide domains, and (111)sites, respectively. Figure 3 shows CV for two types of nanoparticles, prepared in H<sub>2</sub>O-microemulsion and HCl(aq)-microemulsion systems. As observed from CV results, the peak areas at 0.27 and 0.37 V considerably increased when Pt NPs were synthesized in HCl(ag)microemulsion system, whereas the peak areas at 0.12 and 0.53 V decreased. The quantity of (111) sites is nearly negligible for the nanoparticles prepared in HCl (aq)-microemulsion system, which coincides with other observations [13,19].

#### 3.4. Catalytic activity results

The hydrogenation reaction of p-NP, as a reaction model, over the  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts was investigated to determine the effect of HCl in the fabrication process of catalyst on the catalyst activity. It is well known that Pt nanoparticles facilitate electron transfer from H<sub>2</sub> molecule, as a donor, to p-NP molecule as an

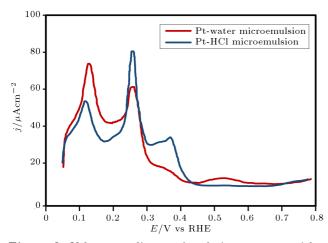


Figure 3. Voltameter diagram for platinum nanoparticles synthesized in water-microemulsion and HCl-microemulsion systems.

acceptor [20]. As is shown in the following mechanism, a six-electron reduction process is necessary to transform p-NP to p-AP (p-aminophenol):

$$2 Pt + H_2 \rightleftharpoons 2 Pt - H$$
$$6Pt - H + p - NP \rightarrow p - AP + 6Pt + 6H^+.$$

The reaction progress was monitored by measuring the absorption spectrum of p-NP as a function of time. After adding the Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts to the reaction mixture of p-NP and H2, a gradual decrease in the absorption peak at 400 nm, related to p-NP, was observed. The preliminary experimental results confirmed that no hydrogenation reduction occurred in the absence of the catalysts. This result confirms that there is no non-catalytic reaction. The percentage of catalytic conversion of p-NP hydrogenation over Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts synthesized in H<sub>2</sub>O-microemulsion and HCl(aq)-microemulsion systems was calculated using Eq. (1), as reported in Table 1.

As a result, the efficiency percent of the catalytic reduction of p-NP over  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalyst synthesized in HCl(aq)-microemulsion was found to be 100% after about 15 min. On the other hand, in the case of  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalyst synthesized in H<sub>2</sub>Omicroemulsion system, the efficiency was observed as about 28.1% after 15 min (Table 1). This interesting result and excellent performance of the catalyst synthesized in HCl(aq)-microemulsion can be explained based on the structure of the Pt nanoparticles dispersed on the alumina. As explained by the electrochemical results, the obtained voltammetric profile of  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalyst synthesized in HCl(aq)microemulsion represents the largest contributions at 0.35-0.37 V relating to the (100) ordered domains (Figure 3). It means that the catalytic reduction of p-NP over  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalyst is mainly accelerated by (100) site. On the other hand, this site can

Table 1. Percentage of catalytic conversion of p-NP hydrogenation over  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts synthesized in H<sub>2</sub>O-microemulsion and HCl-microemulsion systems.

Time (min)	$\mathrm{Pt}/\gamma\mathrm{-Al_2O_3}$	$\mathrm{Pt}/\gamma ext{-}\mathrm{Al}_2\mathrm{O}_3$
	$\mathbf{Synthesized}$	$\mathbf{Synthesized}$
	in water	in HCl 25%
5	4.8	26.2
10	11.9	95.1
15	28.1	100
20	45.8	100
25	51.8	100
30	58.3	100

facilitate electron transfer from donor  $H_2$  to acceptor p-NP through the above mechanism.

#### 4. Conclusion

In this research study,  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalysts were prepared by using microemulsion method with different pH conditions for the first time. One w/o microemulsion contains  $(H_2O + H_2PtCl_6)/n$ -heptane/Triton X-100/2-butanol, and the other contains (HCl(aq) +  $H_2PtCl_6)/n$ -heptane/Triton X-100/2-butanol. Characterization of the prepared nanocatalysts by X-ray diffraction and cyclic voltammetric methods showed that HCl content had significant effect on the shape and activity of the nanocatalysts. The structure effect on the catalytic activity of the prepared nanocatalysts was investigated by hydrogenation reaction of p-NP, as a reaction model. It is concluded that the activity of  $Pt/\gamma$ -Al<sub>2</sub>O<sub>3</sub> nanocatalyst synthesized in HCl(aq)microemulsion with (100) preferentially oriented Pt nanoparticles is strongly more than that prepared in  $H_2O$ -microemulsion system. These results open a new avenue to regulate activity and selectivity of the nanocatalysts prepared in microemulsion systems.

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