A node enrichment strategy in collocated discrete least squares meshless method for the solution of generalized Newtonian fluid flow

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Node enrichment; Meshless methods; Carreau-Yasuda fluid; Least squares technique.

\begin{abstract}
A simple node enrichment strategy using a gradient based error estimator is presented for the Collocated Discrete Least Squares (CDLS) meshless method. Also, a procedure is defined to distribute collocation points according to the field nodes position. Here, shape functions are constructed using the Radial Point Interpolation Method (RPIM). As temporal discretization, a first-order accurate scheme, named the semi-incremental fractional step method, is used. One of the advantages of this scheme is its capability of using large time step sizes for the solution of governing equations on steady state problems. The capability of the presented strategy is shown by investigating the Carreau-Yasuda fluid flow model in solving lid-driven cavity flow problems with different curve fitting indices values.
\end{abstract}

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1. Introduction

There are numerous studies about the numerical simulation of non-Newtonian fluid flow (see [1]). Most of these investigations are performed in a finite element and finite volume field. Using a mesh or grid is a basic characteristic of these conventional numerical methods for the solution of governing equations. During recent years, significant efforts have been devoted to the development of so-called meshless or meshfree methods. The purpose of this methodology is to get rid of the structure of the mesh and to approximate the solution using scattered nodes inside and on the boundaries of the domain. A detailed review on meshless methods is provided by Belytschko [2], Liu [3] and Liu and Gu [4]. Each efficient numerical method should possess some properties, such as a strong mathematical basis, simplicity and parameter independency. The CDLS method is a truly meshless method based on a simple least squares principle. Initially, Arzani and Afshar [5] developed the Discrete Least Squares (DLS) meshless method for the solution of Poisson equations. The main idea was adopted from the least squares technique in FEM. Subsequently, Afshar and Lashkarbolok [6] used collocation points in the DLS method and developed the CDLS meshless method. According to their research, collocation points have significant effects on the performance of the method. Recent research into the CDLS method can be found in [7-10].

It is desirable to refine the spatial domain where the numerical errors are high. However, sometimes there is not a priori knowledge about the distribution of the numerical errors. Adaptive refinement strategies based on error estimators are useful tools to improve the efficiency of the numerical methods by refining the computational domain where it is needed [11]. These
methods have been extensively used by finite element practitioners to solve various engineering problems [12]. Several error estimates and adaptive refinement methods have also been proposed for meshless methods. An adaptive refinement strategy, based on a node-moving methodology, was developed in conjunction with the collocated method for one-dimensional hyperbolic problems by Afshar and Lashkarbolok [6]. The method was extended by Firoozjaee and Afshar [13] for the adaptive solution of hyperbolic problems in two dimensions. The adaptive refinement technique based on the node-moving strategy is extended for the adaptive solution of incompressible Navier-Stokes equations [11]. In that node-moving strategy, the value of a least squares functional of the residual of the governing differential equation at nodal points (or field nodes) is considered a measure of the error and is used to estimate the distribution of the numerical error. The node-moving technique is then employed to relocate the field nodes such that more nodes are used to represent areas of the problem domain with large errors. The problem is then resolved on the refined distribution of nodes for higher accuracy. In this study, a simple node enrichment process, along with a gradient based error estimator, is presented for the CDLS method in the context of generalized Newtonian fluid flow. Errors are estimated by considering both velocity and viscosity gradients. Since, for more field nodes, more collocation points are needed to calculate residuals more accurately, a strategy is presented to allocate collocation points according to the field nodes positions. As temporal discretization, a fractional step method is used. The fractional step method performs the advance in time in three main steps: First, the momentum equation is used to calculate an intermediate velocity and then, in the second step, the pressure is evaluated using the intermediate velocity. Finally, in the third step, the velocity can be calculated using the intermediate velocity and pressure. Several fractional step methods have been introduced in the literature. The non-incremental fractional step method proposed by Chorin [14] is one of the most popular fractional step methods. Another well-known method, the incremental fractional step method, was proposed by modifying the method of Chorin through adding the previous value of the pressure gradient to the momentum equation [15]. The incremental fractional step method and its variants need to satisfy the LBB (inf-sup) condition to lead to a stable solution [16]. On the contrary, the non-incremental fractional step method and its variants are not required to satisfy the LBB condition [16]. Despite this advantage, unfortunately, they yield inaccurate solutions when large time step sizes are used [17]. Dealing with steady-state problems, it is favourable to use large time step sizes to reduce the computational effort. Recently, Firoozjaee and Afshar [9] presented a new fractional step method, named the semi-incremental fractional step method, to use the advantages of the incremental fractional step method without suffering from LBB condition satisfaction. In this study, the proposed method in [9] is used for temporal discretization of generalized Newtonian fluid equations.

2. CDLS meshless method

The CDLS meshless method formulation was given in [6] and [13]. Here, this formulation is given again in more detail. Consider the general form of a partial differential equation:

\[ \mathcal{S}(u) = f \quad \text{in} \quad \Omega, \]  
\[ \mathcal{R}(u) = g \quad \text{on} \quad \Gamma_t, \]  
\[ u = \bar{u} \quad \text{on} \quad \Gamma_u. \]  

Here, \( u \) denotes the unknown function, \( \mathcal{S} \) and \( \mathcal{R} \) are some proper differential operators defined on the problem domain, \( \Omega \), and its Neumann boundary, \( \Gamma_t \), respectively. \( \Gamma_u \) represents the Dirichlet boundary with a prescribed value of \( \bar{u} \), and \( f \) is the source term in the problem domain. The philosophy of the least squares method is to find an approximate solution that minimizes the least squares functional to be defined later. As shown in Figure 1, the problem domain and its boundaries are discretized by field nodes and collocation points. Assume \( n_p \) is the number of nodes in the domain and on the boundaries. Besides field nodes, collocation points are used in the problem domain and on its boundaries. In this methodology, in each field node, one collocation point has to be placed, as shown in Figure 1. The approximated value of function \( u \) at collocation point \( k \), with coordinate \( x_k \), can be obtained through the following interpolation:

\[ u(x_k) = \sum_{i=1}^{n_i} N_i(x_k) u_i, \]  

Figure 1. The domain discretized by field nodes (circles) and collocation points (cross signs).
where \( u_i \) is the value of the unknown function at the \( i \)th field node. \( m_k \) is the number of field nodes that the \( k \)th collocation point, with coordinate \( x_k \), has in its domain. This idea of compact support is shown in Figure 2. To set up such a domain for each collocation point, radius \( ds \) is defined so that a specific number of field nodes are placed into its support domain. In Eq. (4), \( N_i(x_k) \) is the value of the shape function of the \( i \)th node at the \( k \)th collocation point, which will be defined later. In this paper, first, the number of nodes to support the collocation points is defined as \( m_k \). Then, for each collocation, a radius (\( ds \)) is determined so that \( m_k \) nodes are placed in the domain of that collocation. Substitution of Eq. (4) into Eqs. (1)-(3) leads to the differential equation residual (\( R^d \)), the Neumann boundary condition residual (\( R^\partial \)) and the Dirichlet boundary condition residual (\( R^u \)) defined as follows, respectively:

\[
R^d_k = \mathcal{N}(u(x_k)) - f(x_k)
\]

\[
= \sum_{i=1}^{m_k} \mathcal{N}(i(x_k)) u_i - f(x_k) \quad (k = 1 \sim M), (5)
\]

\[
R^\partial_k = \mathcal{H}(u(x_k)) = g(x_k)
\]

\[
= \sum_{i=1}^{n_u} \mathcal{H}(i(x_k)) u_i - g(x_k) \quad (k = 1 \sim n_u), (6)
\]

\[
R^u_k = u(x_k) - \bar{u} = \sum_{i=1}^{n_u} (N_i(x_k)) u_i - \bar{u} \quad (k = 1 \sim n_u).
\]

In these relations, \( n_i \) and \( n_u \) are the number of collocation points located on the field nodes in the Neumann and Dirichlet boundaries, respectively. \( M \) is the total number of collocation points. Now, the following least squares functional of all residuals at all collocation points can be constructed as:

\[
J = \frac{1}{2} \left( \sum_{k=1}^{M} \left[ R^d_k \right]^2 + \alpha \sum_{k=1}^{n_u} \left[ R^\partial_k \right]^2 + \beta \sum_{k=1}^{n_u} \left[ R^u_k \right]^2 \right).
\]

Parameters \( \alpha \) and \( \beta \) in this equation represent the relative weight of the boundary residuals, with respect to the interior residuals, named penalty coefficients.

Minimization of Eq. (8), with respect to parameters \( u_i \) leads to the following system of linear equations:

\[
K U = F,
\]

in which \( U \) is the vector of parameters in field nodes. The typical components of matrix \( K \) and the right hand side vector, \( F \), are defined as:

\[
K_{ij} = \sum_{k=1}^{M} \mathcal{N}(i(x_k)) \cdot \mathcal{N}(j(x_k))
\]

\[
+ \alpha \sum_{k=1}^{n_u} \mathcal{H}(i(x_k)) \cdot \mathcal{H}(j(x_k))
\]

\[
+ \beta \sum_{k=1}^{n_u} N_i(x_k) N_j(x_k) \quad i, j = 1, \ldots, n_u. (10)
\]

\[
F_i = \sum_{k=1}^{M} \mathcal{N}(i(x_k)) f(x_k) + \alpha \sum_{k=1}^{n_u} \mathcal{H}(i(x_k)) g(x_k)
\]

\[
+ \beta \sum_{k=1}^{n_u} N_i(x_k) \bar{u} \quad i = 1, \ldots, n_u. (11)
\]

The stiffness matrix, \( K \), in Eq. (9) is symmetric, even for non-self-adjoint operators. The size of \( K \) just depends on the number of field nodes \( (n_u) \), and the number of collocation points \( (M) \) does not increase the size of the final system of equations. It is also sparse since a small number of nodes contribute to the function evaluation for a collocation point. Therefore, the final system of equations can be solved by effective iterative solvers.

3. Governing equations

Governing equations are comprised of continuity, momentum and constitutive equations for the two dimensional incompressible flow of a generalized Newtonian fluid. They are in Cartesian coordinates given by:

\[
\frac{\partial u^s}{\partial t^s} + u^s \frac{\partial u^s}{\partial x^s} + v^s \frac{\partial u^s}{\partial y^s} = - \frac{1}{\rho^s} \frac{\partial P^s}{\partial x^s}
\]

\[
+ \frac{1}{\rho^s} \left( \frac{\partial P^s}{\partial x^s} + \frac{\partial P^s}{\partial y^s} \right).
\]
\[
\frac{\partial v^*}{\partial x^*} + u^* \frac{\partial v^*}{\partial y^*} + v^* \frac{\partial v^*}{\partial y^*} = - \frac{1}{\rho^*} \frac{\partial P^*}{\partial y^*} + \frac{1}{\rho^*} \left( \frac{\partial r_{xy}^*}{\partial x^*} + \frac{\partial r_{xy}^*}{\partial y^*} \right), \quad (13)
\]

\[
\frac{\partial u^*}{\partial x^*} + \frac{\partial v^*}{\partial y^*} = 0, \quad (14)
\]

\[
\tau_{xx}^* = 2\eta^* \frac{\partial u^*}{\partial x^*}, \quad (15)
\]

\[
\tau_{xy}^* = \tau_{yx}^* = \eta^* \left( \frac{\partial u^*}{\partial y^*} + \frac{\partial v^*}{\partial x^*} \right), \quad (16)
\]

\[
\tau_{yy}^* = 2\eta^* \frac{\partial v^*}{\partial y^*}, \quad (17)
\]

where \( u^* \), \( v^* \) and \( P^* \) are the velocity component in the \( x \) direction, the velocity component in the \( y \) direction and the pressure, respectively. \( \eta^* \) is the generalized Newtonian viscosity which depends on the local shear rate (under isothermal conditions). In Newtonian fluid, \( \eta^* \) is constant for the entire flow field. In this study, the Carreau-Yasuda model is used to describe the fluid viscosity behaviour. It is given by the following formula:

\[
\eta^* = \eta_{\infty} + (\eta_0^* - \eta_{\infty}^*) \left[ 1 + (\lambda^*)^n \right]^{\frac{1}{n}}, \quad (18)
\]

where \( \gamma^* \), \( \lambda^* \), \( n \), \( \eta_{\infty}^* \), \( \eta_0^* \) and \( \alpha \) are the second invariant of the rate of the deformation tensor, characteristic time, power index, infinite shear rate viscosity, zero shear rate viscosity and a dimensionless parameter, respectively. \( \gamma^* \) in the Cartesian coordinate is defined by:

\[
\gamma^* = 2 \left( \frac{\partial u^*}{\partial x^*} \right)^2 + 2 \left( \frac{\partial v^*}{\partial y^*} \right)^2 + \left( \frac{\partial u^*}{\partial y^*} + \frac{\partial v^*}{\partial x^*} \right)^2. \quad (19)
\]

The above equations can be non-dimensionalized through selection of appropriate scales, as follows:

\[
t = \frac{t^* U_0}{L}, \quad x = \frac{x^*}{L}, \quad y = \frac{y^*}{L}, \quad u = \frac{u^*}{L_0}, \quad \rho = \frac{\rho^*}{\rho_0}, \quad P = \frac{P^*}{\rho_0 U_0^2}, \quad \eta = \frac{n_0}{\eta_0^*}, \quad \text{Cu} = \frac{\lambda^* U_0}{L_0}, \quad (20)
\]

where \( U_0 \), \( L_0 \), \( \lambda_0 \) and \( \text{Cu} \) are the reference values of density, velocity, length, characteristic time and Carreau number, respectively. Using constitutive equations, Eqs. (12)-(13) in dimensionless form are given by:

\[
\frac{\partial u}{\partial x} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = - \frac{\partial P}{\partial x} + \frac{1}{Re} \left[ \frac{\partial \eta}{\partial x} \frac{\partial u}{\partial x} \right], \quad (20)
\]

\[
\frac{\partial v}{\partial x} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = - \frac{\partial P}{\partial y} + \frac{1}{Re} \left[ \frac{\partial \eta}{\partial y} \frac{\partial v}{\partial y} \right], \quad (21)
\]

where:

\[
Re = \frac{\rho_0 U_0 L_0}{\eta_0^*}. \quad (22)
\]

Re and \( \rho_0 \) are Reynolds number and reference density, respectively. The above equations are analogous to the following vectorized equation:

\[
\frac{\partial \mathbf{U}}{\partial \tau} + \mathbf{U} \cdot \nabla \mathbf{U} = -\nabla P + \frac{1}{Re} \left( \mathbf{A} \frac{\partial \mathbf{U}}{\partial \tau} \right) + \mathbf{B} \frac{\partial \mathbf{U}}{\partial y} + \mathbf{C} \frac{\partial^2 \mathbf{U}}{\partial x^2} + \mathbf{D} \frac{\partial^2 \mathbf{U}}{\partial y^2} + \mathbf{E}, \quad (23)
\]

where:

\[
\mathbf{U} = \begin{bmatrix} u \\ v \end{bmatrix}, \quad \mathbf{A} = \begin{bmatrix} \frac{\partial \eta}{\partial \tau} & 0 \\ 0 & \frac{\partial \eta}{\partial \tau} \end{bmatrix}, \quad \mathbf{B} = \begin{bmatrix} 0 & \frac{\partial \eta}{\partial \tau} \\ \frac{\partial \eta}{\partial \tau} & 0 \end{bmatrix}, \quad \mathbf{C} = \begin{bmatrix} 0 \\ 0 \end{bmatrix}, \quad \mathbf{D} = \begin{bmatrix} 0 & \frac{\partial \eta}{\partial \tau} \\ \frac{\partial \eta}{\partial \tau} & 0 \end{bmatrix}, \quad \mathbf{E} = \begin{bmatrix} 0 \\ 0 \end{bmatrix}. \quad (24)
\]

4. Temporal discretization

Temporal discretization of the equations in their primitive form is performed by the fractional step method. Fractional step methods perform the advance in time in three main steps; first, the momentum equation is used to obtain the intermediate velocity, \( \mathbf{U}^t \). Then, in the next step, the pressure is evaluated using the intermediate velocity. Finally, in the third step, the velocity is calculated using the intermediate velocity.
and the pressure. In this method, the split form of the
momentum equation is written as follows:

\[
\frac{U' - U^\lambda}{\Delta t} + u^\lambda \frac{\partial U'}{\partial x} + v^\lambda \frac{\partial U'}{\partial y} = \frac{1}{Re} \left( A \frac{\partial \mathbf{U'}}{\partial x} \right. \\
\left. + B \frac{\partial U'}{\partial y} + C \frac{\partial^2 U'}{\partial x^2} + D \frac{\partial^2 U'}{\partial y^2} \right) + E^\lambda - \theta \nabla P^\lambda.
\]

(24)

\(U'\) and \(U^\lambda\) are velocities at the intermediate and
previous time step, respectively. \(\theta\) is a parameter with
a value between 0 and 1; \(\theta = 1\) makes the method
incremental and \(\theta = 0\) makes it non-incremental. In
this paper, \(\theta\) is always chosen to equal 0.5. After calculating
the intermediate velocities (\(U'\)), the pressure field can
be obtained using the Poisson equation for pressure.

\[
\frac{\partial P^{\lambda+1}}{\partial x^2} + \frac{\partial P^{\lambda+1}}{\partial y^2} = \frac{1}{\Delta t} \left( \frac{\partial U'}{\partial x} + \frac{\partial U'}{\partial y} \right)
\]

\[ + \theta \left( \frac{\partial^2 P^\lambda}{\partial x^2} + \frac{\partial^2 P^\lambda}{\partial y^2} \right).
\]

(25)

For Eq. (25), operators \(L\) and \(f\) in Eqs. (10) and (11)
can be written as:

\[
L(\cdot) = \frac{\partial^2 (\cdot)}{\partial x^2} + \frac{\partial^2 (\cdot)}{\partial y^2},
\]

(26)

\[
f = \frac{1}{\Delta t} \left( \frac{\partial U'}{\partial x} + \frac{\partial U'}{\partial y} \right) + \theta \left( \frac{\partial^2 P^\lambda}{\partial x^2} + \frac{\partial^2 P^\lambda}{\partial y^2} \right).
\]

(27)

Using these pressure values, the velocity field can be
updated as follows:

\[
u^{\lambda+1} = u' - \Delta t \left( \frac{\partial P^{\lambda+1}}{\partial x} - \theta \frac{\partial P^\lambda}{\partial x} \right),
\]

(28)

\[
v^{\lambda+1} = v' - \Delta t \left( \frac{\partial P^{\lambda+1}}{\partial y} - \theta \frac{\partial P^\lambda}{\partial y} \right).
\]

(29)

5. Collocation generation

Collocation points have significant effects on the ac-
curcy and even on the convergence of the method [6].
However, there is not a well defined procedure to
distribute these points. It is clear that parts of the
problem domain with denser field nodes require denser
collocation points. In the present study, Delaunay
triangles are used to specify the position of collocation
points. First, all the field nodes are connected to
each other by Delaunay triangles. Then, collocation
points are determined to be in the middle of each
triangle side. As mentioned before, on each field node,
a collocation point also has to be placed. This simple
strategy guarantees that there are enough collocation
points everywhere according to field node positions.
In Figure 3, the position of the collocation points in
part of a sample domain, with respect to field nodes,
is shown.

Figure 3. Collocation points position in a sample domain.

6. Error estimate and node enrichment
strategy

A gradient based error estimator is used here. It is
based on summation of the normalized velocities and
viscosity gradients. It is given by:

\[
\text{Error} = \frac{\frac{\partial u}{\partial x}}{a} + \frac{\frac{\partial u}{\partial y}}{b} + \frac{\frac{\partial v}{\partial x}}{c} + \frac{\frac{\partial v}{\partial y}}{d} + \frac{\partial P}{f},
\]

where \(a, b, c, d, e\) and \(f\) are the maximum value
of \(\frac{\partial u}{\partial x}, \frac{\partial u}{\partial y}, \frac{\partial v}{\partial x}, \frac{\partial v}{\partial y}, \frac{\partial P}{\partial x}\)
and \(\frac{\partial P}{\partial y}\), respectively.

To enrich field nodes, in the first step, the estimated
errors are evaluated at all collocation points. Then,
a finite amount of collocation points with high errors
are chosen by sorting the errors. Finally, these chosen
collocations turn into field nodes for another solution
procedure. To start another solution procedure, again,
new collocation points must be generated, according to
the new distribution of nodes, as described earlier.

7. Shape function construction

In this study, RTIM is used to construct shape func-
tions. Detailed description of the procedure is available
elsewhere [2,3]. In the following numerical examples, a
multi quadratic radial basis function augmented with
polynomials of completed second order is used in the
radial point interpolation method. The multi quadratic
radial basis function \(q\) used in this paper is given by:

\[
q(r) = (ds^2 + r^2)^{0.63},
\]

(30)

where \(ds\) is the radius of the compact support domain
defined earlier. In the following numerical examples,
\( ds \) is always chosen for each collocation point, so that 25 nodes are placed into the support domain of that collocation.

8. Numerical examples
In this study, Carreau-Yasuda fluid flow in a square cavity is solved by a semi-incremental scheme in temporal discretization and a node enrichment process in spatial discretization. In temporal discretization, the semi-incremental factor, \( \theta \), is taken as 0.5 in all problems. For the sake of simplicity, \( \eta_0 \) and \( \eta_{\infty} \) are chosen to be one and zero, respectively. Eq. (18) shows that for a very low value of the characteristic time (or Carreau number), the fluid behaves like a Newtonian fluid. In this case, viscosity is independent of \( n \) and \( \alpha \). For a very high value of Carreau number, in Eq. (18), constant 1 can be neglected considering the typical values of \( Cu^{0.5 \alpha} \) and, hence, the fluid behaves like a power law fluid. The problem is solved by different curve fitting parameters. Three cases are considered, which are listed in Table 1. Each case is solved in two steps. First, the problem is solved using a uniform distribution of nodes. Then, according to estimated errors, some nodes are added to the previous nodes and the problem is solved again. Comparison is performed whenever well known published data is available. In all of the following examples, time step size is chosen to equal 0.01. Regarding penalty coefficients, they should be large enough to ensure boundary condition satisfaction. In this study, penalty coefficients are chosen to be \( \alpha = \beta = 10^5 \) for all cases. The lid-driven cavity flow problem is characterized by a square cavity in which the driving force for the flow is the shear created by a moving lid. The geometry and boundary condition of this problem are shown in Figure 4. Case (I) is equal to a power-law fluid flow with \( Re = 100 \) and index \( n = 0.5 \). In this case, Bell and Surana results [18] are used for comparison. To show the benefit of the enrichment procedure, the problem is first solved using 145 uniform nodes. Then, it is solved again by adding 144 extra nodes in two ways. First, these extra nodes are distributed among the previous nodes uniformly. Second, the extra nodes are distributed among the previous nodes using the enrichment procedure. These two domain discretizations are shown in Figure 5. It should be noted that for the following figures, collocation points located on field nodes are not shown. To make a comparison, the horizontal velocity component profile at the mid-span of the cavity is shown in Figure 6. It shows that with the same number of nodes, the enriched field node distribution shows a much better accuracy than uniform field node distribution. In the next example, case (I) is solved more accurately by distribution of 545 nodes. Using the defined procedure, collocation points are made. Nodes and collocation points are shown in Figure 7. The computed stream functions, before enrichment, are shown in Figure 8. Then, errors are estimated and using the enrichment procedure, 300 new field nodes are added. The new distribution of field nodes is shown in Figure 9, and the computed stream functions using enriched nodal distribution are shown in Figure 10. Case (II) is equal to a power-law fluid flow with \( Re = 100 \) and \( n = 1.5 \). In this case, Bell and Surana results [18] are also used for comparison. The procedure is the same as for case (I). Enriched field node distribution and collocation points are shown in Figure 11. To show the adjustment of the added nodes, counters for estimated errors are shown in Figure 12. In Figure 13, the stream function contours are depicted for this case. Case (III) is equal to a Newtonian fluid at \( Re=100 \). This case is compared with the results of Ghia and Shin [19] and the enriched field nodes and computed stream lines are shown in Figures 14 and 15. In Figures 16 and 17, the velocity profiles computed after the enrichment procedure are compared with the results of [18,19]. To show the effect of this nodal enrichment on the convergence of the method, in Figures 18 and 19, the convergence curves are shown for cases (I) and

![Figure 4. Boundary condition in lid-driven cavity flow problem](image)

<table>
<thead>
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<th>Case number</th>
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<th>( n )</th>
<th>( \alpha )</th>
<th>( Re )</th>
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</tbody>
</table>

Table 1. Problems parameters.
Figure 5. Domain discretization enrichment strategy (up) and uniform distribution (down); bigger circles are field nodes and smaller are collocation points.

Figure 6. Case (I) - u profile along vertical centre line (comparison between enriched and uniform field node distribution that were shown in Figure 5).

(II). According to these figures, the problem converges sooner after enrichment. The convergence index is defined as below:

\[ CI = \log \left( \frac{\max(u_{\text{en}} - u_{\text{un}})}{M} \right) \]  

\[ (31) \]

Figure 7. Uniform distribution of nodes (bigger circles) and generated collocation points (smaller circles) include 515 nodes and 2113 collocation points.

Figure 8. Case (I) - Stream function contours for case (I) using uniform nodal distribution that was shown in Figure 7.

9. Conclusions

In this paper, a node enrichment strategy, along with a gradient based error estimator, was presented for the collocated discrete least squares meshless method. The estimator considers both viscous and inertia gradients. It can be found from the numerical examples that for high Reynolds numbers, the enriched nodes focus on the positions where high velocity gradients are expected (cases (II) and (III)). With low Reynolds numbers or more viscous fluids, the new nodes are concentrated on areas with a higher gradient of viscosity (case (I)). Since the new field node distribution also needs a new collocation distribution, a simple
**Figure 9.** New added nodes (bigger circles) beside old nodes (smaller circles) make new domain discretization.

**Figure 10.** Case (I) - Stream function counters using enriched nodal distribution that was shown in Figure 9.

**Figure 11.** Case (II) - Enriched nodes (bigger circles) and generated collocation points (smaller circles).

**Figure 12.** Case (II) - Estimated errors counters in logarithmic scale.

**Figure 13.** Case (II) - Stream function counters using enriched nodal distribution that was shown in Figure 11.

**Figure 14.** Case (III) - Enriched nodes (bigger circles) and generated collocation points (smaller circles).
Figure 15. Case (III) - Stream function contours using enriched nodal distribution that was shown in Figure 14.

Figure 16. $u$ profile along vertical centre line after node enrichment.

Figure 17. $v$ profile along horizontal centre line after node enrichment.

The procedure was defined to distribute collocation points according to field node positions. As temporal discretization, a first-order accurate scheme, named the semi-incremental fractional step method, was used to guarantee the stability and accuracy of the method, regardless of field node distribution. The scheme was used to solve the lid-driven cavity flow of a Carreau-Yasuda fluid in different curve fitting indices values. The computed solutions show good agreement with the solutions reported in the literature.

References


**Biographies**

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