

Numerical Modeling of Hydraulic Fracturing in Oil Sands

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Hydraulic fracturing is a widely used and efficient technique for enhancing oil extraction from heavy oil sands deposits. Application of this technique has been extended from cemented rocks to uncemented materials, such as oil sands. Models, which have originally been developed for analyzing hydraulic fracturing in rocks, are in general not satisfactory for oil sands. This is due to a high leak-off in oil sands, which causes the mechanism of hydraulic fracturing to be different from that for rocks. A thermal hydro-mechanical fracture finite element model is developed, which is able to simulate hydraulic fracturing under isothermal and non-isothermal conditions. Plane strain or axisymmetric hydraulic fracture problems can be simulated by this model and various boundary conditions, such as specified pore pressure/fluid flux, specified temperature/heat flux, and specified loads/traction, can be modeled. The developed model has been verified by comparing its results to existing analytical and numerical solutions for thermo-elastic consolidation problems. The model has been used to simulate a laboratory experiment of hydraulic fracture propagation in oil sands. The results from the numerical model are in agreement with experimental observations. The numerical model and laboratory experiments both indicate that, for uncemented porous materials, such as sands (as opposed to rocks), a single planar fracture is unlikely to occur and a system of multiple fractures or a fracture zone consisting of interconnected tiny cracks should be expected.

INTRODUCTION

Hydraulic fracturing is a widely used technique to enhance oil and gas production. The technique was introduced to the petroleum industry in 1947, and is now a standard operating procedure. By 1981, more than 800,000 hydro fracturing treatments had been performed and recorded. Today, about 35% to 40% of all currently drilled wells are hydraulically fractured [1].

Since its inception, hydraulic fracturing has developed from a simple low volume and low injection rate reservoir stimulation technique to a highly engineered and complex procedure that can be used for many purposes. Figure 1 depicts a typical hydraulic fracturing process in the petroleum industry. The procedure is as follows. First, a neat fluid, such as water (called

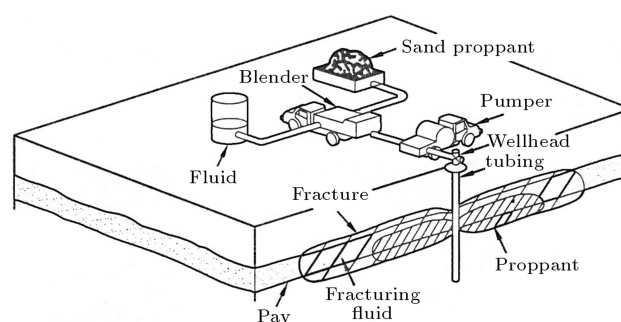


Figure 1. Typical hydraulic fracturing treatment in petroleum industry (after [1]).

‘pad’), is pumped into the well at the desired depth (pay zone), to initiate the fracture and to establish its propagation. This is followed by pumping slurry, which is a fluid mixed with a propping agent, such as sand (often called a ‘proppant’). This slurry continues to extend the fracture and concurrently carries the proppant deeply into the fracture. After pumping, the injected fluid chemically breaks down to a lower viscosity and flows back out of the well, leaving a highly conductive propped fracture for oil and/or gas to easily

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flow from the extremities of the formation into the well. It is generally assumed that the induced fracture has two wings, which extend in opposite directions from the well and is oriented, more or less, in a vertical plane. Other fracture configurations, such as horizontal fractures, are also reported to occur, but they constitute a relatively low percentage of situations documented. Experience indicates that at a depth of below 600 meters, fractures are usually oriented vertically. At shallow depths, horizontal fractures have been reported [1]. The fracture pattern, however, may not be the same for different types of soil and rock.

'Oil sands' exist in some parts of the world as thick deposits in deep and semi-deep underground layers. For extraction of oil from oil sand deposits, one of the widely used methods, as described above, is hydrofracturing, in which hot water/steam is injected into the wells at a very high rate and temperature. Although sand is a cohesionless material, the viscous bitumen that exists in the porous medium causes the combination of sand and bitumen to behave like a porous rock that may experience fracturing due to high injection pressure. The study of types and patterns of fracture in uncemented oil sand deposits, by means of numerical modeling, is the basic objective of this paper.

For decades, petroleum engineers have been developing models for simulating hydraulic fracturing in oil reservoirs. In the early 1960's, the industry felt the need for a design tool for this fast growing technique. In response to this need, a number of two-dimensional (2-D) models were developed for designing hydraulic fracturing treatments. This type of simple closed form solution has been used by the industry with some success; however, as the technology progressed from low volume/rate to high volume/rate treatments in more sophisticated and massive hydraulic fracturing projects, the industry demanded more rigorous design methods in order to minimize costs. In the last 20 years, a number of 2-D and 3-D numerical models have been developed (some of these models will be discussed later). The most common equations used in these numerical models are fluid flow and heat transfer equations, which are usually solved iteratively. Geomechanical aspects are incorporated in some of the models, mostly in an uncoupled manner. Mainly vertical or horizontal planar fractures were considered, based on the 2-D closed form solutions mentioned above. The degree of sophistication of these models varies considerably and their results cannot be validated with much confidence. The main problem in validating these models is that the configuration of the induced fracture is not really known; therefore, the results of the model are usually evaluated based on fluid injection pressure measurements and/or the production history of the well.

The application of these models to oil sands,

however, has not been very successful and predictions of the model, in some cases, have been poor. Some researchers attribute the discrepancy to the effect of high leak-off rates in oil sands. On the other hand, the peculiar characteristics of oil sand, such as an interlocked structure with a high dilation rate, a nonlinear stress-strain behavior with strain softening after the peak, a dilation phenomenon at shear failure and a temperature-dependent behavior, may also contribute to the discrepancy between model predictions and field measurements.

In this paper, a brief overview of the earlier studies will be presented and a mathematical formulation of the developed fully coupled thermal hydro-mechanical fracture model will be discussed in detail. Modeling of the fracture process and its numerical treatment will then be explained and benchmarking of the developed finite element model will be presented by comparing its results to the existing analytical, numerical and experimental solutions.

EARLIER STUDIES OF HYDRAULIC FRACTURING

Zhel'tov and Khristianovitch [2], Perkins and Kern [3] and Geertsma and Deklerk [4] are among the first investigators to develop models for hydraulic fracturing. Zhel'tov and Khristianovitch [2] introduced the concept of mobile equilibrium, i.e. slow moving fracture propagation as a result of hydraulic action. Geertsma and Deklerk [4] used their concepts and provided a closed form solution for a planar fracture. This model is based on the assumption of plane strain deformation in a 'horizontal plane' and is usually called the GdK model. Perkins and Kern [3] proposed a different closed form solution for hydraulic fracture propagation problems. The model is based on the assumption of plane strain deformation in a 'vertical plane'. Nordgren [5] improved this work by incorporating the effect of leak-off and, hence, this model is usually called PKN. In these models, the height of the fracture, h_f , is considered to be known, which is equal to the thickness of the oil-bearing layer (pay). For the determination of other values, such as fracture length (L_f), maximum fracture opening and injection pressure, a set of equations has been derived.

There have been some efforts to simulate 3-D fracture propagation [6,7]. In these models, the assumption of isotropic elasticity is used and the effects of pore pressure are neglected. The elasticity equations are coupled with the equation of flow inside the fractures. In these models, the concept of inducing a planar fracture is retained but the height of the fracture is not fixed and varies with changes in stress. Fracture extension is controlled by a linear elastic fracture mechanics criterion. Advani et al. [8] developed a finite

element program for modeling 3-D hydraulic fractures in multi-layered reservoirs. They extended the earlier work of the Pseudo three-dimensional (P3D) model presented by Advani and Lee [9] and other investigators in the early 80's. This work investigated tensile planar hydraulic fracture propagation in layered reservoirs with elastic behavior.

Settari and Raisbeck [10,11] provided two of the early work on hydraulic fracture simulation in 'oil sand deposits'. In 1979, they developed a two dimensional finite difference model for single-phase compressible fluid flow in a linear elastic porous material with a tensile fracture, similar to the PKN model. This model was extended to a two-phase thermal flow [11] in order to describe the process of a first cycle steam injection for three different fracture geometries.

Atukorala [12] developed a finite element model for simulating either horizontal or vertical hydraulic fracturing in oil sands. In this work, for the sake of simplicity, the fluid flow analysis was separated from stress analysis. These two equations were solved iteratively by imposing a compatibility condition on the volume of the fluid in the fracture. The fracture shape was assumed elliptic with blunt tips, in order to avoid the singularity of stresses at the crack tip. A linear elastic fracture mechanics criterion was used for analyzing the tensile fracture in a nonlinear elastic domain. No thermal effect was considered in this study.

Settari et al. [13] investigated the effects of soil deformation and fracture on the reservoir in a partially coupled manner. The effect of leak-off on fracture dimensions was emphasized. Oil sand failure was considered to be shear failure with a Mohr-Coulomb criterion. Dilation was not modeled in this work, but it was assumed that a constant change in volumetric strain occurs after reaching a peak shear stress (failure). They developed a computer program, called CONS, based on the above, partially coupled stress-flow, analysis. Settari [14,15] extended this work by incorporating temperature effects (thermal flow) in the formulation.

Frydman and Fontoura [16] simulated the process of borehole pressurization, the mechanism for which is the same as hydraulic fracture treatment with a coupled hydromechanical approach. They developed a new fracture element, considering the effect of a cohesive zone in crack analysis. In their work, the direction of the fracture propagation was predefined and no thermal effect was considered.

Ouyang et al. [17] developed a mathematical model and employed an adaptive finite element scheme to simulate the distribution of proppant in a propagating hydraulic fracture.

Itaoka et al. [18] studied the crack growth behavior under high tectonic stress, conditions corresponding to great depths. Their study presents a finite element

model for the analysis of hydraulic fracturing, taking into account the mixed-mode fracture. They investigated crack growth behavior as the mode of crack propagation.

Yang et al. [19] numerically studied the effect of heterogeneity and permeability on the initiation and propagation of hydraulic fracturing.

Reynolds et al. [20] used Stimplan software package to determine the optimum fracture dimensions, sizing and sand schedule. Stimplan is a pseudo 3-D, numerical model performing an implicit finite difference solution to basic equations of mass balance, elasticity and fluid flow.

Lu et al. [21] developed a pseudo 3-D hydraulic fracturing using radial flow, which made a better prediction regarding fracture height.

Cook et al. [22] conducted a joint experimental-numerical study regarding the exploration of near-well bore mechanics. An experimental procedure, using a true-triaxial apparatus, was developed for the laboratory simulation of slurry injection, and a Discrete Element Method (DEM) numerical model was used for simulation of the experiments. They found that, under isotropic horizontal stress conditions, multiple vertical fractures were induced and propagated in random orientations.

In the early models, it was assumed that fracture in oil sand is similar to fracture in soft cemented rock, such as sandstone; however, the prediction of these models did not match field observations. For example, the fracture length was smaller than the value predicted by the models, the fracture opening was larger and the injectivity was much higher than anticipated. These facts indicated that hydraulic fracturing in oil sand, contrary to rock, is dominated by leak-off. This high leak-off cannot be adequately described by classical models, such as those proposed by Carter [23] or Nordgren [5]. In order to describe this situation, geomechanical aspects have to be invoked. By incorporating the geomechanical behavior of oil sand in the model, such as shear failure and dilation effects (and the corresponding increase in porosity and permeability), a significant improvement in the results of the model was observed. From a reservoir engineering viewpoint, the main objective of modeling is being able to predict the production rates of oil wells. Thus, geomechanical aspects are employed in these models, mainly to better improve their prediction ability.

Fracture modeling in porous materials is clearly dependent on the stress field in the soil, as well as pore fluid pressures. Therefore, contrary to most available reservoir engineering models, any attempt to simulate hydraulic fracturing in oil sand deposits should incorporate a detailed stress/deformation analysis.

It should be noted that, in hydraulic fracturing,

four processes are acting simultaneously. Ground deformation, fluid flow, heat transfer, and fracturing phenomenon are the main issues involved in hydraulic fracturing. Therefore, for the modeling of hydraulic fracturing in geomaterials, at least three conservation laws for applied load, fluid flow, and heat transfer, in the form of three partial differential equations, have to be solved simultaneously. Fracture configuration should be based on stress/deformation analysis in the ground. In this case, imposing a kind of prescribed fracture geometry on the model is not necessary.

FORMULATION OF THE FULLY COUPLED THERMAL HYDROMECHANICAL (THM) MODEL

In formulating the model, three partial differential equations of equilibrium, continuity of fluid flow, and heat transfer are considered in incremental forms. Changes in displacement in three directions, $\{\Delta U\}$, changes in pore pressure ΔP , and changes in temperature ΔT , are the primary unknowns, which define the state of any point inside the domain. Since small strains/displacements are assumed, $\{\Delta U\}$, ΔP and ΔT , during a time increment, Δt , are small and second (or higher) order incremental terms are neglected in the formulation. In this section, a superimposed dot means a derivative with respect to time, '*' stands for nodal values and '-' means prescribed values. Subscript 't' means the value at time t , and subscript ',' indicates a derivative with respect to the coordinate axes.

An equilibrium equation is used as the basis for the deformation analysis. The equilibrium equation in an incremental form reads as follows [24,25]:

$$\Delta\sigma_{ij,j} + \Delta F_i = m' \Delta \ddot{U}_i + C' \Delta \dot{U}_i. \quad (1)$$

A weighted residual method is used for obtaining the weak form of Equation 1. After integration by parts:

$$\begin{aligned} \int_S \Delta\sigma_{ij} n_j \omega ds - \int_V \Delta\sigma_{ij} \omega_{,j} dV \\ = \int_V (-\Delta F_i + m' \Delta U_i + c' \Delta U_{i,t}) \omega dV, \end{aligned} \quad (2)$$

the following boundary conditions are considered (Figure 2):

- Stress boundary condition (natural B.C.):

$$\Delta\sigma_{ij} n_j = \Delta \bar{t}_{si} \text{ on } S\sigma, \quad (3)$$

- geometric boundary condition (essential B.C.):

$$U_i = \bar{U}_i \text{ on } Su. \quad (4)$$

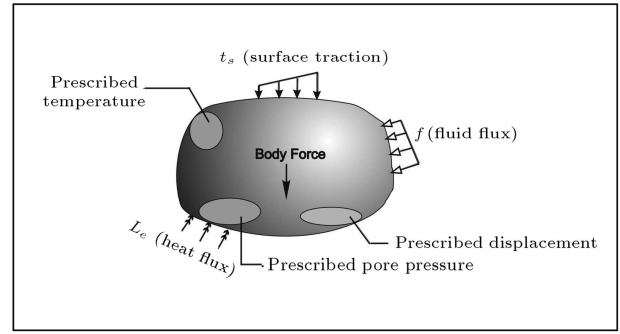


Figure 2. Boundary conditions of a typical domain.

Since dynamic effects are not considered in this study, inertia and damping terms will be neglected. The principle of effective stress can be written in an expanded form incorporating the effect of thermal expansion:

$$\begin{aligned} \Delta\sigma_{ij} &= \Delta\sigma'_{ij} - \Delta P \delta_{ij} \\ &= D_{ijkl} \left(\Delta\epsilon_{kl} - \frac{1}{3} \alpha_s \delta_{kl} \Delta T \right) - \Delta P \delta_{ij}. \end{aligned} \quad (5)$$

For consistency with the other two conservation laws, 'P' is considered to be positive in compression. Soil/rock particles are considered to be incompressible and the effect of creep and/or other strains are disregarded in Equation 5. Assumption of the incompressibility of solid grains is usually valid, since the compressibility of pore fluid, especially pore fluid with occluded gas bubbles, such as oil (bitumen), is very high. Thus, in comparison, the compressibility of solid grains can be neglected. Equation 5 can be used for substituting total stress with effective stress in Equation 2.

In order to obtain the finite element form of Equation 2, spatial discretization can be performed, using the following relationships:

$$\begin{aligned} \Delta U_i &= [N] \{\Delta U^*\}, & \Delta\epsilon_{ij} &= [B] \{\Delta U^*\}, \\ \Delta\epsilon_V &= [C] \{\Delta U^*\}, \\ \Delta P &= \langle N_P \rangle \{\Delta P^*\}, & \Delta P_{,j} &= [B_P] \{\Delta P^*\}, \\ \Delta T &= \langle N_T \rangle \{\Delta T^*\}, & \Delta T_{,j} &= [B_T] \{\Delta T^*\}. \end{aligned} \quad (6)$$

By employing the Galerkin method:

$$[\omega] = [N] \text{ and } [\omega]_{,j} = [B], \quad (7)$$

'N' indicates the shape function matrix and 'B' is the derivative of shape functions, with respect to the spatial coordinates x , y and z . In order to make it possible to use different interpolation schemes for calculating displacements, pore fluid pressures, and temperatures, different 'N' and 'B' will be used for

pore fluid pressures and temperatures. These will be designated by subscripts 'P' and 'T', respectively. For calculating displacements, 8-node rectangular isoparametric elements are used. For calculating pore pressures and temperatures, however, 8-node rectangular elements are changed to 4-node rectangular elements by using the appropriate shape functions. It has been generally observed [26,27] that, in order to obtain compatible coupled fields, the displacement interpolation should be one order higher than the pore pressure interpolation. Also, Aboustit et al. [28] have reported that the use of a 4-node rectangular element for pore pressures, along with an 8-node rectangular element for displacements, resulted in less oscillation in the analysis of a consolidation problem (compared to a case in which an 8-node element was used for both pore pressure and displacements).

By substituting Equations 3 to 7 into Equation 2, the following equation is obtained:

$$\begin{aligned}
 & \left(- \int_V [B]^T [D] [B] dV \right) \{ \Delta U^* \} \\
 & + \left(\int_V [B]^T \{ m \} < N_P > dV \right) \{ \Delta P^* \} \\
 & + \left(\int_V [B]^T [D] \frac{1}{3} \alpha_S \{ m \} < N_T > dV \right) \{ \Delta T^* \} \\
 & = - \int_{S_\sigma} [N]^T \{ \Delta \bar{t}_S \} dS + \int \lim its_V [N]^T (- \{ \Delta F \} \\
 & + m' \{ \Delta \ddot{U} \} + c' \{ \Delta \dot{U} \}) dV. \quad (8)
 \end{aligned}$$

In Equation 8, $\{m\}$ represents the Kronecker delta in vector form. The final finite element form of this equation would be:

$$[K_{11}] \Delta U^* + [K_{12}] \Delta P^* + [K_{13}] \Delta T^* = \{F_1\}, \quad (9)$$

where K_{11} , K_{12} and K_{13} represent the factors of ΔU^* , ΔP^* and ΔT^* in Equation 8, respectively, and the whole right-hand side of this equation is shown as F_1 .

For fluid flow, the mass continuity equation for porous media is used [29]:

$$\nabla \cdot (\rho v) - G = - \frac{\partial}{\partial t} (\phi \rho). \quad (10)$$

By applying the weighted residual method to obtain the weak form of this equation and then integrating by

parts, Equation 10 becomes:

$$\begin{aligned}
 \int_S (\rho \bar{v})_i n_i \omega dS - \int_V (\rho v)_i \omega_{,i} dV & = - \int_V \frac{\partial}{\partial t} (\phi \rho) \omega dV \\
 & + \int_V G \omega dV. \quad (11)
 \end{aligned}$$

Two types of boundary condition are considered as follows (shown in Figure 2):

- Specified velocity (flux) at the boundary:

$$v_i = \bar{v}_i \quad \text{on } S_v, \quad (12)$$

- Specified pore fluid pressure at the boundary:

$$P = \bar{P} \quad \text{on } S_p. \quad (13)$$

The terms ϕ , ρ , $\frac{\partial \phi}{\partial t}$, $\frac{\partial \rho}{\partial t}$ and v_i can be substituted with relations described below, assuming that the rate of change, with respect to time, can be approximated by the change during the time increment Δt :

- a) Porosity

$$\phi_t = \left(\frac{V_V}{V_b} \right)_t = \frac{V_b - V_s}{V_b}, \quad (14)$$

where V_b is the bulk volume of soil/rock and V_V and V_s are the volume of voids and the volume of solids, respectively.

$$\phi_{t+\Delta t} = \frac{(V_b + \Delta V_b) - (V_s + \Delta V_s)}{(V_b + \Delta V_b)}. \quad (15)$$

Now, $\Delta V_b = \varepsilon_V V_b$ by definition and $\Delta V_s = V_s \alpha_S \Delta T$, assuming that the change in the volume of solids can be mainly attributed to the thermal expansion of solids, because the compressibility of solids compared to the compressibility of pore fluid and bulk medium, is negligible. Hence, the volume change of solids, due to change in pore pressure and effective stresses, can be ignored. Therefore, by substitution for ΔV_b and ΔV_s in Equation 15 and some manipulations, one obtains:

$$\phi_{t+\Delta t} = \frac{1}{1 + \varepsilon_V} [\phi_t + \varepsilon_V - \alpha_S \Delta t (1 - \phi_t)], \quad (16)$$

and:

$$\Delta \phi = \phi_{t+\Delta t} - \phi_t = \frac{1 - \phi_t}{1 + \varepsilon_V} (\varepsilon_V - \alpha_S \Delta t), \quad (17)$$

- b) Fluid density: Variations of fluid density with changes in pressure and temperature can be described as follows:

$$\rho_t = \rho_0 \{ [1 + \beta_T (P - P_0)] [1 - \alpha_P (T - T_0)] \}. \quad (18)$$

Assuming that α_P and β_T are the coefficients of fluid thermal expansion and fluid compressibility, respectively, Equation 18 can be written for time 't + Δt ' in the following form:

$$\rho_{t+\Delta t} = \rho_t(1 + \beta_T \Delta P)(1 - \alpha_P \Delta T), \quad (19)$$

$$\Delta \rho = \rho_{t+\Delta t} - \rho_t = \rho_t \beta_T \Delta P - \rho_t \alpha_P \Delta T$$

$$- \rho_t \beta_T \alpha_P \Delta P \Delta T \approx \rho_t (\beta_T \Delta P - \alpha_P \Delta T), \quad (20)$$

c) Fluid velocity: Darcy's law, in general index form, is given by:

$$v_i = -K_{ij} \frac{\partial H}{\partial x_j}, \quad (21)$$

where K is permeability (m/sec) and H is total head. Representing K in terms of absolute permeability, k (m²), and expanding H yields the following:

$$v_i = -\frac{k_{ij}\gamma}{\mu} \left(z + \frac{P}{\gamma} \right)_{,j} = -\frac{k_{i3}\rho g}{\mu} - \frac{k_{ij}}{\mu} \frac{\partial P}{\partial x_j}$$

$$+ \frac{k_{ij}P \left(\frac{\partial \rho}{\partial x_j} \right)}{\mu \rho}, \quad (22)$$

where μ , z , P and γ are dynamic viscosity of fluid, elevation, pore pressure and fluid unit weight, respectively. The term k_{i3} represents the third row of the permeability tensor corresponding to the z axis.

By discretization in space, as described in Equation 6, the relationship for velocity can be expanded as follows:

$$v_i = -\frac{k_{i3}\rho_t g}{\mu_t} + \frac{k_{ij}[B_P]\{P_t^*\}}{\mu_t} - \frac{k_{ij}\theta[B_P]\{\Delta P^*\}}{\mu_t}$$

$$+ \frac{k_{ij} < N_P > \{P_t^*\}}{\mu_t \rho_t} \frac{\partial \rho_t}{\partial x_j}$$

$$+ \frac{k_{ij}\theta < N_P > \{\Delta P^*\}}{\mu_t \rho_t} \frac{\partial \rho_t}{\partial x_j}. \quad (23)$$

θ is a number which may vary from 0 (explicit scheme) to 1.0 (implicit scheme). All values with the subscript 't' denote that they are considered to be at time 't' (known), for the sake of simplicity. They are modified at the end of each time step. Three terms, without the primary unknown (ΔP^*), are lumped together into Z_i , which represents the velocity at time 't'. The two remaining terms with (ΔP^*) constitute Δv_i .

$$v_i = -Z_i - \theta \left(\frac{k_{ij}[B_P]}{\mu_t} - \frac{k_{ij} < N_P > \partial \rho_t}{\mu_t \rho_t \partial x_j} \right) \{\Delta P^*\}, \quad (24)$$

where:

$$Z_i = \frac{k_{i3}\rho_t g}{\mu_t} + \frac{k_{ij}[B_P]\{P_t^*\}}{\mu_t}$$

$$- \frac{k_{ij} < N_P > \{P_t^*\}}{\rho_t \mu_t} \frac{\partial \rho_t}{\partial x_j}. \quad (25)$$

In summary, the following relations are used in the formulation:

$$\phi = (1 - \theta)\phi_t + \theta\phi_{t+\Delta t} = \phi_t + \theta\Delta\phi$$

$$= \phi_t + \theta \left[\frac{1 - \phi_t}{1 + \varepsilon_v} (\varepsilon_v - \alpha_S \Delta T) \right], \quad (26)$$

$$\rho = (1 - \theta)\rho_t + \theta\rho_{t+\Delta t} = \rho_t + \theta\Delta\rho$$

$$= \rho_t + \theta\rho_t(\beta_T \Delta P - \alpha_P \Delta T), \quad (27)$$

$$\frac{\partial \phi}{\partial t} \approx \frac{\Delta \phi}{\Delta t} = \frac{1 - \phi_t}{1 + \varepsilon_v} \frac{(\varepsilon_v - \alpha_S \Delta T)}{\Delta t}, \quad (28)$$

$$\frac{\partial \rho}{\partial t} \approx \frac{\Delta \rho}{\Delta t} = \frac{\rho_t}{\Delta t} (\beta_T \Delta P - \alpha_P \Delta T), \quad (29)$$

$$v_i = (1 - \theta)v_{it} + \theta v_{it+\Delta t} = v_{it} + \theta \Delta v_i$$

$$= \left[\frac{k_{ij}\gamma}{\mu} \left(z + \frac{P}{\gamma} \right)_{,j} \right]_t + \theta \Delta \left[\frac{k_{ij}\gamma}{\mu} \left(z + \frac{P}{\gamma} \right)_{,j} \right]. \quad (30)$$

These equations should be substituted in Equation 11. By spatial discretization using Equation 6 and by employing the Galerkin method, $\langle \omega \rangle = \langle N_P \rangle$ and $\langle \omega \rangle_{,j} = [B_P]$, Equation 11 is converted to the integral form, from which the final finite element form of the fluid flow continuity equation can be obtained as:

$$[K_{21}]\Delta U^* + [K_{22}]\Delta P^* + [K_{23}]\Delta T^* = \{F_2\}, \quad (31)$$

where K_{21} , K_{22} and K_{23} represent the factors of ΔU^* , ΔP^* and ΔT^* , respectively, in the final integral form of Equation 11 and the whole right-hand side of this equation is shown as F_2 .

The heat transfer process is incorporated in the model by using the first law of thermodynamics, applicable to porous media [30]:

$$\nabla \cdot L_e - Q = -\frac{\partial(\rho E)}{\partial t}. \quad (32)$$

By applying the weighted residual method to Equation 32 and integration by parts:

$$\int_S (L_{ei} n_i) \omega dS - \int_V L_{ei} \omega_{,i} dV = - \int_V \frac{\partial}{\partial t} (\rho E) \omega dV$$

$$+ \int_V Q \omega dV. \quad (33)$$

Two kinds of boundary condition are considered, which are shown in Figure 2:

- Specified heat flux at the boundary:

$$L_{ei} = \bar{L}_{ei} \quad \text{on } S_L, \quad (34)$$

- Specified temperature at the boundary:

$$T = \bar{T} \quad \text{on } S_T. \quad (35)$$

L_e can be expanded as below, indicating a thermal energy flux due to conduction and convection:

$$L_{ei} = -\lambda \frac{\partial T}{\partial x_i} + f_i \rho \left[C_P(T - T_0) + \frac{gz}{J} \right], \quad (36)$$

where the first term represents thermal conduction and the second term stands for thermal convection, λ is the coefficient of conductivity and J is the mechanical equivalent of heat. The other terms are defined in the notation list. Also, (ρE) can be written as follows:

$$(\rho E) = (1 - \phi) \rho_S C_S (T - T_0) + \phi S \rho_f C_V (T - T_0). \quad (37)$$

In Equation 37, the first and second terms are the heat capacitances of solids and pore fluid, respectively. Since changes in ρ_S , relative to changes in ρ_f , are negligible, $(\rho_S C_S)$ are usually combined together and called M_σ .

By assuming a degree of saturation, $S = 1.0$, (for a medium fully saturated by a compressible fluid) substituting volumetric flux, f_i , with its equivalent v_i , and by using Equations 36 and 37 for substituting L_e and ρE , respectively, Equation 33 can be written as follows:

$$\begin{aligned} \int_S (\bar{L}_{ei} n_i) \omega dS + \int_V \lambda \frac{\partial T}{\partial x_i} \omega_{,i} dV \\ - \int_V v_i \rho C_P (T - T_0) \omega_{,i} dV \\ - \int_V v_i \rho \frac{gz}{J} \omega_{,i} dV \\ + \int_V \frac{\partial}{\partial t} [(1 - \phi) M_\sigma (T - T_0)] \omega dV \\ + \int_V \frac{\partial}{\partial t} [\phi \rho C_V (T - T_0)] \omega dV \\ - \int_V Q \omega dV = 0. \end{aligned} \quad (38)$$

By substituting Equations 26 to 30 into Equation 38, discretization in space using Equations 6, and employing the Galerkin method: $\langle \omega \rangle = \langle N_T \rangle$ and $\langle \omega \rangle_{,i} = [B_T]$, the final finite element form of the heat transfer equation can be written as follows:

$$[K_{31}] \Delta U^* + [K_{32}] \Delta P^* + [K_{33}] \Delta T^* = \{F_3\}, \quad (39)$$

where K_{31} , K_{32} and K_{33} represent the factors of ΔU^* , ΔP^* and ΔT^* , respectively, in the final integral form of Equation 38, and the whole right-hand side of this equation is shown as F_3 .

It should be noted that all second (or higher) order incremental values, such as $(\Delta U)^2$ and $(\Delta P)^2$ etc. are considered to be small and, therefore, are neglected in the formulation. In order to have a 'fully coupled' model, Equations 9, 31 and 39 should be solved simultaneously. As shown, all of these equations contain the same state variables, which are displacements, $\{\Delta U\}$, pore fluid pressures, ΔP , and temperatures, ΔT . In coupled form:

$$\begin{bmatrix} K_{11} & K_{12} & K_{13} \\ K_{21} & K_{22} & K_{23} \\ K_{31} & K_{32} & K_{33} \end{bmatrix} \begin{Bmatrix} \{\Delta U^*\} \\ \Delta P^* \\ \Delta T^* \end{Bmatrix} = \begin{Bmatrix} F_1 \\ F_2 \\ F_3 \end{Bmatrix}. \quad (40)$$

The off-diagonal terms in $[K]$ represent the coupling terms in the analysis. It is worth noting that $[K]$ is not symmetric, even though an elasticity or an associated plasticity constitutive relation for soil or rock is used, because, in general, $K_{13} \neq K_{31}$ and $K_{23} \neq K_{32}$. The matrix $[K]$ and vector $\{F\}$ are first determined at the element (local) level. The global $[K]_G$ and $\{F\}_G$ are then assembled, based on $[K]$ and $\{F\}$ obtained at the element level, in order to determine all of the unknowns throughout the finite element domain.

$$[K]_G \{X\}_G = \{F\}_G. \quad (41)$$

FINITE ELEMENT MODELING OF FRACTURES

The discrete fracture approach (as opposed to the smeared approach) is used for the simulation of fractures in the finite element mesh. The 'smeared approach' takes the properties of fractures and smears them over an area of soil/rock matrix without introducing any real fracture. This approach is most appropriate for situations in which numerous and uniformly spaced fractures predominate. A 'discrete fracture' is best suited to cases where a limited number of dominant fractures exist. The basic idea in this approach is that, after an occurrence of fracture, the continuous medium no longer exists and each individual fracture and its particular characteristics are of interest.

Generally, different types of fracture initiation criteria may be used in the program. Tensile strength

criterion and criteria based on fracture mechanics principles, as well as empirical relations, can be used in the numerical analysis. For the first two, the results of the stress analysis are used to determine whether or not the crack initiates at certain nodes. In the present study, since modeling of the fracturing process in 'oil sands' is of concern, a reliable criterion, based on laboratory experiments, in which the stress intensity factor for oil sands is measured, could not be found. So, for uncemented material, such as oil sands, a tensile strength criterion has been adopted, i.e. fracturing initiates whenever the stress at a node is below tensile strength.

Despite the importance of mode I (tensile fracture), the high leak-off phenomenon and the influence of generated pore pressure on the oil sands fracturing process reveals that a kind of shear fracture mechanism may also be involved, due to low effective stresses and lack of shear strength. Since the mechanism of shear fracture in uncemented saturated materials is different from in rock, in this study, a Mohr-Coulomb type shear criterion was used to detect the initiation of a shear fracture.

The fracturing process is simulated by using a splitting nodes technique. This technique requires that, in the potential fracture zone, each node in the mesh is assigned to double nodes with the same coordinates. During the analysis, whenever the fracture criteria (tensile or shear) are satisfied at the nodes, the double nodes will split into two separate nodes resulting in a change in the mesh geometry. Since the problem is solved by marching in time, in the next time step, the problem will be solved with the new geometry with a crack (separated nodes) inside the mesh. If, in this time step, stresses at the nearby double nodes satisfy the fracture criteria, node splitting will take place again and, in this way, propagation of the fracture can be modeled. It is worth noting that, before splitting the nodes, the degrees of freedom for the double nodes are the same. This means that double nodes will not increase the total number of degrees of freedom (i.e., total number of unknowns) or the dimension of the general coefficient matrix. This reduces computational effort and enhances the efficiency of the program. Based on the small strain theory, changes in displacements, $\{\Delta U^*\}$, (the corresponding pore pressures, ΔP^* , and temperatures, ΔT^*) are assumed to be small at any time step. Hence, nodal coordinates are updated at the end of each time step. In this manner, the configuration of the fracture and its aperture are updated continuously.

For modeling the flow of fluid and/or heat inside the fracture, a new type of 'fracture element' is developed [31]. This fracture element is a 6-node isoparametric rectangular element, as shown in Figure 3. Shape functions of the developed fracture

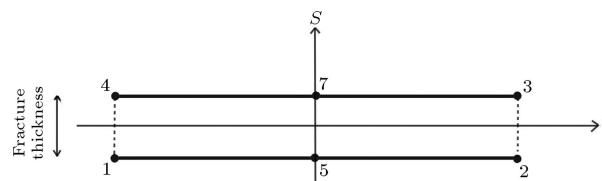


Figure 3. 6-node rectangular fracture element.

elements are the same as shape functions of quadrilateral rectangular elements modified for omitting two side nodes (nodes 6 and 8). This kind of element can be used in the areas of the mesh where the possibility of fracturing is high; for instance, a zone around a notch, or a zone close to the fluid injection area that is prone to fracturing. If the estimation of the zone of fracturing, in advance, is difficult, these fracture elements can be used throughout the entire mesh. Initially, the fracture elements are embedded inside the mesh between other elements; their thickness is zero and they are absent from the analysis. When 4 out of 6 nodes of a fracture element split, due to the tensile or shear fracture, the program activates the fracture element automatically. It is also possible to establish a criterion for the fracture element aperture and whenever the aperture reaches a certain value, the element stiffness is incorporated into the global stiffness matrix calculations. Therefore, the geometry of the mesh will change and the effects of the activated fracture element will be taken into account. The stiffness of fracture elements is set to zero. This is justified, due to the very low stiffness of fracture elements relative to other elements. However, fracture elements are very important in transmitting fluid and/or heat through the medium, due to their high conductivities. Therefore, they possess all of the terms related to fluid flow and heat transfer, exactly the same as other elements. The injected fluid/heat finds these elements easier and quicker paths to flow through. Details of the finite element formulation of the developed fracture elements are explained in Pak [31].

An important feature in modeling hydraulic fracturing is the existence of pressure and temperature gradients inside a fracture. Some researchers [32,33] assumed a gradient, based on empirical results and field data. In the present approach, this gradient is modeled by selecting an appropriate permeability for the fracture element. Conceptually, tensile fractures in a cohesive material produce clean fractures, however, this is often not the case, especially when the apertures are small and the physical bonds between soil or rock particles might still exist. Even in a clean fracture, because of a small aperture, the roughness of the walls and a change in the fracture direction, the permeability inside a fracture must have a finite value. Some investigators have used a parallel plate theory to determine the hydraulic conductivity. Witherspoon et

al. [34] and Ryan et al. [35], among others, have shown that this theory accurately describes the flow through natural and induced fractures. Therefore, by assigning a realistic permeability for the fracture elements, a pressure gradient would be automatically incorporated into the analysis. In the same way, by introducing a heat capacitance for the fracture elements, it is also possible to establish a thermal gradient. If the coefficients of permeability and heat capacitance for the fracture elements are higher than those of the surrounding medium, normally, fluid flow and heat transfer occur more easily within the fracture elements. These phenomena are expected to occur in seepage and heat transfer problems, i.e. the gradients tend to concentrate in the areas with higher permeability and/or heat capacitance. This is what actually occurs in seepage and heat transfer problems, as will be discussed later.

Although the mathematical and finite element formulation of this study are quite general, since it is a first attempt to model the hydraulic fracturing process using a fully coupled thermal hydro-mechanical fracture finite element model, it was decided to consider only two-dimensional problems, in order to ensure that the model can adequately handle the complicated physical process and can accurately capture all of the key issues of the problem. For the same reason, a single-phase compressible flow is considered in the model.

BENCHMARKING OF THE COUPLED FINITE ELEMENT FRACTURE MODEL

Modeling the Plane Strain Thermal Consolidation Problem

The thermo-elastic consolidation problem has been solved by Aboustit et al. [28] and also by Lewis et al. [36]. In this case, a column of linear elastic material is subjected to a unit surface pressure and a constant surface temperature of $T = 50^\circ$. Figure 4 shows the finite element mesh of the problem. The pore pressure is kept equal to zero at the top surface; everywhere else, the boundaries of the soil are sealed and insulated (i.e. no fluid or heat flow is permitted). The parameters used in the analysis are summarized in Table 1 and the time steps used in the analysis are shown in Table 2. Almost the same temporal discretization shown in Table 2 was used in both studies by Aboustit et al. [28] and Lewis et al. [36], because this discretization scheme provided good agreement with the analytical solution for 'isothermal' consolidation problems [37].

All components in the coefficient matrix shown in Equation 40 are included in this analysis, except $[K_{31}]$ and $[K_{23}]$. This is done for reasons of comparison with the results of Aboustit et al. [28] and Lewis

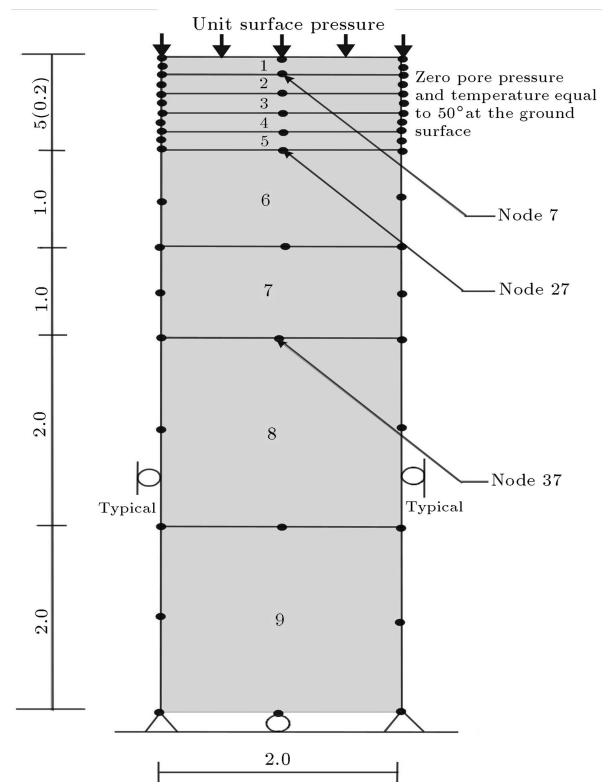


Figure 4. Plane strain thermo-elastic consolidation.

et al. [36], in which these two matrices are set to zero. At the beginning of the analysis, a nine-point integration scheme was used to reduce oscillation in the results. However, since no significant improvement was observed, a four-point integration scheme was employed.

The results are shown in Figures 5 to 7. Figure 5 shows that displacements at nodes 7, 27 and 37 agree well with the results obtained by Lewis et al. [36], except that the peak values are a little higher. After the peak, displacements become negative (i.e. heave). The same result is reported by Lewis et al. [36] for values after the peak. Figure 6 shows the variation of calculated pore pressure, which clearly indicates the dissipation of pore pressure with time. However, the results of this study show that the rate of pore pressure dissipation is slower than that reported by Lewis et al. [36]. It should be noted that calculating pore pressure is the most difficult part of the analysis, since it is very sensitive to time increment Δt and oscillation may occur at early times. Figure 7 demonstrates an excellent match between the calculated temperature in this study and those given by Lewis et al. [36].

Modeling Axisymmetric Thermal Consolidation Around a Buried Heat Source

The effects of a cylindrical radiating heat source, buried in a thermo-elastic soil, were investigated by Booker and Savvidou [38], where an analytic solution for a

Table 1. Input data for thermoelastic consolidation and fracture problems.

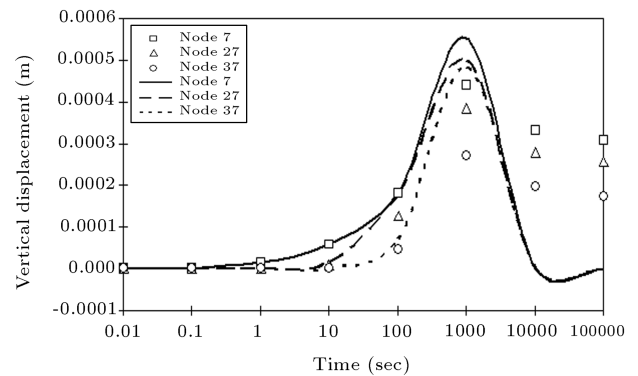
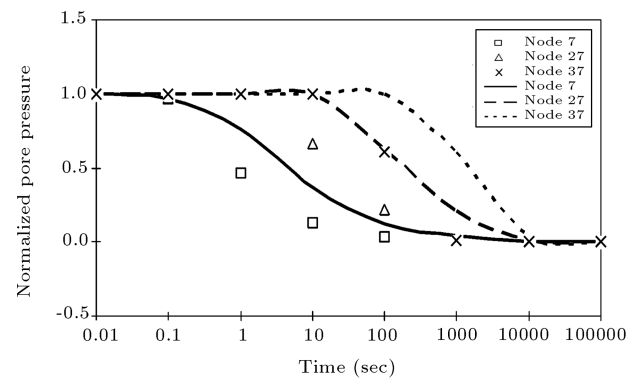
Parameters	Plane Strain Analysis	Axisymmetric Analysis	Fracture Simulation
Mass coefficient ($\text{kN/m}\cdot\text{sec}^{-2}$)	0.00	0.00	0.00
Damping coefficient ($\text{kN/m}\cdot\text{sec}^{-1}$)	0.00	0.00	0.00
Soil/rock thermal expansion($1/^{\circ}\text{C}$)	0.9×10^{-6}	0.203×10^{-6}	0.9×10^{-6}
Fluid thermal expansion ($1/^{\circ}\text{C}$)	0.00	0.630×10^{-5}	0.1×10^{-5}
Fluid compressibility (kPa^{-1})	0.00	0.00	0.5×10^{-3}
Soil heat capacitance ($\text{J/m}^3\cdot^{\circ}\text{C}$)	40.0	40.0	5.00
Fluid heat capacitance ($\text{J/m}^3\cdot^{\circ}\text{C}$)	40.0	40.0	0.00
Thermal conductivity ($\text{J/sec}\cdot\text{m}\cdot^{\circ}\text{C}$)	0.20	1.03	20.0
Soil density (ton/m^3)	0.00	0.00	0.00
Fluid density (ton/m^3)	1.00	1.00	1.00
Fluid viscosity ($\text{kPa}\cdot\text{sec}$)	0.1×10^{-5}	0.1×10^{-5}	0.1×10^{-5}
Absolute permeability (m^2)	0.4×10^{-12}	0.4×10^{-11}	5.5×10^{-12}
Modulus of elasticity (kPa)	6000.0	6000.0	$0.6 \times 10^{+8}$
Poisson's ratio	0.40	0.40	0.40
Acceleration of gravity (m/sec^2)	9.81	9.81	9.81
Initial porosity	0.1	0.1	0.3
θ	1.00	1.00	1.00

Table 2. Time increments for thermo-consolidation problems.

Time Increment (seconds)	Number of Time Steps
0.01	10
0.1	10
1	10
10	10
100	10
1000	10

point-heat source was numerically integrated over the surface of a cylindrical canister. Apparently, this is the only ‘analytical solution’ available for such a problem, as reported by Lewis et al. [36] and Vaziri and Britto [39]. A number of validation tests for thermal-hydro-mechanical problems have been proposed by other investigators, e.g. Alonso and Alcoverro [40] and Alonso et al. [41] in the course of the Catsius Clay project.

The finite element mesh depicted in Figure 8 is adopted from Lewis et al. [36]. It consists of 27 elements and 106 nodes. Booker and Savvidou [38] provided an analytical solution for the case of a cylindrical heat source where $\frac{a'}{a_v} = \frac{1}{4}$, $\frac{c}{\kappa} = 2.0$ and $\nu = 0.4$, in which a' is the soil thermal expansion coefficient, ν is the Poisson ratio, c is the coefficient of consolidation, κ is the coefficient of thermal diffusivity

**Figure 5.** Variation of vertical displacement in time (Symbols: From [36], Lines: Finite element model).**Figure 6.** Variation of pore pressure in time (Symbols: From [36], Lines: Finite element model).

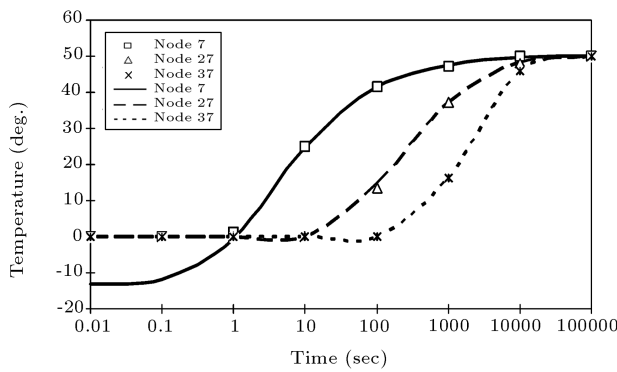


Figure 7. Variation of temperature in time (Symbols: From [36], Lines: Finite element model).

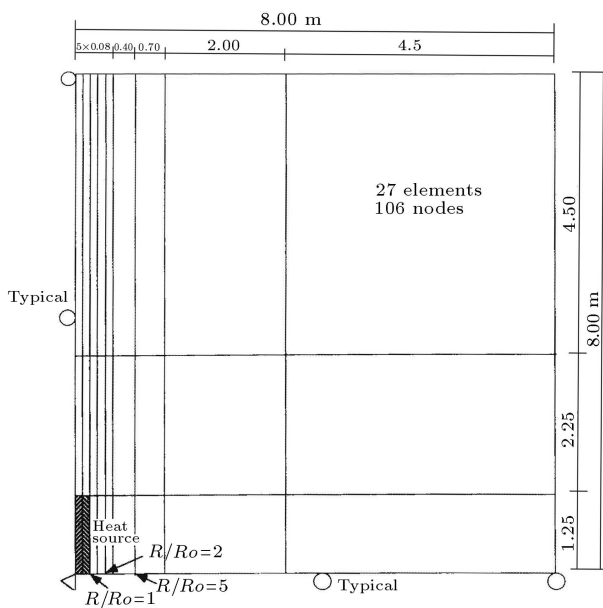


Figure 8. Finite element mesh for axisymmetric thermo-elastic consolidation problem [36].

and $a_u = \beta_S(1 - \phi) + \beta_w(\phi)$, where β_S and β_w are the coefficients of thermal expansion for solid particles and fluid, respectively, and ϕ represents the porosity. The parameters used in the analysis are summarized in Table 1. The heat source was simulated by a constant heat input of 1000.0 J for both elements at the source. Temporal discretization is shown in Table 2.

Results are illustrated in Figures 9 to 11, which show horizontal displacements, pore pressures, and temperatures at three different nodes, $R/R_o=1$, $R/R_o=2$, and $R/R_o=5$ shown in Figure 8 (R_o is the radius of the cylindrical heat source). Figure 9 indicates that displacements gradually increase up to a certain level, then, level off and remain constant when the generated pore pressures are dissipated and the temperatures have reached the steady state condition. Since changes in horizontal displacement have not been addressed in the analytical solution provided by Booker and Savvidou [38], in Figure 9 results

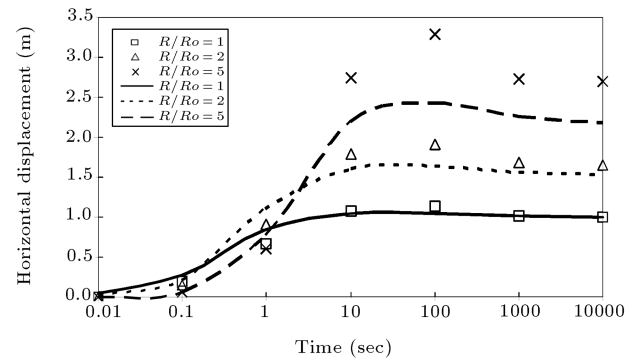


Figure 9. Comparison between analytical and numerical solutions for horizontal displacements (Symbols: [36], Lines: Finite element model).

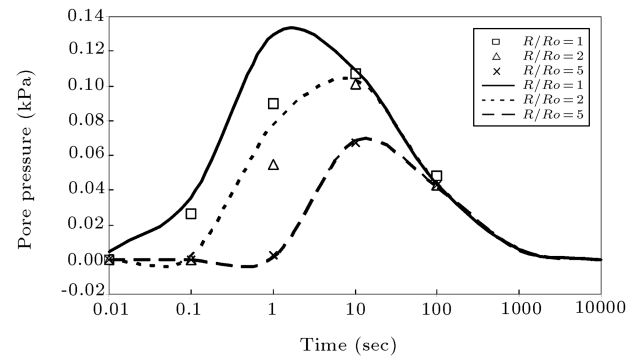


Figure 10. Comparison between analytical and numerical solutions for pore pressure (Symbols: Analytical, Lines: Finite element model).

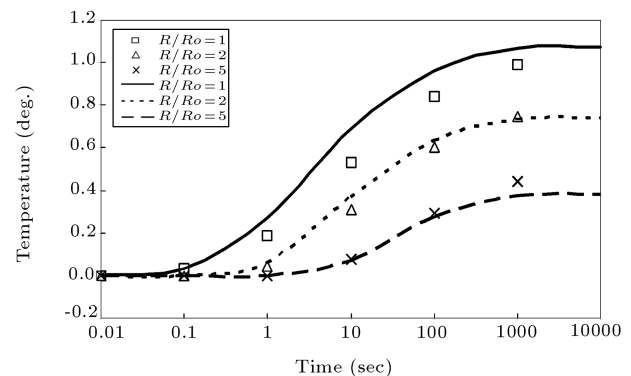


Figure 11. Comparison between analytical and numerical solutions for temperature (Symbols: Analytical, Lines: Finite element model).

of the developed finite element model are compared with those reported by Lewis et al. [36] for the same problem. Figure 10 shows the pore pressure generation and dissipation caused by the radiating heat source. For $R/R_o=1$, the time to reach the maximum pore pressure in the numerical solution is behind the analytical one, but for $R/R_o=2$ and $R/R_o=5$, the maximum values occur at the same time and their

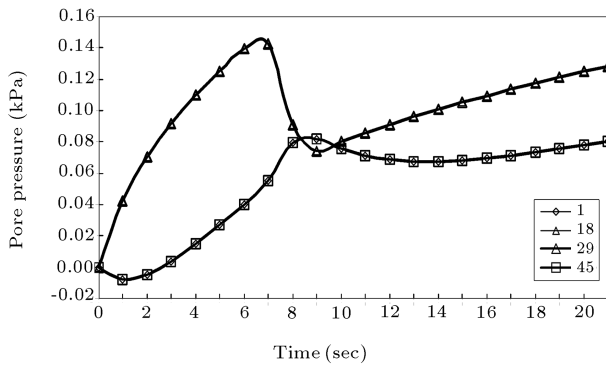


Figure 13. Variation of pore pressure at some nodes in the soil and at the fracture.

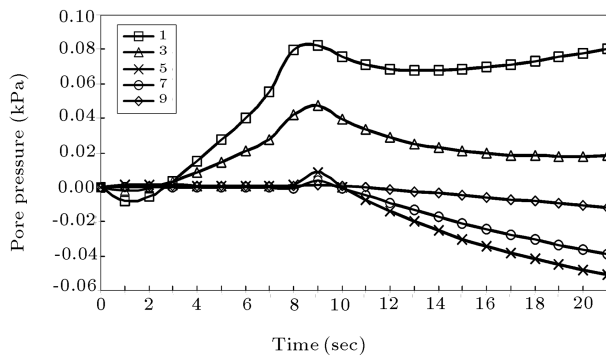


Figure 14. Variation of pore pressure in the soil due to the effect of fracturing.

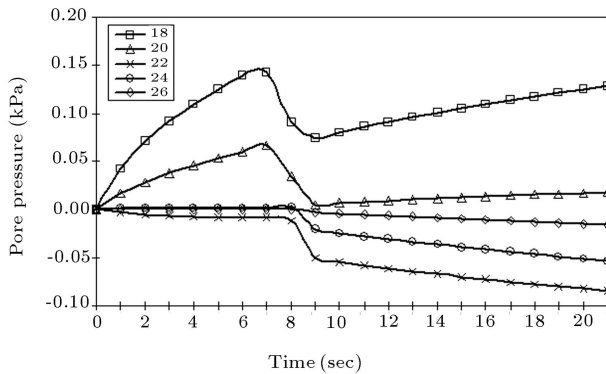


Figure 15. Variation of pore pressure along the fracture.

However, these negative values decrease as the node gets closer to the right boundary where a zero pore pressure is imposed.

Figure 16 compares the variation of temperature at node 18, which is located at the injection zone, and node 1, which is located far from the injection area. As expected, temperature at the injection zone is higher. Variation of temperature along the mesh and also inside the induced fracture is illustrated in Figures 17 and 18, respectively. As the figures show, due to an injection of heated fluid, the temperature

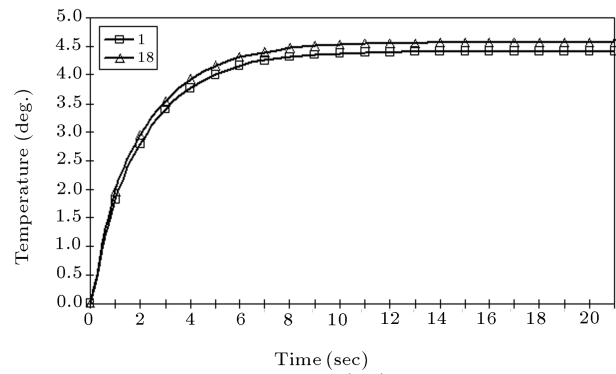


Figure 16. Variation of temperature in the soil and at the fracture.

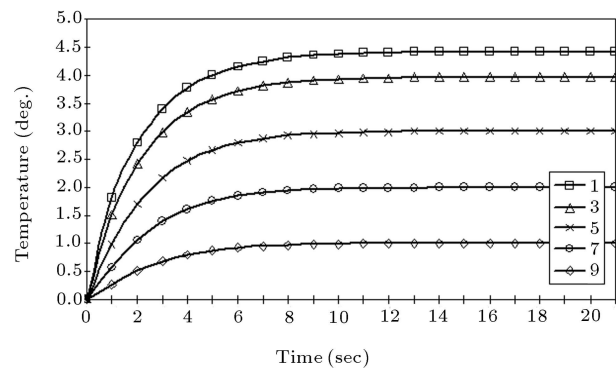


Figure 17. Variation of soil temperature due to the injection of hot fluid.

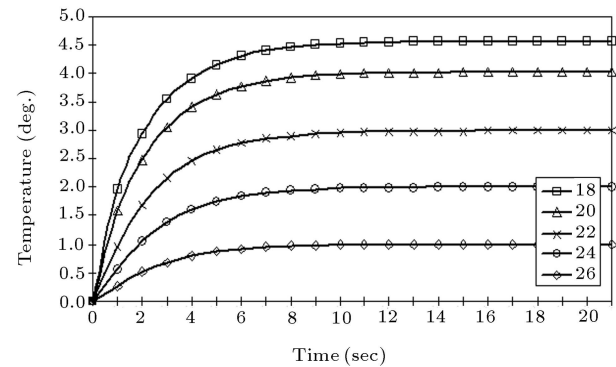


Figure 18. Variation of temperature along the fracture due to the injection of hot fluid.

is gradually and smoothly increasing toward a steady state condition.

Modeling of Large Scale Hydraulic Fracture Laboratory Experiments

A joint CANMET/industry/AOSTRA funded project was undertaken by Golder Associates to perform hydraulic fracturing experiments in a large-scale triaxial chamber. The main objectives of the study were: (1) To provide a better understanding of the mechanism

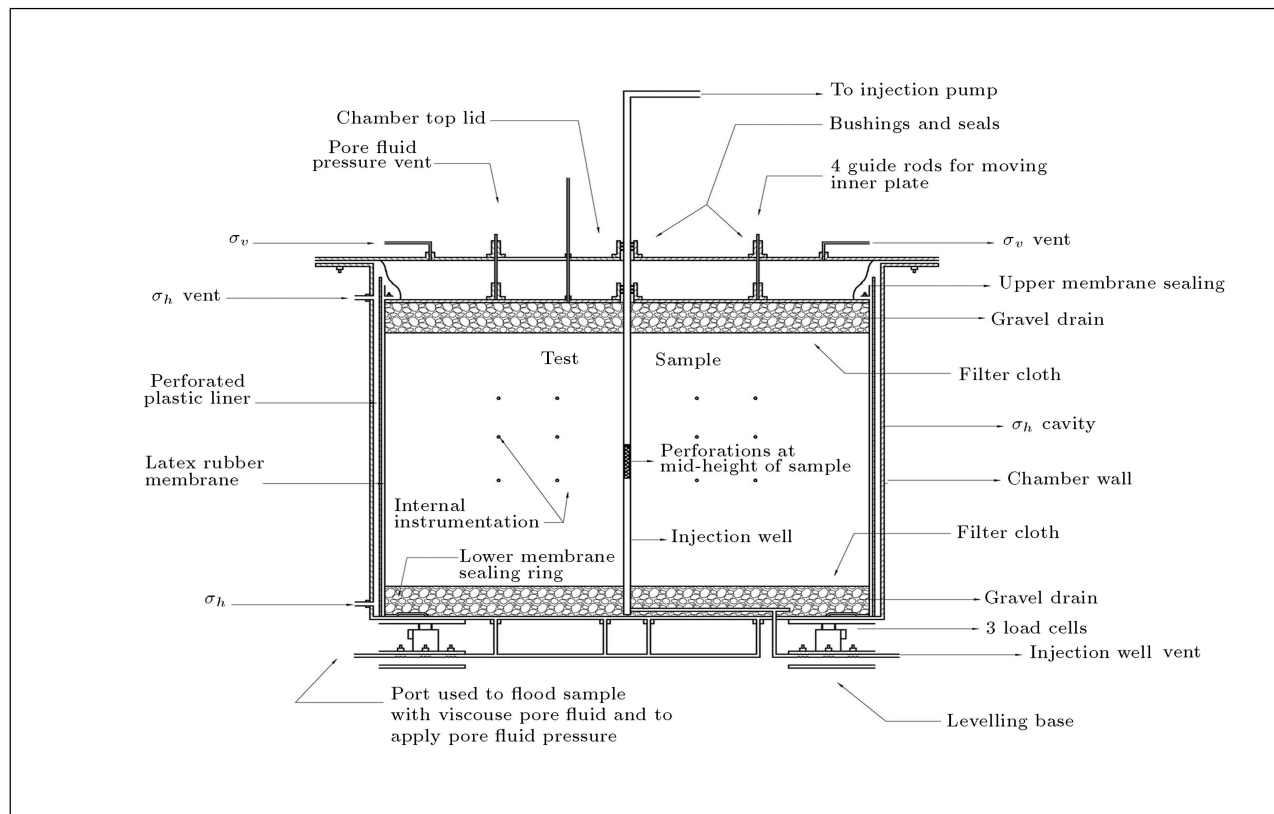


Figure 19. Schematic view of large scale triaxial chamber (not to scale) from Golders Associates Report [42-44].

of hydraulic fracture formation and propagation in uncemented oil sands under conditions of high leak-off and (2) To determine the effect of fluid injection rate and, also, the influence of different stress fields on the fracturing process. These experiments were carried out in a large triaxial stress chamber, shown schematically in Figure 19, which can accommodate samples of up to 1.00 meter high and 1.40 meter in diameter. Quartz sand was used in these experiments, which was saturated with a viscous fluid, such as invert liquid sugar instead of oil, and injected with dyed invert liquid sugar (phases I and II) and dyed water (phase III), in order to trace the fracture. Figure 19 shows a hollow steel pipe, with an outside diameter of 33.5 mm and perforated at mid-height, which was used to simulate the injection well. Principal stresses of up to 1000 kPa could be applied independently in the vertical (σ_v) and radial (σ_h) directions, as illustrated in the figure.

Lane Mountain 125 quartz sand was chosen for the laboratory tests. Its behavior was reported to be similar to oil sand, which exhibits high dilatancy and post peak softening during triaxial compression under low effective confining stresses. The specific gravity of Lane Mountain sand grain was determined to be 2.65 and its permeability was measured to be 4.56×10^{-3} cm/sec to water and 4.0×10^{-6} cm/sec to liquid sugar.

Boundary conditions were free draining at the top and bottom of the chamber, which were connected to a constant pressure equal to +200 kPa. No radial drainage was allowed.

At the end of each test, the sample was excavated in horizontal lifts, normally 1.5 to 3.0 cm in thickness, under black light. When each lift was completely excavated, the locations of the dye were marked with black string and, then, a normal photograph was taken under normal light [42-44].

In this study, test 4 of phase II experiments was selected for numerical modeling. The sample dimensions and position of instrumentation are shown in Figures 20 and 21. Two permeability tests carried out on the saturated sample gave permeability values of 4.9 and 4.6 Darcys. Horizontal and vertical boundary tractions of 600 kPa and 400 kPa, respectively, were applied on the sample, with a back pressure of 200 kPa to keep the sample fully saturated. The $K_0 (= \sigma'_h / \sigma'_v)$ value was equal to 2 for this test, which indicated that horizontal fracture planes were expected. In this test, 250 ml of dyed liquid sugar were injected into the test sample in 8.3 seconds (30 ml/sec.).

A finite element mesh comprised of 704 elements (260 eight-node rectangular elements and 444 six-node fracture elements) with 1562 nodes (including the double nodes) was used. Due to the axial symmetry

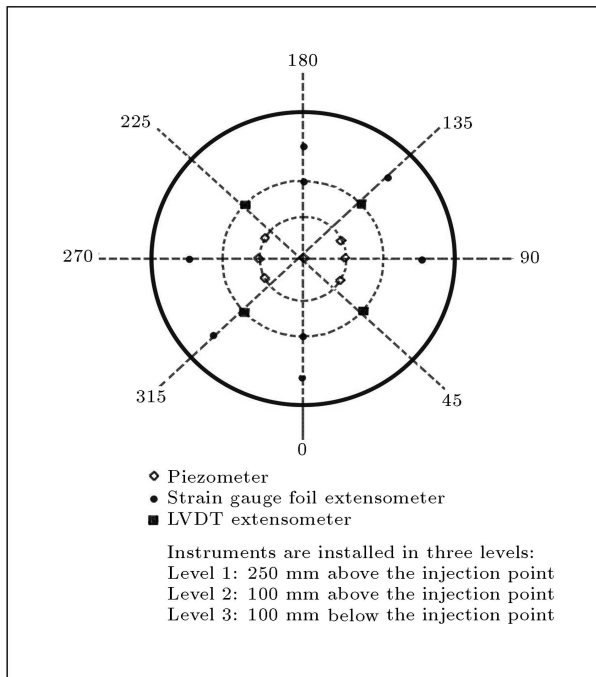


Figure 20. Plan view of instrumentation around the injection zone.

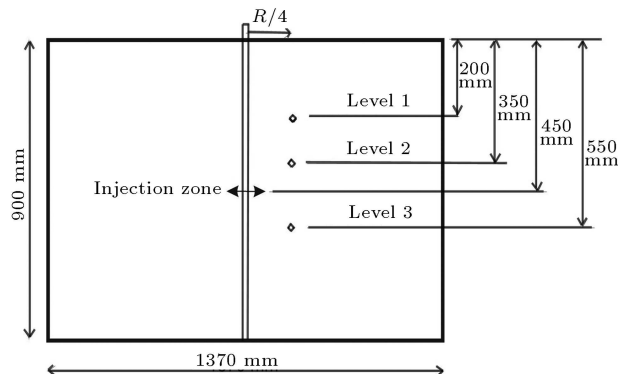


Figure 21. Sample dimensions and position of piezometers for test #4 of phase 2 of the experiments.

of the problem, only half the sample was analyzed, as shown in Figure 22. The boundary conditions were:

- Bottom boundary: Fixed in the horizontal and vertical directions, free drainage,
- Top boundary: Free, free drainage,
- Left boundary: Fixed in the horizontal direction, no drainage allowed,
- Right boundary: Free, no drainage allowed.

An important aspect of the coupling process is finding an appropriate value for time increment, Δt , suitable for all field equations. Due to the high speed of stress waves in soil/rock, the time increment in the equilibrium equation should be small enough to capture the behavior of soil/rock accurately. On the other

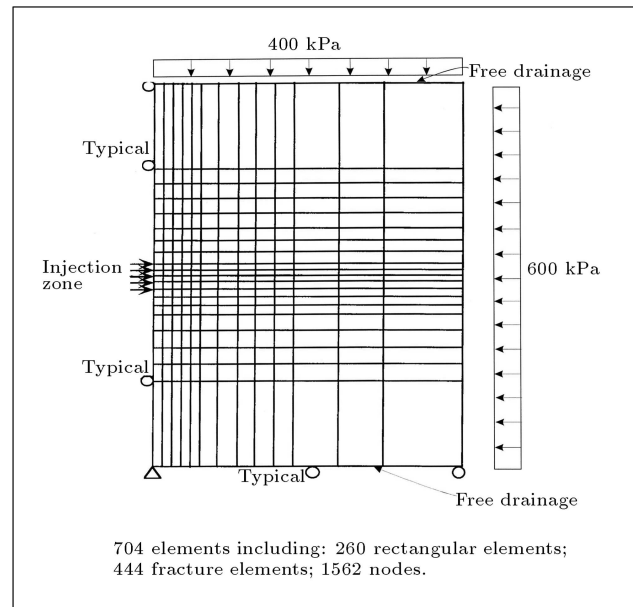


Figure 22. Finite element mesh and boundary conditions for modeling test 4 of phase 2.

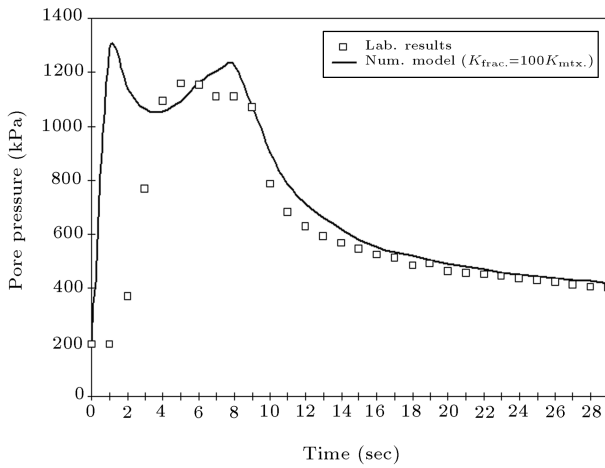
hand, the time increment cannot be very small because the coupled analysis of the consolidation phenomenon requires that Δt be larger than some certain value in order to avoid instability and spurious oscillations [45,46]. The time increment for this analysis was chosen to be one second.

An axisymmetric analysis was carried out considering the linear elastic behavior for sand with an elastic modulus equal to 41050 kPa and a Poisson ratio of 0.25. These values were obtained from small scale triaxial tests on Lane Mountain sand. The permeability of the fracture elements was considered to be 100 times greater than the surrounding soil matrix ($100 k_{soil}$). In this analysis, nodal coordinates were not updated and a nominal thickness equal to 2 mm was considered for the fracture elements. This is close to the width of the real fractures in oil sands, which is 3 to 5 mm [13]. A list of the parameters used in the analysis is summarized in Table 4.

The test was simulated by injecting fluid at the perforated area of the wellbore. An injection rate of 30 ml/sec in this test is equal to an injection flux of 0.0052 m/sec when divided by the perforated area. The variation of pore fluid pressure at the injection zone is shown in Figure 23. Although the calculated peak pressure is slightly higher than the measured pressure, the overall behavior is very similar. The initial slopes of the two curves are different; this is because, in the finite element analysis, the stresses were examined at the end of each time step to identify the possibility of fracture. For instance, if the time increment is 1 second, no fracturing will occur until the end of the time increment. Obviously, in reality, fractures can

Table 4. List of parameters for modeling of thermo-elastic consolidation and hydraulic fracture problems.

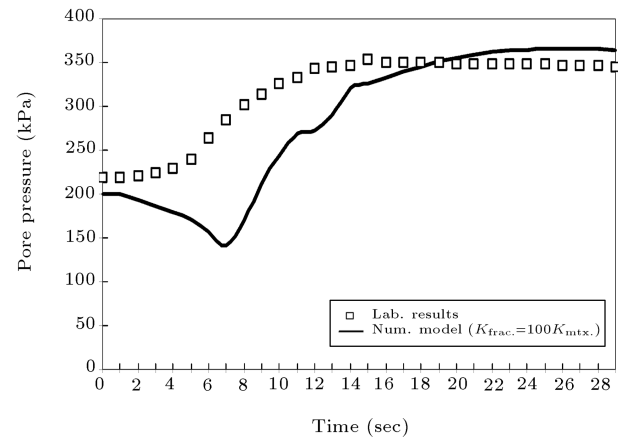
Parameters	Hydraulic Fracture Problem
Mass coefficient ($\text{kN/m}\cdot\text{sec}^{-2}$)	0.00
Damping coefficient ($\text{kN/m}\cdot\text{sec}^{-1}$)	0.00
Soil/rock thermal expansion ($1/^\circ\text{C}$)	-
Fluid thermal expansion ($1/^\circ\text{C}$)	-
Fluid compressibility (kPa^{-1})	0.3×10^{-5}
Soil heat capacitance ($\text{J/m}^3\cdot^\circ\text{C}$)	-
Fluid heat capacitance ($\text{J/m}^3\cdot^\circ\text{C}$)	-
Thermal conductivity ($\text{J/sec}\cdot\text{m}\cdot^\circ\text{C}$)	-
Soil density (ton/m^3)	2.0
Fluid density (ton/m^3)	1.33
Fluid viscosity ($\text{kPa}\cdot\text{sec}$)	1.49×10^{-3}
Absolute permeability (m^2)	$4.48 \times 10^{-12} - 4.48 \times 10^{-10}$
Modulus of elasticity (kPa)	41050.0
Poisson's ratio	0.25
Acceleration of gravity (m/sec^2)	9.81
Initial porosity	0.48
θ	1.00

**Figure 23.** Comparison between calculated and measured pore pressures (piezometer: At injection zone).

occur in a fraction of second, resulting in a higher rate of flow and lower pressure.

As seen in Figure 23, there is a jump in the pore pressure at the beginning of injection, followed by a fairly constant pore pressure during the injection. At the end of injection, both calculated and measured curves show a decline in pore pressure, which represents the consolidation phenomenon.

Pore pressures at the piezometers, installed at a distance of 75 mm from the injection pipe (Figures 20 and 21), are compared to the numerical solution in

**Figure 24.** Comparison between pore pressure variation of lab experiment and numerical model at the piezometer (100 mm above the injection zone).

Figures 24 and 25. Piezometers were installed at three levels, but the lower one did not show a significant change in pore pressure. A good agreement between the numerical results and measured values in the laboratory can be observed.

The fracture pattern obtained from the numerical model is shown in Figure 26. The sequence shows the fracture pattern at the onset of injection, 4 seconds after starting injection, 8 seconds after starting injection (end of injection), and at 30 seconds. The numerical model showed a fracture zone, which gradually ex-

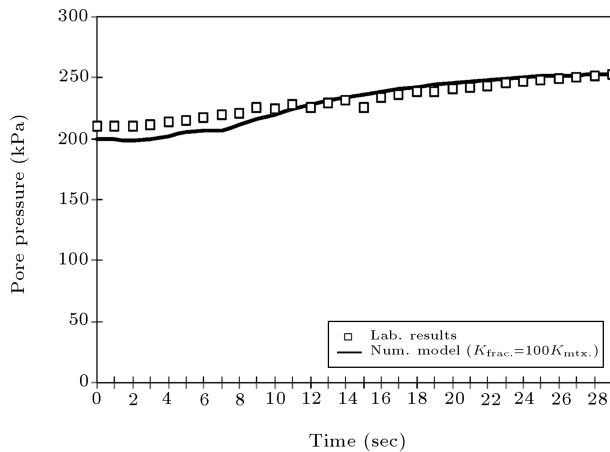


Figure 25. Comparison between pore pressure variation of lab experiment and numerical model at the piezometers (100 mm below the injection zone).

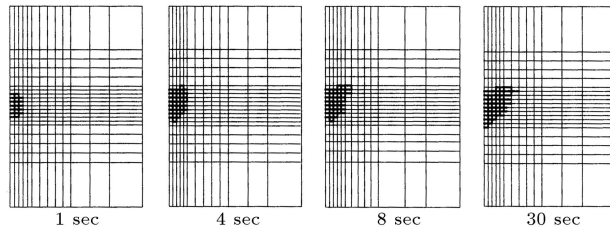


Figure 26. Pattern of fracture propagation from numerical model.

panded with injection. The actual fracture pattern observed in the laboratory is shown in Figure 27. Despite the fact that $K_o = 2.0$, neither the numerical model nor the experimental results showed the anticipated planar fracture. Studies on pore pressure distribution inside the medium indicated that fracture occurs at places with higher pore pressure. In other words, the contours of higher pore pressure can approximately determine the zone of fracturing [47].

Fracture Propagation in an Elastoplastic Material

In petroleum engineering, it is known that the compressibility of oil sand is nonlinear at low stresses (e.g. [14]). In geotechnical terms, this basically means that the stress-strain behavior of oil sand is nonlinear and its bulk modulus (stiffness) varies with changes in stress. Some researchers have considered a nonlinear elastic (hyperbolic) model for simulating this behavior [48], while others have proposed an elastoplastic constitutive model (e.g. [49]). In this study, in order to evaluate the effects of soil failure on fracture patterns in isothermal conditions, an associated Mohr-Coulomb model was employed. This model is capable of simulating high dilation, which is an important characteristic of oil sand. In this model, the following

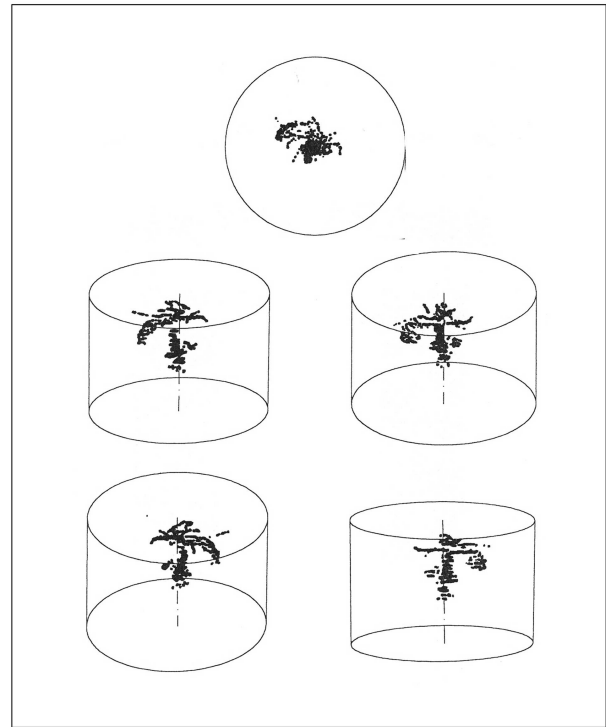


Figure 27. Fracture pattern from laboratory experiment reproduced from Golder Associate Report [43].

parameters were used:

$$\begin{aligned} C_p &= 0, & C_r &= 0, \\ \phi_p &= 38^\circ, & \phi_r &= 38^\circ, \\ E &= 41050 \text{ kPa}, & \nu &= 0.25, \end{aligned}$$

where C_p is the peak cohesion, C_r is the residual cohesion, ϕ_p represents the peak friction angle, ϕ_r means the residual friction angle and E and ν represent the modulus of elasticity and Poisson ratio, respectively.

Boundary tractions of 600 kPa horizontal and 400 kPa vertical, with 200 kPa back pressure were applied on the sample. According to the Mohr-Coulomb failure criterion, the ratio of the principal stresses at yielding is given by:

$$\frac{\sigma_1 - \sigma_3}{2} = \frac{\sigma_1 + \sigma_3}{2} \sin \phi + C \cos \phi. \quad (42)$$

For $C = 0$ and $\phi = 38^\circ$;

$$\frac{\sigma_1 - \sigma_3}{2} = \frac{\sigma_1 + \sigma_3}{2} \sin 38^\circ \rightarrow \frac{\sigma_1}{\sigma_3} = 4.2.$$

Hence, at places where this ratio applies, soil becomes plastic and stresses and pore pressures are affected, accordingly. The pore pressure variation at the injection zone is shown in Figure 28. In this figure, the results of the analysis, with different permeabilities for the fracture elements (500 and 1000 times greater than the permeability of the surrounding soil), are included. In general, the initial pore pressure in this case shows

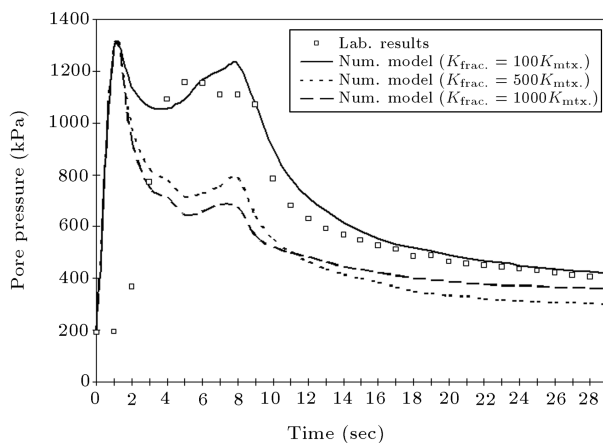


Figure 28. Pore pressure variation at the injection zone with different permeabilities for fracture elements.

around 30% higher pore pressure compared to the elastic case. The effect of increasing the permeability of fracture elements on reducing pore pressure can be observed in this figure.

Fracture patterns for elastoplastic analysis are depicted in Figure 29. Compared to the fracture patterns of elastic analysis, they are less dispersed and the fracture zones are smaller. The numerical model, in this case, indicates that tensile and shear fractures can simultaneously occur in the hydraulic fracturing process. Despite the fact that the shear failure zone is small, the dilation characteristics of the material will generate compressive stresses in a confined condition, which can inhibit fracture growth. This explains why there is a less dispersed fracture zone in the elastoplastic analysis.

CONCLUSIONS

A fully coupled thermal hydro-mechanical fracture finite element model is developed, which is able to simulate the process of hydraulic fracturing under isothermal and non-isothermal conditions. The modeling of large scale hydraulic fracturing laboratory experiments in uncemented porous materials, such as sand, has provided results, which are in agreement with experimental observations. In this model, the

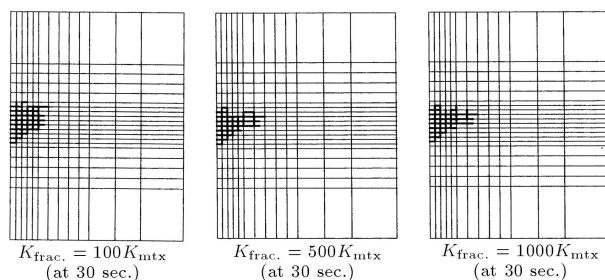


Figure 29. Fracture pattern with associated Mohr-Coulomb model.

importance of the amount of pore pressure and its distribution is emphasized in the process of hydraulic fracturing in uncemented porous materials. The fracture pattern is roughly similar to the contours of high pore pressure. The numerical model shows that a change in the permeability of soil and/or fractures has a drastic effect on the variation of pore pressure and the resulting fracture pattern.

The model establishes that, in uncemented porous materials, tensile and shear fractures can occur simultaneously. The numerical model and laboratory experiments both indicate that, for uncemented porous materials, such as oil sands, a simple planar fracture is unlikely to occur and a system of multiple fractures or a fracture zone consisting of interconnected tiny cracks should be expected.

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NOMENCLATURE

σ_{ij}	stress tensor at a point
F_i	external load vector
U_i	displacement vector i.e. $\langle u \ v \ w \rangle^T$
m'	mass coefficient
c'	damping coefficient
i, j	indices taking 1, 2 and 3 representing coordinate axes
ω	weighting factor
n_j	unit vector normal to the surface
S	surface boundary
V	volume
σ'_{ij}	effective stress tensor (tension positive)
ΔP	change in pore fluid pressure (compression positive)
δ_{ij}	Kronecker delta
D_{ijkl}	soil/rock constitutive matrix
ε_{kl}	(total) strain tensor
α_S	coefficient of thermal expansion for soil/rock (porous matrix)
ΔT	change in temperature
ρ	density of fluid
v	velocity vector of flowing fluid
G	fluid mass output (sink) or input (source)
ϕ	porosity of soil mass

t	time
∇	del operator
α_S	coefficient of thermal expansion for soil/rock
α_P	coefficient of thermal expansion for fluid
β_T	fluid compressibility
ε_V	volumetric strain
L_e	volumetric thermal energy flux
E	internal energy per unit mass
ρ	fluid density
Q	energy input (source) or output (sink) per unit volume
t	time
ϕ	porosity of soil/rock matrix
ρ_S	soil/rock density
C_s	heat capacity of soil/rock
ρ_f	fluid density
S	degree of saturation
λ	coefficient of conductivity
f_i	volumetric flux of flowing fluid
g	acceleration of gravity
z	elevation
J	mechanical equivalent of heat
C_v	heat capacity of fluid at constant volume
C_p	heat capacity of fluid at constant pressure
T	temperature
T_o	initial temperature

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